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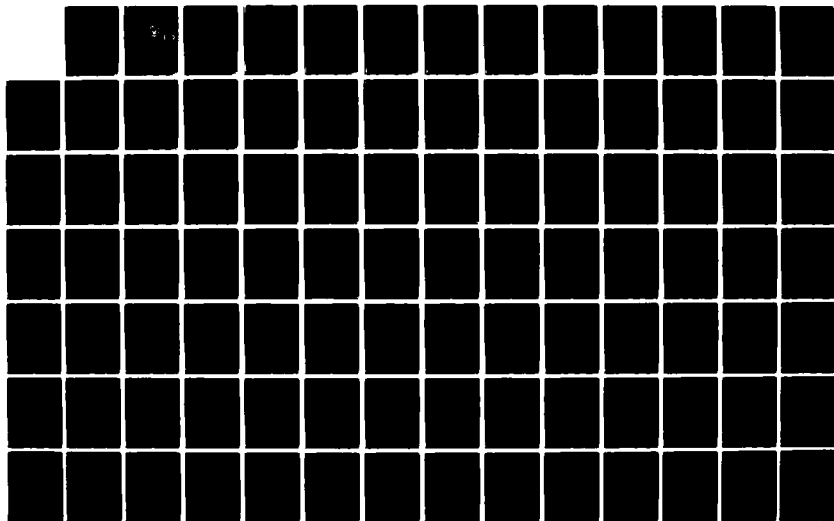
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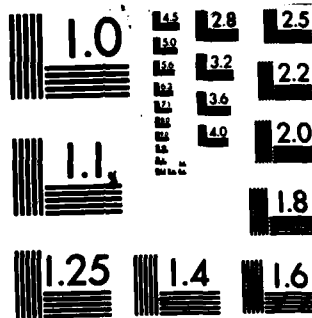
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THESIS

MARINE STEAM CONDENSER
DESIGN OPTIMIZATION

by

Thomas M. Buckingham

December 1983

Thesis Advisor:

R. H. Nunn

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Marine Steam Condenser
Design Optimization

by

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Lieutenant, United States Navy
B.A., College of the Holy Cross, 1977

Submitted in partial fulfillment of the
requirements for the degree of

MASTER OF SCIENCE IN MECHANICAL ENGINEERING

from the

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ABSTRACT

A surface-condenser analysis code was coupled with a constrained function minimization code to produce an automated marine condenser design and optimization package. The program, CONDIP, was based on the principles developed in ORCON1, a sophisticated computer code produced by the Oak Ridge National Laboratory. CONMIN, the optimization program, was developed at the Ames Research Center.

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TABLE OF CONTENTS

I.	INTRODUCTION	10
	A. BACKGROUND	10
	B. METHODOLOGY	10
	C. OBJECTIVE	13
II.	NUMERICAL OPTIMIZATION	14
	A. BACKGROUND	14
	B. CONSTRAINED FUNCTION MINIMIZATION (CONMIN)	15
	C. CONTROL PROGRAM FOR ENGINEERING SYNTHESIS (COPEs)	19
III.	CONDENSER DESIGN IMPROVEMENT PROGRAM (CONDIP) . .	21
	A. BACKGROUND	21
	B. CODE DEVELOPMENT	26
	1. Steam Flow Effects	29
	2. Steam Pressure and Temperature Effects . .	33
	C. LIMITATIONS	37
IV.	DESCRIPTION OF THE MAIN AND SUPPORTING SUBROUTINES	42
	A. MAJOR SUBROUTINES	42
	1. ANALIZ	42
	2. INPUT	42
	3. OUT3	43
	4. ORCON	43
	5. SECALC	44
	6. HETTRN	46
	7. COOLEX	47
	8. OUT2	48

9.	OUT2C	48
10.	OUT3	48
B.	SUPPORTING SUBROUTINES	49
V.	RESULTS	64
A.	CONDIP VERIFICATION	64
B.	EXPLANATION OF THE CASE STUDIES	69
1.	Constraint Framework for CONDIP	71
2.	Design Variable Framework for CONDIP	73
C.	CASE STUDIES USING CONDIP	75
1.	Case One	75
2.	Case Two	76
3.	Case Three	77
4.	Case Four	79
5.	Case Five	80
VI.	CONCLUSIONS	89
VII.	RECOMMENDATIONS	91
	APPENDIX A: GLOSSARY	93
	APPENDIX B: USERS MANUAL FOR CONDIP	97
	APPENDIX C: CONDIP LISTING	132
	LIST OF REFERENCES	224
	INITIAL DISTRIBUTION LIST	226

LIST OF TABLES

I.	Input Design Data	82
II.	CCNDIP Verification Results	83
III.	Volume Minimization	84
IV.	Power Minimization	85
V.	Power Minimization With Volume Constant	86
VI.	Volume Minimization With Power Constant	87
VII.	Volume Minimization With Linear Variations	88

LIST OF FIGURES

4.1	Flow Diagram For ANALIZ and COPES/CONMIN	19
4.1	Flow Diagram for the ANALIZ Subroutine	51
4.2	Flow Diagram for the INPUT Subroutine	52
4.3	Flow Diagram for the ORCON Subroutine	53
4.4	Flow Diagram for the SECALC Subroutine	54
4.5	Flow Diagram for the HETTRN Subroutine	60
4.6	Flow Diagram for the COOLEX Subroutine	61
B.1	Sample Data Input	131

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I. INTRODUCTION

A. BACKGROUND

For many years the steam plant was unchallenged in its role as the primary type of marine propulsion systems. But recently gas turbines have become a desirable alternative despite the fact that they are less efficient than comparable steam plants. The primary advantage of gas turbines is their light weight and compact size. Thus, in order for the marine steam plant to survive, it is imperative that lighter, more compact and efficient steam plants be developed.

While there are numerous advanced concepts in all areas of steam propulsion which can be explored, one simple way to streamline the steam plant is the elimination of overdesign. Most overdesign is due to unnecessary safety factors used to offset lack of detailed knowledge about the thermal processes in the plant. Identification of the minimum safe design could significantly reduce unnecessary overdesign and result in the development of a smaller, more compact power plant.

B. METHODOLOGY

In the United States the most prevalent criterion for the design and specification of surface condensers is based on the "square-root of V" relationship, as developed by the Heat Exchange Institute (HEI) [Ref. 1]. The HEI method was adopted by the Department of the Navy Bureau of Ships (now Naval Sea System Command) for specification of U.S. Naval condensers.

The HEI method is very simple in its approach, calculating the overall heat transfer coefficient as a function of cooling water velocity through the tubes, inlet coolant temperature, tube wall thickness and material, and fouling. The limitations of this method are apparent. Designs based on HEI are insensitive to shell-side conditions. Saturation steam pressure, temperature and enthalpy are assumed to be constant as steam passes through the bundle, whereas in reality there is a continual pressure drop as steam flow passes over the rows of tubes, with a corresponding decrease in saturation temperature. There is also no provision for any effects of condensate film, external tube enhancement, etc. on the shell-side of the bundle. In addition, the HEI method does not account for the presence and effect of non-condensable gases that inevitably contaminate a condenser.

With the capabilities of high speed computers now available, more comprehensive methods have been developed to account for the deficiencies of the HEI method. In particular, a radial flow computer code was developed to calculate the local heat transfer and thermodynamic properties on a row by row basis. Known as ORCON1, this code was developed by Oak Ridge National Laboratory (ORNL) under contract to the Office of Saline Water during the period from 1968-1970 [Ref. 2]. The program was based, in part, on the work performed by Eissenberg [Ref. 3]. Eissenberg's experimental results led to correction factors on the basic Nusselt equation to account for condensate inundation effects on tubes within a condenser bundle. Basically, ORCON1 divides the condenser into sectors and performs a row by row analysis within each sector, determining local heat transfer coefficients, heat flux, steam characteristics, the effect of condensate inundation and numerous other parameters at each row. ORCON1 is also capable of incorporating the effects of both tube-side and steam-side enhancement factors. Since

ORCON1 represented a much more comprehensive and detailed analysis of the condenser than the less exact HEI method, its results could be expected to be more precise.

Some work has been done at the Naval Postgraduate School to improve the capabilities of ORCON1. In his development of OPCODE2, Johnson [Ref. 5] added subroutines to ORCON1 which calculated tube-side pressure drops, corresponding pumping power and condenser volume. Nunn and Marto [Ref. 14] have incorporated the effects of vapor shear in an amended version of ORCON1 called MORCON. MORCON includes the correlations developed by Fujii [Ref. 4] to determine the effect of vapor velocity on the thermal resistance of the condensate film on the condenser tubes. In general, vapor shear effects tend to enhance the condenser heat transfer on the steam-side of the tube while condensate inundation tends to inhibit it.

The ability to represent numerically the actual thermodynamic processes occurring within the condenser has improved dramatically. However, the capability to couple these increasingly comprehensive and complex condenser design programs with an optimizing procedure has not made comparable progress. Optimization is a powerful tool which can help in reducing overdesign and achieving the goal of a safe compact condenser design.

There are currently numerous computer optimization programs available which can be coupled with general design programs of all types to numerically improve and ultimately determine the best design. The key is to properly write the design program so that it is compatible with the optimizer. Johnson [Ref. 5] developed a computer program called OPCODE1, based on the HEI method of condenser design, and was able to couple it with one such numerical optimizer. The results of OPCODE1 demonstrated how condenser designs can indeed be safely improved upon. It also revealed the

versatility of condenser design optimization as a powerful design tool. However, Johnson was unsuccessful in coupling OPCODE2 (his derivative of ORCON1) with an optimizer. This failure does not alter the fact that in order to fully appreciate more sophisticated condenser design analyses, such as that used in ORCON1, it is imperative that computer programs be developed which will be compatible with current numerical optimizers.

C. OBJECTIVE

There were two primary objectives of this thesis. The first objective was to develop a computer code which incorporates the basic condenser analysis of ORCON1 and the subsequent improvements made in MJRCON and OPCODE2, but which will be capable of being coupled with a numerical optimizer to yield a complete, detailed design package. This design package can then be used as a tool in obtaining a much more reasonable conceptual design and for use in comparison studies. It would provide the naval architect the ability to optimize weight, volume, cost or any other potential design objective of the marine plant.

The second objective was to make this design package capable of determining the single best design rather than simply an improvement over the initial design. The key was to construct the program in such a way so the optimizer does not stop at some relative optimum, but continues the analysis until no further improvement can be realized. It is most desirable to be able to reach this single true optimum design regardless of initial design variable values.

II. NUMERICAL OPTIMIZATION

A. BACKGROUND

Nearly all design problems require either the minimization or maximization of a parameter. This parameter will be called the problem's objective function or design objective [Ref. 6]. For a given design to be feasible or acceptable, it must satisfy a set of design constraints which are either maximum or minimum limiting values for a pre-determined set of parameters or functions of parameters. For example, in any condenser design the outer diameter of a condenser tube can never be less than zero and there is normally some practical upper limit which also cannot be exceeded. These limits are design constraints on the tube outer diameter. In the design problem there is also a set of design variables which are parameters whose values can be changed within specified limits in order to minimize or maximize the design objective. For example, in minimizing the condenser volume an engineer may want to vary tube inner diameter, tube wall thickness and tube length. These three parameters would thus be examples of typical design variables.

For such complex design problems as the treatment of the condenser design in ORCON1, it is necessary to choose an optimization scheme which can handle the problem and provide a rational, rapid approach to design automation and optimization. An optimization program based on direct methods for solution of constrained problems [Ref. 11] was chosen for this research work.

B. CONSTRAINED FUNCTION MINIMIZATION (CONMIN)

Vanderplaats [Ref. 7] developed an optimization program, CONMIN, capable of optimizing a very wide class of engineering problems. CONMIN is a fortran program, in subprogram form, that optimizes a multi-variable function subject to a set of inequality constraints.

It is practical at this point to introduce three basic definitions and their respective conditions [Ref. 8].

DESIGN VARIABLES: Those parameters which the optimization program is permitted to change in order to improve the design. Design variables appear only on the right side of an equation, are continuous, and have continuous first derivatives.

DESIGN CONSTRAINTS: Any parameter which must not exceed specified bounds for the design to be acceptable. Design constraints may be linear or nonlinear, implicit or explicit, but they must be functions of the design variables. Design constraints appear only on the left side of equations.

OBJECTIVE FUNCTION: The parameter which is going to be minimized or maximized during the optimization process. The objective function may also be either linear or nonlinear, implicit or explicit, and must be a function of the design variables. The objective function usually appears on the left side of an equation. The only exception is if the objective function is also a design variable.

Assuming that the optimization process requires the minimization of a particular objective function the general optimization problem can be stated as:

Find the vector of design variables, \underline{X} ,
To minimize the objective function, $F(\underline{X})$,
Subject to the constraints:

$$G_j(\underline{X}) \leq 0.0 \quad j = 1, NCON \quad (\text{eqn 2.1})$$

$$VLB_i \leq \underline{X} \leq VUB_i \quad i = 1, NDV \quad (\text{eqn 2.2})$$

In the general problem, $G_j(\underline{X})$ are the constraint functions; there are NCON constraints and NDV design

variables; VLB_i and VUB_i are the lower bounds and upper bounds of the i -th design variable. If the equality condition is met, $(G_j(\underline{X})=0.)$, the constraint is active. If the inequality is met, $(G_j(\underline{X})<0.)$, the constraint is inactive. Finally, if the inequality of equation 2.1 is violated, $(G_j(\underline{X})>0.)$, that constraint is said to be violated. Because of numerical inaccuracies representing exact zero on the computer, the equality condition is represented by a band around the value $G_j(\underline{X})=(0.\pm CT)$ where CT is the constraint thickness.

Any design which satisfies the inequalities of equations 2.1 and 2.2, thus having no violated constraints, is said to be feasible. If the design violates any of these constraints it is said to be an infeasible design. The design which best minimizes the objective function while still remaining feasible is said to be optimal.

CONMIN requires an initial set of values for the design variables \underline{X} to obtain an initial design which is either feasible or infeasible. If the initial design is feasible, CONMIN moves in a direction which will minimize the objective function. If the initial design is infeasible, CONMIN moves toward a feasible solution with minimal increase in the object function.

The optimization process proceeds in an iterative fashion. Johnson [Ref. 5] presents in greater detail the procedures utilized in CONMIN to search for the minimum objective value. In general, the methods used by CONMIN to determine search direction include the method of steepest descent, the method of conjugate direction, and the method of feasible directions. For further background concerning CONMIN and the numerical techniques utilized in optimization, consult Vanderplaats [Ref. 7], Fletcher and Reeves [Ref. 9], Zoutendijk [Ref. 10], and Vanderplaats and Moses [Ref. 12]. However, it is necessary to stress a few pertinent points which will aid in understanding how the program was developed in this thesis.

The optimization process begins by calculating the gradient of the objective function using a finite difference technique. A perturbation is applied to each of the design variables in a single forward step and the gradient vector is determined.

$$\Delta F(X) = \begin{bmatrix} \frac{\partial F(X)}{\partial x} \\ \frac{\partial F(X)}{\partial x} \end{bmatrix}$$

The search direction is then calculated and is a function of this gradient and any active or violated constraints resulting from the applied perturbation. Subsequent search directions are a function of previous search directions, as well as current gradient information and any appropriate constraint factors. Obviously, the size of the perturbation and the size of the bandwidth about an active constraint will have a great deal of effect on the search direction and ultimate optimization process. This detail will be recalled later-on during the code development.

There are some limitations to CONMIN. The number of design variables (NDV) directly affects the computational time required to reach an optimum. Since the calculation of the gradient information required for each design variable at the beginning of each design iteration is found by using a single forward finite difference step, requiring a complete pass through the analysis portion of the program, there is an increase in CPU time as NDV increases. Also, as NDV increases, there is the corresponding rise in machine related numerical innacuracy. Vanderplaats [Ref. 6] recommends no more than twenty as a practical limit for the number of design variables.

It is quite possible that while design improvement may be obtained, the single best design optimum or true optimum

may not be reached. This is not an uncommon occurrence and there are several possible explanations. For example, the design problem may not be formulated properly or the analysis may be extremely complex and non-linear. However, a more common reason is that there are "relative optimums" between the initial design and the single true optimum. This concept of relative vs true optimum design can be better explained through an analogy. The search for the best optimum design can be likened to a blind man climbing to the top of a mountain. The blind man knows he is proceeding up the mountain by sensing the direction of ascent. However, the paths he takes may be limited by barriers or fences which will restrict the directions he can go. These fences represent constraints in the optimization problem. During the journey he may also encounter small crests and valleys. If the available paths lead the blind man up to one of these crests prior to reaching the mountain top, he will be confronted with a situation where he will sense no further rate of ascent and he will stop his journey. So although he has made progress from his initial starting point, the man did not achieve his ultimate goal of climbing the mountain.

During optimization, the search for a true optimum may proceed along a path on which the objective function assumes such relative optimum values. If the optimizer can not be made to "look beyond" these relative peaks, then the optimization will cease - at a design which may be an improvement over the initial one but short of the true optimum. This problem may be overcome by starting the design with several different initial design vectors, \mathbf{x} , until the same optimal design is repeated. Another alternative may be to increase the size of the finite difference so that the optimizer uses larger perturbations of \mathbf{x} thus looking beyond any small increases in the objective function which could stand in the way of further design progress. This second

alternative will be specifically addressed during the discussion of the code development.

C. CONTROL PROGRAM FOR ENGINEERING SYNTHESIS (COPES)

The optimizer, CONNIN, was written in subroutine form. Vanderplaats [Ref. 13] has developed a main program to simplify the use of CONNIN and aid in the design optimization process.

The user must supply an analysis subroutine called ANALIZ, which consists of three segments: input, analysis and output. COPES acts as an interface between ANALIZ and the optimizer CONNIN. Based on a flag from COPES (ICALC=1,2,3) ANALIZ performs the proper function. Figure 2.1 offers a simplified illustration of the interrelationship between COPES, ANALIZ and CONNIN.

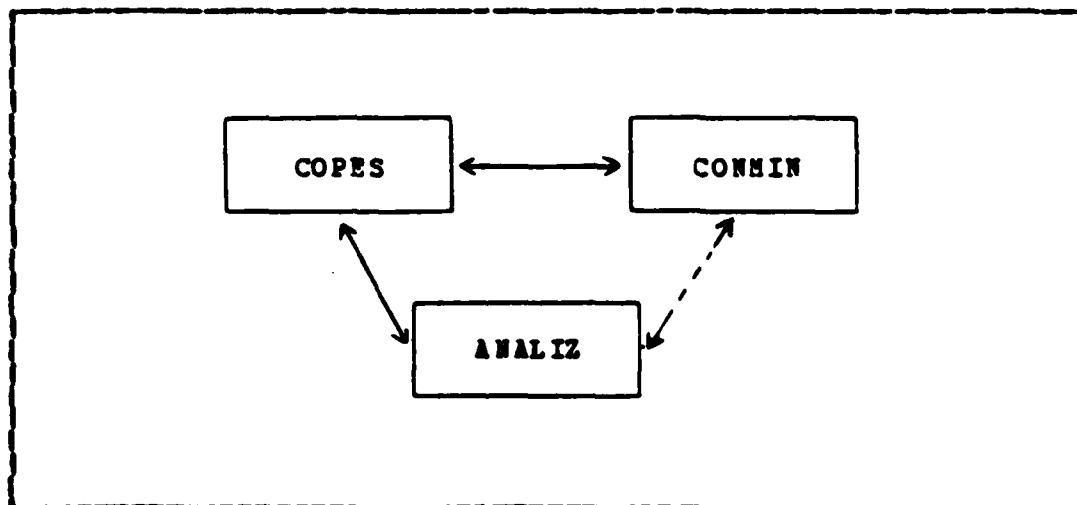


Figure 2.1 Flow Diagram For ANALIZ and COPES/CONNIN.

COPES currently provides four specific capabilities, two of which will be applied in this work:

1. Single analysis - just as if COPES/CONMIN were not used.
2. Optimization - minimization or maximization of a multi-variable function with corresponding constraints.

COPES requires certain initial data from the user in order to coordinate the optimization process. Initial values for the design variables as well optimizer control parameters are utilized by CONMIN to conduct its numerical analysis. There are a few optimizer parameters which are particularly important to the treatment of condenser designs. One is the finite difference step used in gradient calculations. Another is the normalization factor used in COPES evaluation of a constraint function. COPES utilizes the following expressions in determining constraint function violations:

$$\frac{BU - CPV}{SCAL1} \leq 0.$$

$$\frac{CPV - BL}{SCAL2} \leq 0.$$

where SCAL1 and SCAL2 are the normalization factors, BU and BL are the upper and lower limits of the constraint, and CPV is the constraint function value. It is intuitive that the normalization factor can play an important role in determining the size of the active region about a given design constraint. Both finite difference and constraint normalization will be recalled later during the code development.

The power of COPES is that it has simplified the procedures involved in using a sophisticated program such as CONMIN. The user is therefore freed from the unwanted role of systems analyst and can concentrate on the design analysis.

III. CONDENSER DESIGN IMPROVEMENT PROGRAM (CONDIP)

A. BACKGROUND

In the late 1960's, engineers at the Oak Ridge National Laboratory developed a sophisticated computer code under contract to the Office of Saline Water. This code, called ORCON1, [Ref. 2] was generated to aid in the analysis and parametric study of large, generally circular condensers. Much of ORCON1 was dependent on Eissenberg's research work [Ref. 3] on the effects of condensate rain on the shell-side convective heat transfer coefficient. Johnson [Ref. 5] took ORCON1 and made a few minor modifications to determine tube side pressure losses and volumetric calculations. Nunn and Marto [Ref. 14] further incorporated the correlations proposed by Fujii [Ref. 4] to determine the effects of shearing forces exerted by high vapor velocities on the condensate film and resulting shell-side heat transfer coefficient.

It was at this point that the development of CONDIP was begun. CONDIP was dependent primarily on the principles detailed in ORCON1 but also incorporated subsequent developments to the basic program. CONDIP was written, however, in such a way as to be compatible with the optimizer, CONMIN.

CONDIP analyzes a single or double pass, circular or semicircular condenser, with steam flowing radially inward on the shell-side of the tubes and variable salinity water flowing on the tube-side. An optional, rectangular air cooler bundle is provided-for as well as shell-side baffles. The circular bundle is normally divided into 30-degree sectors with symmetry about the central axis to reduce computational effort. Unless otherwise specified, tubes are

placed on a 60-degree equilateral, triangular pattern of concentric rows with the rows added from an inner void out to the outermost row. The void serves as a collection header for non-condensable gases prior to passage through an air cooler, if specified. As in ORCON1, CONDIP proceeds sector by sector, row by row through the condenser utilizing an average tube to represent the row segment, and calculates the following quantities in each sector:

- a) Steam pressure losses at the entrance of a sector.
- b) Total pressure of the steam/non-condensable gas mixture entering a row segment.
- c) Saturation pressure of steam entering a row segment.
- d) Saturation temperature of the steam entering a row segment.
- e) Steam flow entering the row segment.
- f) Velocity of the steam/non-condensable gas mixture at the minimum cross-section in the row segment.
- g) The fraction of non-condensable gas in the mixture by weight.
- h) The overall heat transfer coefficient for the average tube in the row segment.
- i) The steam-side condensing coefficient.
- j) The tube-side heat transfer coefficient.
- k) The shell-side film heat transfer coefficient composed of the non-condensable gas film and the condensate film.
- l) The shell-side friction factor.
- m) The shell-side pressure loss as steam passes over the row segment.
- n) The shell-side Reynolds number based on the mass flow at the minimum cross-sectional area in the row segment.
- o) The heat transfer rate per square foot of condenser tube.
- p) The mass flow rate of steam/non-condensable gas mixture at the minimum cross-section in the row segment.

- q) The mass flow of condensate produced as steam passes over the row segment.
- r) The cooling water temperature at the outlet end of the condenser.
- s) The coolant pressure loss on the tube-side.
- t) The average Reynolds number of the coolant through the tube.
- u) The heat transfer coefficient for the non-condensable gas film.
- v) The internal heat film heat transfer coefficient.
- w) The number of tubes per row segment.
- x) The cross-section area available for steam flow per row segment.
- y) The cumulative shell-side pressure drop.
- z) The LMTD based on inlet and outlet coolant temperatures and saturation temperature at each row segment.

In addition to the above parameters, the area-weighted overall heat transfer coefficients for the condenser, cooler and combined condenser are used to calculate the "back calculated" log mean temperature difference (LMTD). Steam exit-fraction, condenser volume, coolant pumping power and numerous other factors are calculated from the cumulative results of the row and sector analysis.

There are two significant contributions to the external film heat transfer coefficient which have a profound impact on the overall analysis. As mentioned earlier, Eissenberg [Ref. 3] corrected for condensate inundation effects on the external heat transfer coefficient with a series of empirical relations. He created a flooding factor F using the following relation:

$$F_n = .6F_d + (1 - .5647 F_d) n^5 \quad (\text{eqn 3.1})$$

where F_d is a constant indicating the effect of tube spacing and orientation on condensate side drainage. With closely packed tubes, significant side drainage can occur in low velocity steam flow. Condensate generated on tubes above may, due to surface tension effects, proceed laterally to adjacent tubes rather than down. Thus F_d tends to approach 1.0 for closely packed, staggered tube bundles and zero for disperse bundle layouts. S is a constant ranging in value from:

$$(.07 < S < .25)$$

If the condensate rain is acting under the influence of gravity alone S approaches 0.25. But the influence of any steam velocity present begins to alter the rate and direction of condensate flow and correspondingly decrease S . Thus S is a function of vapor velocity and direction, as well as bundle geometry.

The condensate film coefficient for the average tube in the n -th vertical row is then calculated from the uncorrected heat transfer coefficient, h_o , as follows:

$$h_n = [nF_n - (n-1)F_{n-1}] h_o \quad (\text{eqn 3.2})$$

It is obvious that the determination of a corrected heat transfer coefficient is highly dependent on the choice of S and F_d in equation 3.1. S and F_d are extremely subjective constants and there does not exist a current analytical expression to determine them. Yet the choice of these constants can have profound impact on the condenser design. In CONDIP, as in DRCCN1 [Ref. 2], the following, relatively conservative values for S and F_d were used:

$$S = 0.2$$

$$F_d = 0.5$$

An additional important contribution to the external film coefficient is the effect of velocity shear forces on the condensate film. Fujii [Ref. 4] developed the following experimental correlations to correct the Nusselt number for the effect of velocity shear:

$$[Nu_m / Nu_o] = c_1 Nu_o^{(4a-1)} Re_L^{(.5-2a)} \quad (\text{eqn 3.3})$$

where Nu_m is the mean Nusselt number, Re_L is the two-phase Reynolds number (based on vapor velocity, tube outside diameter and kinematic viscosity of the condensate) and Nu_o is the standard Nusselt number for the zero shear case. The empirical constants c_1 and a lie within the following ranges:

$$1.13 < c_1 < 1.24$$

$$0.196 < a < 0.2$$

depending on how tube thermal conditions are described. In CONDIP the values for c_1 and a were:

$$c_1 = 1.24$$

$$a = 0.2$$

It should be noted that equation 3.3 is only valid in the range:

$$3.3 < (Re_L / Nu_o) < .28.$$

For smaller values of this parameter Fujii recommends the use of a slightly reduced value of the standard Nusselt number:

$$Nu_m = 0.96 Nu_o \quad (\text{eqn 3.4})$$

It is apparent that the vapor velocities commonly encountered in naval condensers can have an impact on the heat transfer coefficient.

B. CODE DEVELOPMENT

Johnson [Ref. 5] attempted to couple OPCODE2 (his version of ORCON1) with the optimizer CONMIN, but with little success. There were several reasons for this.

ORCON1 uses iterative techniques to solve for such quantities as condensate rate, steam mass flow rate and steam pressure through the sector. If unrealistic values are encountered, such as negative pressures or steam flow, or if the final steam exit-fraction exceeds a predetermined value, ORCON1 stops the analysis, returns to the beginning of the program and changes certain initial input parameters. The analysis begins again and the process is repeated until a satisfactory design is achieved. Thus ORCON1 has a limited capability to make design decisions to obtain a feasible design.

CONMIN, as do most optimizers, requires complete control in determining all iterative design variable values. As explained earlier, it uses perturbation techniques to calculate gradient information for each design variable and active design constraint, which it then uses to determine search directions. A perturbation of the design variable by CONMIN requires a complete, once-through analysis. If ORCON1 is coupled with CONMIN then any adjustment by ORCON1 will yield false gradient information to the optimizer and hinder, if not completely prevent, CONMIN from arriving at the optimum design. During program development it became apparent that the two programs were working independently against each other and that in its present state ORCON1 was incompatible with CONMIN.

In the formulation of CONDIP, it was necessary to locate and neutralize all the places where such design decisions are made. By removing the ability for CONDIP to make any design decisions it became totally passive and dependent on CONMIN for design variable changes.

However, once this was accomplished, another problem area was discovered. In the ORCON1 code and subsequently in CONDIP there are numerous thermal process and properties calculations that use logarithmic functions and other mathematical relationships which could produce singularities if the variables in the arguments approach zero or are negative. For example, saturation steam temperature is calculated from steam pressure using a logarithmic relationship. If, during a design analysis, saturation pressure approaches a negative value, this represents a clear violation of physical realities and of the limits of that property. Yet a computer cannot make that distinction so it tries to calculate the corresponding saturation temperature which, because of the logarithmic relationship, would be undefined. As just explained, ORCON1 with its built-in decision capability simply starts over when this situation is encountered. But CCNDIP, being completely dependent on CONMIN for design decisions, does not have that capability. Remembering that CONMIN requires a complete once-through analysis in order to collect enough information to make a design decision, it was necessary to somehow bypass such mathematical instabilities in order to keep the program operating. Yet the analysis still had to yield reasonable results from the given design in order to obtain meaningful gradients. This prompted the formulation of mathematical relationships to create "penalty" constraints which, if properly written, would indicate to the optimizer that a function or thermal property has violated its physical limits. However, not only would penalty constraints have to be defined, but a "fix up" or "correction" of the violated property or variable would be required in order to allow the analysis to continue. A good physical understanding of the inter-relationship between condenser parameters and the thermal processes resulting from the condenser design is

necessary so that the "fix up" of the violated property would still yield fairly accurate condenser information on which CONMIN could base its search for the optimized design.

For example, a condenser is usually designed around a given steam load. If the condenser has too many tubes, is too long, or coolant flow is too great, then the condenser will be overdesigned. There will be dry tubes within the condenser as all the steam is condensed before steam flow reaches the inner void. In CONDIP this means that zero or negative steam flow will be encountered in the analysis.

If, on the other hand, tube surface area is too small, coolant flow is inadequate or the condenser tube spacing is too tight and is choking the steam flow, then one of two things will happen. Either a quantity of uncondensed steam will make it completely through the condenser, or steam pressure loss in the condenser will cause steam pressure to drop below zero. In addition, there are two reasons why all the steam might not condense. It could be simply due to insufficient heat transfer surface area or it could be because the saturation temperature of the steam has dropped below the coolant inlet temperature. If the latter situation occurs, then there is no driving force for heat to transfer from the steam to the coolant. There is only one way that this situation can occur: if steam saturation pressure drops below some value indirectly determined by the coolant inlet temperature. In any event this condenser is certainly underdesigned and not capable of supporting the required steam load.

As stated earlier, the purpose of optimization is to obtain the best, feasible design. Thus, an understanding of the relationship between the physical characteristics of a given design and the subsequent thermal performances will certainly help in defining the appropriate penalty constraints and their corresponding limits. It will also

aid in the determination of appropriate "corrections" when those limits are violated. It is important to note that with the introduction of these penalty constraints, the definition of a feasible design is revised. A feasible design is now defined as one in which thermal properties and functions are not allowed to violate their physical limits, as well as other design constraints, anywhere in the condenser.

In CONDIP there are three basic thermal properties which could create the above mentioned problems if they fall below a certain value. They are steam saturation pressure, steam flow and steam temperature. Because of the direct relationship between steam saturation pressure and temperature, it was possible to deal with them simultaneously. The solutions that were developed to overcome the effects of these thermal violations determined the extent which CONDIP would optimize.

1. Steam Flow Effects

One source of mathematical instabilities within the program is if steam flow over the tubes falls to zero or below. It is intuitively obvious that steam flow can not physically fall below zero and that in order to keep the program running the steam flow rate must be kept greater than zero. However, correcting for this alone would certainly alter the results of that particular condenser design, perhaps even imply a feasible design.

To indicate to the optimizer an infeasible design was actually encountered - one in which steam flow had dropped below zero - the penalty function WTST was created. Since the condenser analysis is performed sector by sector and assuming there are J sectors in the condenser, then there had to be arrangements for J penalty constraints. This prompted the creation of the array, WTST(J), representing constraint penalty functions for each sector. The absolute

magnitude of these functions were directly related to both the severity of the steam flow violation and the number of dry tubes remaining in the sector. WTST(J) ranged in value from negative infinity to zero, where a value of zero represented a condenser design in which no flow violations occurred. Thus, WTST(J) were constrained functions whose lower limit was zero. For example, during an analysis, if steam flow was determined to fall below zero, then WTST for that sector would be given some negative value. In subsequent designs, as the number of dry tubes approached zero and better designs were obtained, then the magnitude of the penalty function approached zero indicating no constraint violation.

Since penalty constraints are entirely contrived relationships with no real physical basis, it is desirable to minimize their number to avoid the possibility of sending inaccurate signals to the optimizer.

To eliminate the need to use the WTST penalty functions as constraints, the values of WTST(J) were consolidated at the end of the sector analysis into the condenser steam exit-fraction constraint. Normally, steam exit-fraction ranges from zero to one and is simply equal to:

$$\frac{\text{steam leaving the condenser}}{\text{steam entering the condenser}}$$

By incorporating the WTST violations into steam exit-fraction, the exit-fraction was made a continuous function ranging in value from negative infinity to one. The negative steam exit-fraction represented a partially dry condenser and its magnitude was in direct proportion to the number of dry tubes. Thus instead of having to evaluate and calculate gradients for J number of WTST(J) constraints, the optimizer simply had to evaluate a previously defined and now expanded exit-fraction constraint.

It should be stressed that making steam exit-fraction continuous through zero was equally as important as eliminating the need for additional constraints. It can be reasonably assumed that for all practical condenser applications, exit steam fraction will always be limited to some positive number near zero. Here is where one applies the physical knowledge of the condenser and its relation to the thermal property of steam flow. As explained earlier, dry tubes represent an over-designed condenser. Thus the natural tendency is for the optimizer to alter those design variables so as to create a more compact condenser. As this occurs, steam exit-fraction will naturally increase. The upper active limit of that constraint will determine the optimum feasible design. While it is not necessary to have a lower limit for steam exit-fraction, it is very important for it to be a continuous smooth function especially in the region near the upper limit. It is therefore critical to properly define the penalty functions $WTST(J)$ in a way so as to provide a smooth transition from the negative, artificial values of negative steam exit-fraction to the real, positive values.

Since the steam flow penalty functions will not be used as constraints, the analytical results will provide gradient information to the optimizer. However, once steam flow has been determined to fall below zero, steam flow for that first dry row of tubes and all subsequent rows must be fixed up with dummy values to allow the program analysis to continue. How that "fix-up" is accomplished will ultimately determine the search direction for the optimizer.

Physically, once steam flow has gone to zero, there should be no further latent heat transfer, no subsequent condensate production, and further pressure losses should be only due to the flow of non-condensable gases. It is necessary to make the computer generated analysis reflect as

closely as possible these physical realities. Since the optimizer no longer has the penalty functions to use in calculating a search direction, other constraint values obtained from the analysis will dictate the next search direction. Gradients will also be calculated using these results and the determination of the next search direction will incorporate these gradients as well. In the case of negative steam flow, steam flow and condensate production over dry rows were given nominal values which were as small as the computer analysis would tolerate. These extremely small values closely approximate zero steam flow and generate results which resemble physical reality as closely as possible.

The following example is provided to better illustrate the logic used in CONDIP to handle negative steam flow. CONDIP determines flow rate through each row in each sector. During a sector analysis, CONDIP calculates the condensate generated at a given row and subtracts that value from the steam flow entering that row to calculate the steam leaving. The exiting steam flow rate is then checked to determine whether steam flow has gone to zero. If it has not, then the analysis continues. If it has, then the following two events occur.

The penalty function, $WTST(J)$, is calculated for that sector and dummy values are inserted for steam flow and condensate rate at the row where the violation occurred. For the remainder of the analysis condensate generation and subsequent steam flow calculations are bypassed and the remaining rows in the sector are fixed up with dummy values for steam flow and condensate. The analysis continues utilizing these dummy values in all appropriate heat transfer and pressure calculations. At the conclusion of the sector analysis, the values of the penalty functions, $WTST(J)$, of each sector are incorporated into the steam exit-fraction.

If the analysis revealed zero dry tubes then WTST(J) for all sectors would be zero and the steam exit-fraction would simply be calculated as:

$$\frac{\text{steam leaving the condenser}}{\text{steam entering the condenser}}$$

If, however, dry tubes were encountered in the condenser analysis then WTST(J) of some or all the sectors would be negative and dependent in magnitude on the number of dry tubes in each of the J sectors, as well as the severity of the steam flow violation. Steam flow leaving any sector which has gone dry would be zero and steam exit-fraction would be evaluated as:

$$\frac{\text{steam leaving any wet sectors}}{\text{steam entering the condenser}}$$

plus a weighted value of all the WTST(J) penalty function values. Using the relationships just described, it is apparent that steam exit-fraction: is negative if condenser tubes are dry; approaches zero as the design becomes feasible; and is greater than zero if there is steam leaving the condenser.

2. Steam Pressure and Temperature Effects

The other possible source of mathematical instability occurs when steam pressure falls below some preset limit. If pressure falls to zero, numerous mathematical singularities will be generated. Yet, before this situation can occur steam temperature will have already fallen below inlet coolant temperature causing singularities in the log mean temperature difference (LMTD) heat transfer calculation. Thus, the lower pressure limit which cannot be physically exceeded is not zero but the minimum saturation pressure established by the inlet coolant temperature. In CONDIP, this lower limit is given the variable name, PTLIM.

As steam flows through the condenser, pressure continually decreases due to friction losses and therefore, it is evaluated at each row in each sector. When the steam saturation pressure drops below PTLIM, indicating a physical violation of realistic limits, then the creation of a penalty function and a corresponding "fix up" of saturation pressure is required to allow the program to continue. The treatment of the problem was therefore analogous to the previous situation dealing with negative steam flow.

PTST(J) was the penalty function devised to indicate to the optimizer that the pressure limit, PTLIM, was violated in any of the J sectors. Values of these constraints ranged from negative infinity to zero, depending on the degree and location in the condenser of the violation. Since pressure is calculated on a row by row basis in each sector, the magnitudes of the pressure penalty functions were directly dependent not only on how much the calculated pressure dropped below PTLIM, but also on the number of rows remaining in the sector. Thus, as the condenser approached a feasible design the PTST(J) constraint values approached zero, indicating lessening violation of the minimum pressure.

As emphasized earlier, it is important to minimize the number of constraints, not only to avoid the possibility of sending confusing signals to the optimizer but also to reduce cost and improve program efficiency. This was accomplished here by inserting dummy values not only into the violated pressure variables but also associated thermal properties such as condensate generation, heat transfer coefficients and heat transfer rates for the row where the violation occurred and all subsequent rows in the sector. The dummy values were chosen such that realistic gradient information would be sent to the optimizer. The proper choice of "fix-up" values for these variables resulted in

the elimination of penalty functions as design constraints, and provided sufficient information to determine subsequent search directions.

It is necessary to understand the influence that steam pressure and temperature exert on the overall condenser analysis. With this knowledge it will be easier to predict the physical designs which could cause violations of the pressure limit. PTLIM is violated due to excessive steam flow pressure losses. As explained earlier, these large pressure losses would result from large steam velocities that are found in condensers which are too tightly designed. Thus, the particular condenser design is incapable of handling the required steam load, implying an infeasible design. Understanding this relationship will aid in choosing the appropriate "fix-up" values which will indicate to the optimizer that when the pressure limit is violated an infeasible condenser has been designed.

Physically, When steam temperature falls below coolant inlet temperature (PTLIM is violated) there is no heat transfer from the steam to the coolant and no additional steam is condensed. These physical realities must be reflected in the condenser analysis. Therefore, in subsequent rows, condensation and heat transfer rates were set equal to zero. Since there is no further condensation, the steam exit-fraction is equal to the steam flow at the point of violation divided by the total flow into the condenser. Thus PTLIM indirectly determines the exit steam fraction of the infeasible design. This relationship between exit-fraction and the PTLIM violation is what makes the penalty constraints obsolete. If PTLIM is violated early in the steam's passage through the condenser, steam exit-fractions will be large, violating its upper constraint limit and thus reflecting an underdesigned condenser. As the condenser design improves, then exit-fractions will decrease.

Physically, this can only be accomplished if the condenser design "opens up", reducing pressure losses in the condenser. Consequently, as condenser designs become larger, steam exit-fractions decrease and the condenser is driven towards a feasible design.

The following example illustrates the logic employed by CONDIP to handle steam pressure and temperature violations within the analysis. Condenser inlet flow is divided by the number of sectors in the condenser. Condenser inlet saturation pressure is determined by the steam inlet temperature. Entrance pressure losses are calculated and subtracted from the inlet pressure. The resulting pressure is checked against PTLIM and a violation at this point indicates a totally infeasible condenser in which no steam is condensed. Steam exit-fraction will thus be equal to one. If the saturation pressure is greater than PTLIM the analysis continues row by row through the sector. Pressure losses over each row are calculated and subtracted from the row inlet pressure to determine pressure into the next row of tubes. If this next-row steam pressure is determined to fall below PTLIM, then a thermal violation has occurred requiring "fix up". Subsequent rows are made to indicate zero condensate generation and zero heat transfer. Steam flow over the remaining rows is maintained at a constant value, which will subsequently be used to determine steam exit-fraction. Pressure variables over the remaining rows are given small positive values just large enough to allow the analysis to continue. Although all heat transfer and condensate calculations will be bypassed, the analysis must be allowed to continue so that pressure losses will continue to be calculated based on the steam flow at the point of violation. This is important since steam flow adjustments to the sectors are based on certain pressure comparisons between the sectors. The cumulative sum of all row pressure losses

in each of the sectors must be equal to within some tolerance. If they are not then steam flow into each of the sectors is altered so that the exit pressures from each sector converge to some common value. Thus, an accurate reflection of true pressure losses is important to this calculation.

The value of the steam exit-fraction is again determined to be the single constraint necessary to drive subsequent condenser designs to a feasible optimum configuration. The pressure penalty constraints proved to be superfluous information, but the corresponding variable "fix-up" was critical in the determination of search direction.

C. LIMITATIONS

During the development of CONDIP, it became apparent that steam exit-fraction would become the key constraint during optimization of any objective function. A feasible design implies that steam exit-fraction is a small positive number perhaps somewhere between zero and 0.1 percent. As explained earlier, violations of either steam flow or pressure physical limits resulted in penalty functions and variable "fix-up" which were later directly or indirectly incorporated in the calculation of steam exit fraction. Thus any feasible design, let alone the optimum one, centers on the limits placed upon this design constraint. Any number of design variable combinations will yield a feasible design, and each design variable affects steam exit-fraction differently. The intertwined, complex calculations used to ultimately determining exit-fraction are done by sector and row with each design variable repeatedly playing a factor. For example, the profound effect of both vapor shear and condensate inundation on the shell-side heat transfer coefficient and consequently steam exit-fraction, is

indirectly determined by numerous design variables. However, their effects are impossible to predict. The cascading effect of the thousands of calculations performed during the course of a design analysis is to ultimately create a single, highly non-linear variable in the form of the steam exit-fraction, upon which design decisions will be made.

As more design variables were involved in the analysis, the optimizer had difficulty determining their often conflicting effects on both the objective function and the steam exit-fraction. A small perturbation of each of the design variables independently would yield gradients indicating design improvement. But when these gradients were evaluated simultaneously to actually determine the direction of the subsequent design, their combined effect would actually indicate either no improvement of the objective function or a violation of the steam exit fraction design constraint. The end result would be that the optimization process would stall as no feasible search direction could be obtained. Larger perturbations to the design variables were required to properly evaluate their relative effects on the objective function and any active or violated constraints. This would enable the optimizer to overcome either small inconsistencies or discontinuities in the objective function and the constraint functions which would otherwise prevent the optimizer from reaching the optimum design. This was accomplished during data input by changing the normalized finite difference step from 0.01 to about 0.1. Increasing the finite difference is not without its drawbacks. As the optimum objective value is approached, the optimizer overlooks the subtle effects of small changes in the design variables because of the relatively large perturbations. Thus, depending on the initial design variables, the optimizer will improve the design to some point near, but necessarily not at, the optimum.

When a design becomes feasible, steam exit-fraction will always become an active constraint. But the stated goal is not in achieving a feasible design but in driving the design to a feasible optimum. However, this iterative process can not be accomplished at the expense of violating a constraint and it was here that further complication was introduced. The initial impetus in any optimization process is to first obtain a feasible design. However, once the very small steam exit-fractions are obtained that are necessary for a feasible design, the exit-fraction becomes extremely sensitive to any further design variable changes. Thus any effort to further improve the current design could easily cause exit fraction to increase. Even slight increases would be perceived as violations of the constraint limit and thus prevent further optimization from the first feasible design. There are two possible solutions to this problem. Either increase the upper limit on the exit-fraction constraint or redefine the constraint. COPES formulates the general constraint function in such a way as to allow the user to increase the active region about the constraint limit. This is accomplished here by increasing the normalization factor in the following expression for the exit-fraction constraint function:

$$\frac{BU - EXITFR}{SCAL} \leq 0.$$

where BU is the upper constraint bound, EXITFR is the exit-fraction constraint value and SCAL is the normalization factor for this constraint. Increasing the normalization factor reduces the optimizer's sensitivity to constraint violations by enlarging the range of constraint values in which the constraint is active. This enlarges the region of feasibility and allows the optimizer more flexibility in altering design variables by reducing the risk of violating

the constraint. The overall effect is that the design optimization can continue but at the expense of accurate constraint limits. The normalization factor used effectively for the exit-fraction in CONDIP analysis was approximately 0.1.

One of the stated objectives was to create a robust program which would consistently yield the single best optimum design independent of the initial design and not get hung up on a relative optimum. As it was explained earlier, although relative optimums represented design improvement, they also indicated the inability of the optimizer to locate the single best or true optimum design. However, the objective was achieved for only three design variables. When more than three design variables were used, the optimum designs became loosely dependent on the initial input, although not in any predictable way. This is not to say that the condenser design did not optimize. By incorporating the finite difference and scaling normalization on exit-fraction as described above, final designs did yield objective function values which were continually within about ten percent of the true optimum regardless of the initial design. However, there was just no guarantee that the single, best optimum design could be consistently obtained. In summary, the reasons why CONDIP did not consistently optimize to the single, true optimum were: the extreme non-linearity of the steam exit-fraction, the need for a large finite difference gradient, and the need for a normalization factor for the exit-fraction upper limit constraint.

While the optimum design solutions obtained from CONDIP may be sufficient, there are several ways to improve the results and increase the chances of obtaining the best possible design. The easiest way is to try several initial input values until the user is satisfied that the best solution has been obtained. The problem with this approach is

that it is both costly and time consuming. A second recommendation is to couple an extremely simplified version of the condenser analysis with the optimizer to obtain a educated guess as to what the optimum design should be. The results of this analysis could then be used as input for CONDIP. OP CODE1, which utilizes the HEI methods in its analysis, is a likely candidate. The advantage of this approach is that a quicker, cheaper analysis can be used to obtain a rough idea of the anticipated optimum design. CONDIP can then use these design results to obtain even better and more accurate solutions, faster. There is still no guarantee, however, that the true optimum will be solved. Perhaps with the development of more robust and versatile optimizers, ones which uses numerical techniques and methods that are better suited to this type of problem than CONMIN, more precise solutions can be obtained. However, there is little more that can be done to simplify the analysis of the steam exit-fraction and subsequently linearize the problem.

IV. DESCRIPTION OF THE MAIN AND SUPPORTING SUBROUTINES

A. MAJOR SUBROUTINES

The following section contains a brief description of the major subroutines in CONDIP. The appropriate flow diagrams are also provided to better illustrate and complement the explanations. For further information concerning the various subroutines and functions see the CONDIP listing in Appendix C and ORCON1 [Ref. 2].

1. ANALIZ

This subroutine basically arranges CONDIP in a standardized form which is compatible with COPES/CONMIN. COPES uses a variable flag, ICALC, to coordinate the optimization process with ANALIZ. Utilizing this flag ANALIZ then calls the input, analysis and output portions of CONDIP as required. When COPES sets ICALC equal to one ANALIZ reads in all initial input. This is the only time any input can be entered. When ICALC equals two, COPES works with CONMIN to optimize the design. ANALIZ makes available the analysis portion of the program to be used repeatedly by CONMIN. When COPES sets ICALC equal to three, the optimization is complete and ANALIZ calls all applicable output subroutines. Figure 4.1 illustrates the flow process for ANALIZ.

2. INPUT

This subroutine enters all initial input of data by which the initial design is determined. The resultant design may be either feasible or infeasible, subject to the limitations previously discussed, so it is not critical what values are initially assigned to the design variables.

However, the initial input is screened to prevent the introduction of totally unrealistic values of variables into the program. For example, initial tube thickness, tube inner diameter, tube number and tube length are all checked to ensure that their values are greater than zero. If any of the screened initial inputs do not satisfy the minimum requirements, then the program exits prior to entry into the optimizer. The limits of the design variables and constraints will prevent similar situations from occurring during the analysis. Figure 4.2 presents the flow diagram for the INPUT subroutine.

3. OUT3

This subroutine simply prints all the initial values entered in the INPUT subroutine.

4. ORCON

This subroutine calculates the bundle geometry, flooding factors and such coolant flow parameters as pressure loss, flow rate, and pumping power. There are two options available to determine bundle geometry, each with certain advantages and disadvantages.

Option1: The number of rows is entered as a constant and the tube number is determined based on pitch, tube outer diameter, and row spacing. The advantage of this method to determine bundle geometry is that it allows the user to linearly vary pitch and/or tube inner diameter by row. The disadvantage is that tube number is a dependent variable. The optimizer is therefore limited in determining the optimum design by the specified number of rows.

Option2: The number of tubes can be used as a design variable while the number of rows is determined by tube number, row spacing, pitch and tube outer diameter. There

is more flexibility in this method of condenser design but it is not possible to linearly vary tube pitch and inner diameter. The condenser bundle is generated from a specified inner void out, and all the appropriate condenser geometry is determined for one of the identical 30 degree sectors. Overall bundle volume is then calculated as is the ratio of tube hole area to tube sheet area.

Once the basic condenser geometry has been determined, the code then proceeds through an algorithm to calculate baffle location based on an input value specifying the number of baffles desired in the condenser bundle. After this has been completed, flooding factors are determined. That is, the number of tubes in a vertical row above the central tube in each row is calculated. This is done for each of the six sectors on one side of a circular bundle. Symmetry is assumed for the other side. These flooding factors are later used in calculations to determine the effect of condensate inundation on shell-side heat transfer coefficients.

Finally, ORCON calculates coolant mass flow, coolant velocity, header pressure difference and pumping power based on the type of coolant flow input received. The flow chart in Figure 4.3 is a simple illustration of the logic used in ORCON. From ORCON, the subroutine SECALC is called.

5. SECALC

This subroutine determines all the parameters of each of the sectors in the condenser by row. The first calculation made in SECALC is the determination of the cooler geometry, if there is one. Entrance pressure losses into the condenser bundle are calculated for each sector and saturation pressure is checked to ensure that it is greater than PTLIN. From this point, much of the remaining

subroutine is comprised of two do-loops with one nested inside the other. The outer loop cycles through however many sectors are in the condenser model. The inner loop cycles through the rows in the sectors. Pressure, temperature, mixture velocity, steam flow and condensate flow are calculated at each sector row. The subroutine HETTRN is called repeatedly to provide the necessary heat transfer information. Pressure and steam flow is checked continually at each row to ensure that neither falls below its predetermined lower limits. In the event that either situation occurs, the appropriate penalty function and fix-up procedure is implemented to enable the analysis to continue. As previously discussed, these values are chosen to reflect as accurately as possible real conditions which would occur when steam flow or pressure violate their physical limits.

Once all the sectors have been analyzed the cumulative steam-side pressure losses from each sector are compared. Steam pressure at the inner void must be uniform, therefore the sector pressure losses are required to be equal within some allowable tolerance. If they are not, then the distribution of inlet steam flow into each sector is altered to force the pressure losses to converge to a single value. Once steam flow to the sectors has been adjusted, the sector and row analysis in SECALC is repeated until the pressure losses within each sector approach a common value. After the pressure comparison has been satisfied, certain overall condenser parameters are calculated such as steam exit-fraction, bundle heat load, and steam-side pressure drops.

Finally, if a cooler is required, the subroutine COOLEX is called. Otherwise the condenser analysis is complete. The flow diagram for SECALC is presented in Figure 4.4.

6. HETTRN

This subroutine is called repeatedly in SECALC to solve for all shell and tube-side heat transfer properties for each row in each sector of the condenser. In particular, values for the overall heat transfer coefficient and log mean temperature difference are utilized by SECALC in computing condensate production and heat transfer rate at each row of tubes.

On entering this subroutine, a series of estimates for certain row variables are calculated. Based on an assumed initial value for the overall heat transfer coefficient, the exit coolant temperature and corresponding film temperature are calculated. Utilizing these temperatures, the LMTD, thermal resistances, individual heat transfer coefficients and numerous other heat transfer parameters are then calculated. Finally, another value for the overall heat transfer coefficient is determined based on the above-mentioned analysis, and this final value is subsequently compared to the initial value. If they are not in agreement, within a specified degree of tolerance, then the initial value for the overall heat transfer coefficient is updated and the entire process is repeated until the initial and final values converge. This iterative process is necessary as temperature dependent heat transfer coefficients, film temperature drops, and exit coolant temperatures are all being calculated simultaneously.

Note that it is in HETTRN that the concepts of vapor shear and condensate inundation are incorporated. Heat transfer coefficients are corrected for both effects based on the calculations presented earlier. Also note that since steam temperature is never allowed to drop below inlet coolant temperature in the calling subroutine SECALC, resultant LMTD calculations in HETTRN will not yield singularities.

Once all the heat transfer variables have been determined, control is returned to SECALC where the appropriate results are utilized and stored. The appropriate flow diagram for HETTRN presented in Figure 4.5.

7. COOLEX

This subroutine solves for all the necessary parameters required in the cooler analysis. The cooler is assumed to be of rectangular cross-section with the height of the cooler not to exceed the difference between the condenser inner and outer radii. The values used for tube pitch and tube diameters in the cooler are the same as the innermost row of the condenser bundle.

Steam exits the condenser bundle, collects in the inner void and enters the bottom row of the cooler. The steam then proceeds vertically up through the cooler. The physical location of the cooler is not a prerequisite to the subsequent design, although it is expected that the cooler will be placed within the condenser bundle, thus the limit on cooler height.

The first calculation in COOLEX determines the steam velocity at minimum cross-section in the first row of tubes, VLCMAX. VLCMAX is directly proportional to the amount of steam and non-condensable gas entering the cooler as well as the cooler geometry. Therefore the constrained limits for VLCMAX will play a major factor in the overall condenser design.

Subsequent row analysis is treated identically as in SECALC. However, all pertinent heat transfer data are calculated directly within COOLEX, making it independent of HETTRN. Steam pressure and steam flow are checked at each row to ensure that the appropriate limits are not violated and all thermodynamic parameters are calculated. At the conclusion of COOLEX, cooler performance variables such as

heat load, exit-fraction steam, steam pressure losses and overall heat transfer coefficients are calculated and control is returned to SECALC. The flow diagram for the COOLEX subroutine is illustrated in Figure 4.6.

8. OUT2

This subroutine prints the overall condenser bundle results including heat load, steam exit-fraction, overall heat transfer coefficient, overall condenser LMTD and bundle volume. Normally, OUT2 is called once after the initial design is analyzed and again after the optimum design has been determined. Final design variable values such as tube number, coolant flow, tube pitch, tube wall thickness and tube inner diameter are also printed.

9. OUT2C

This subroutine prints the cooler results as well as the combined cooler/condenser results. This subroutine is called from the subroutine OUT2 and is called only if a cooler is required and subsequently designed. Therefore, these results will always be printed in conjunction with OUT2 output.

10. OUT3

This subroutine prints a very detailed output of the condenser and cooler results by row and sector. Nearly all the thermodynamic and heat transfer properties are presented, thus providing a rather complete picture of conditions everywhere in the condenser. This is extremely helpful in determining, for example, where additional heat transfer enhancement would be most beneficial, or where baffles should be best located to reduce the effects of condensate inundation.

B. SUPPORTING SUBROUTINES

The following is a brief description of supporting functions and subroutines called frequently by the main subroutines.

1. DPSVTY: This subroutine returns the value of the mutual diffusivity of the steam and non-condensable gas present.
2. ITR: This function subroutine transforms the calculated data, received in the argument list, to the log values and performs a linear regression on two or more points using the model.
3. AMUFN: This function subroutine calculates the viscosity of the non-condensable gas in $\text{lbm}/(\text{ft-sec})$.
4. BMUFN: This function subroutine calculates the viscosity of a saline solution in the range of 0-24 percent concentration and temperatures of 40-210 °F in $\text{lbm}/(\text{hr-ft})$.
5. CPAFN: This function subroutine returns a value for the heat capacity of the inert, non-condensable gas mixed in with the steam in units of $\text{Btu}/(\text{lbm-mol-}^\circ\text{F})$.
6. CPFN: This function subroutine calculates the specific heat of a saline solution units of $\text{Btu}/(\text{lbm-}^\circ\text{F})$.
7. CPSPN: This function subroutine calculates the heat capacity of steam in $\text{Btu}/(\text{lbm-mol-}^\circ\text{F})$.
8. HGPFN: This function subroutine returns a value for the latent heat of vaporization of water in Btu/lbm .
9. PRSDRP: This subroutine returns the shell-side pressure drop across a row of tubes in psia .
10. PSATFN: This function subroutine calculates saturation

pressure of steam as function of temperature. Pressure is returned in units of psia.

11. ROEFN: This function subroutine calculates the density of a saline solution of concentration range 0-24 percent and temperature range of 40-300 °F. Density is returned in units of lbm/(cu.ft.).

12. SKBFN: This function subroutine calculates the thermal conductivity of a saline solution of concentration range 0-24 percent and a temperature range of 40-300 °F. Thermal conductivity is in (Btu)/(hr-f-°F).

13. TSATFN: This function subroutine returns the value for steam temperature in °R given a pressure in psia.

14. VGFN: This function subroutine calculates the specific volume of steam as a function of temperature and pressure. It has units of (cu.ft.)/lbm.

15. SWTCH: This function subroutine reverses the order of a stored array.

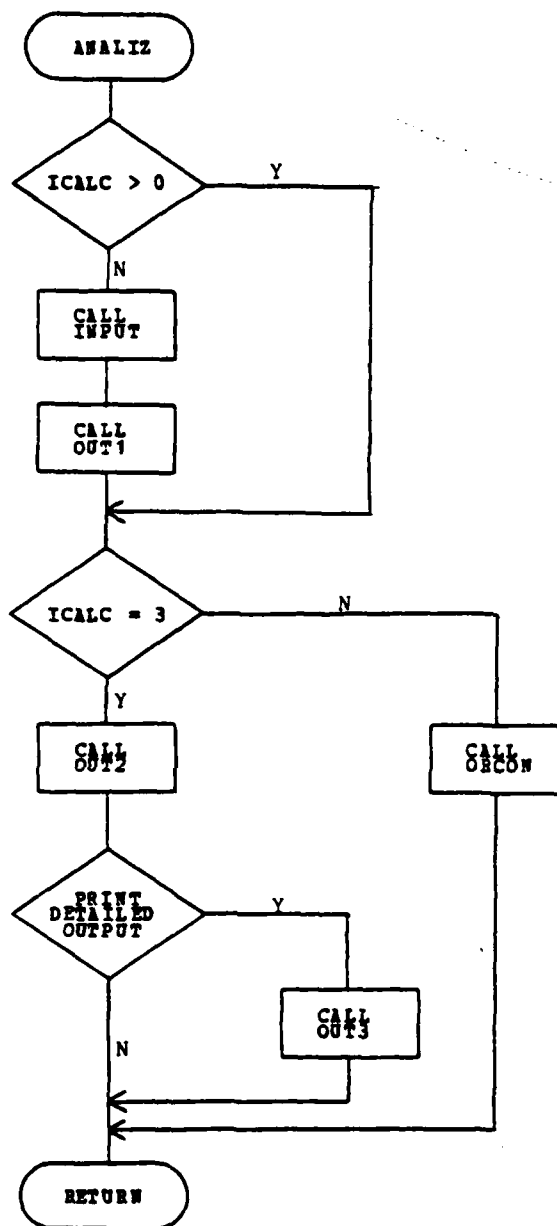


Figure 4.1 Flow Diagram for the ANALIZ Subroutine.

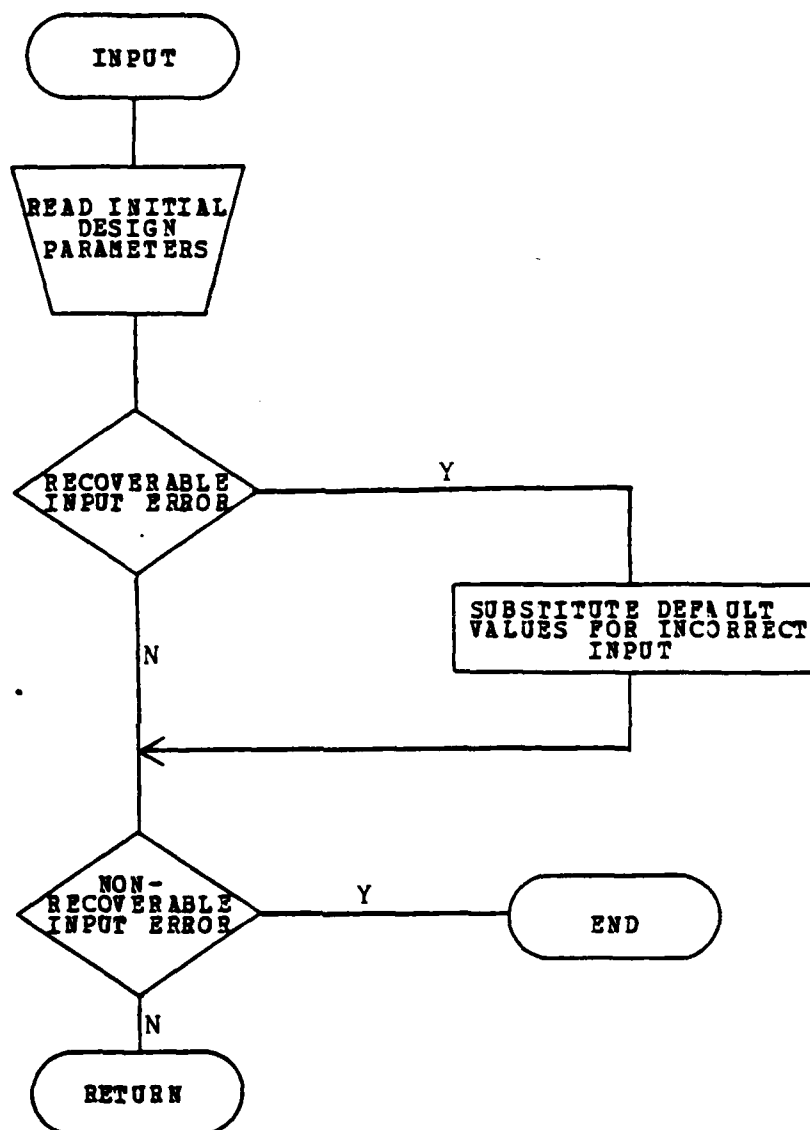


Figure 4.2 Flow Diagram for the INPUT Subroutine.

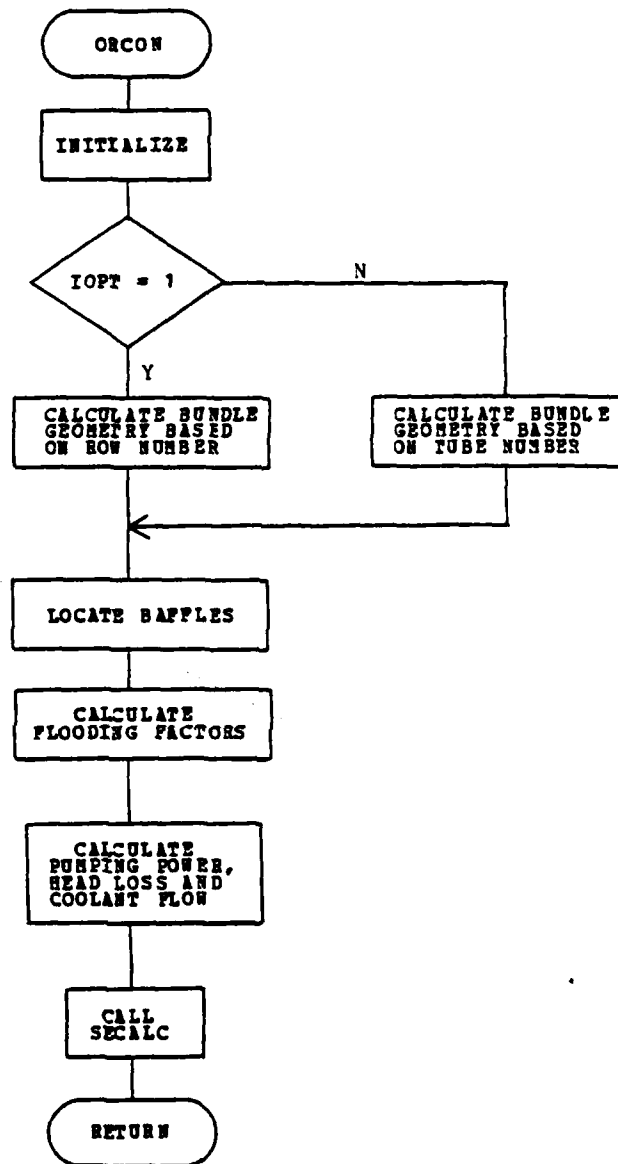


Figure 4.3 Flow Diagram for the ORCON Subroutine.

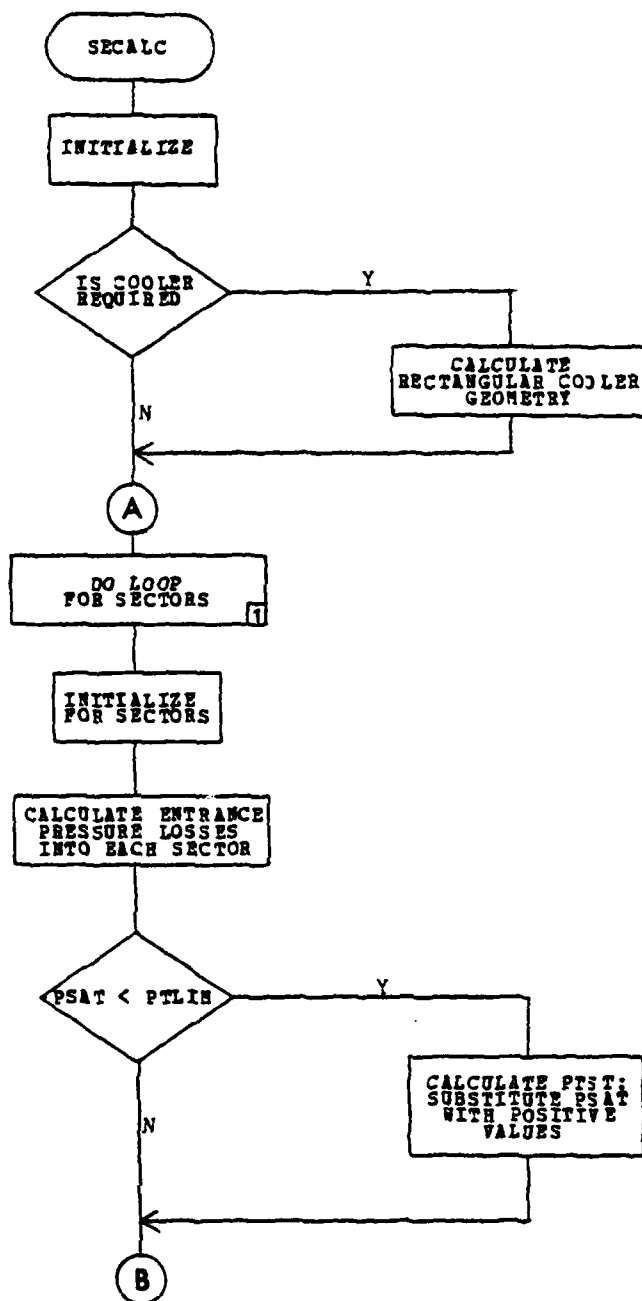
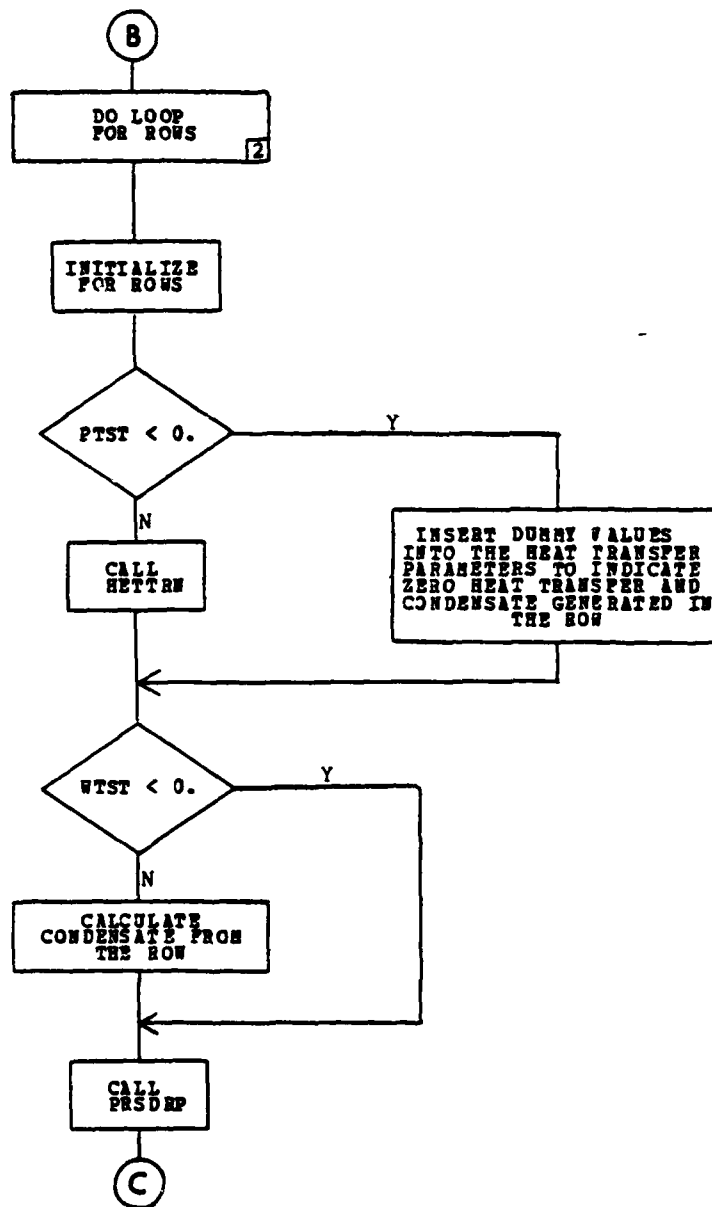
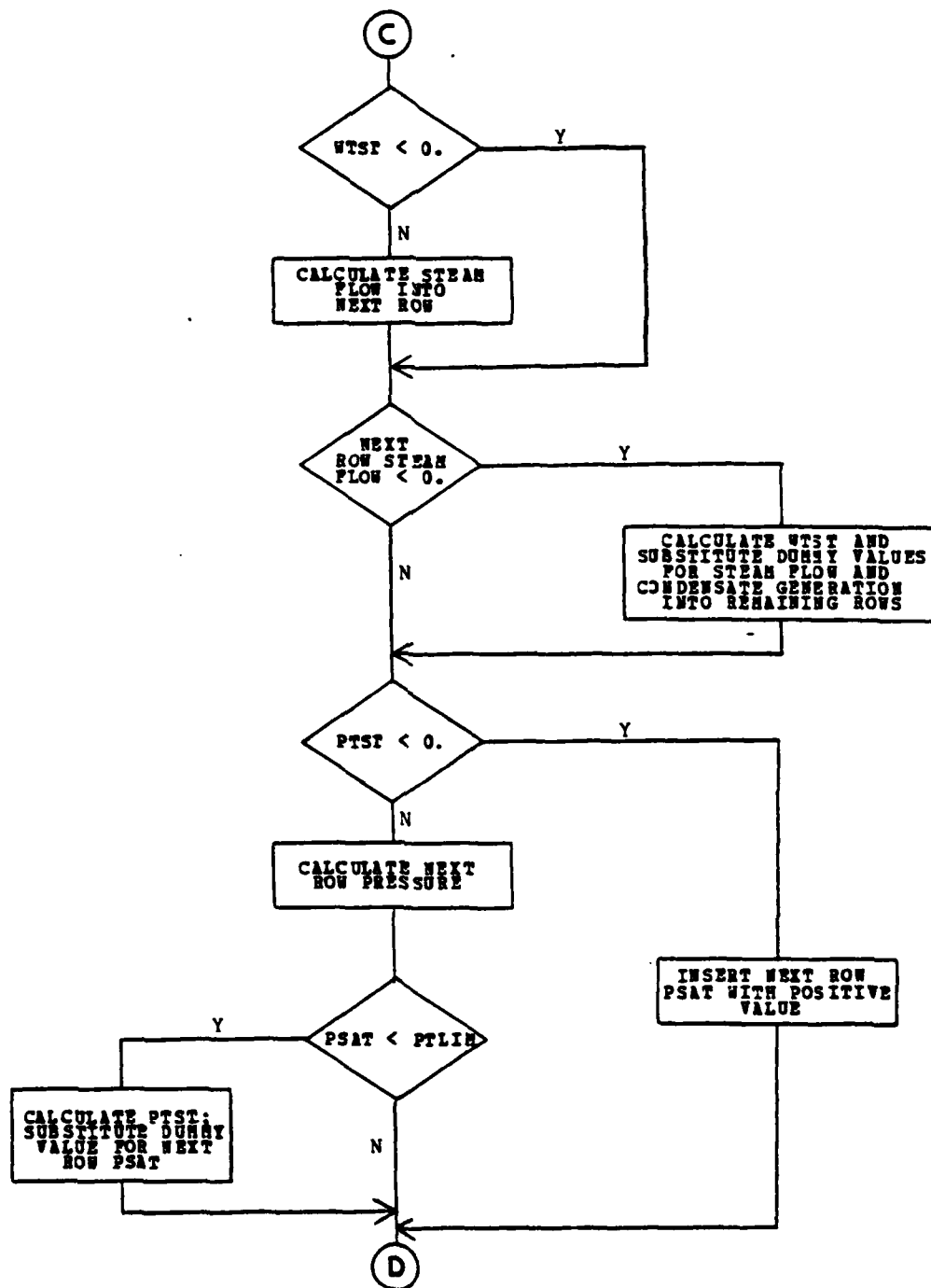


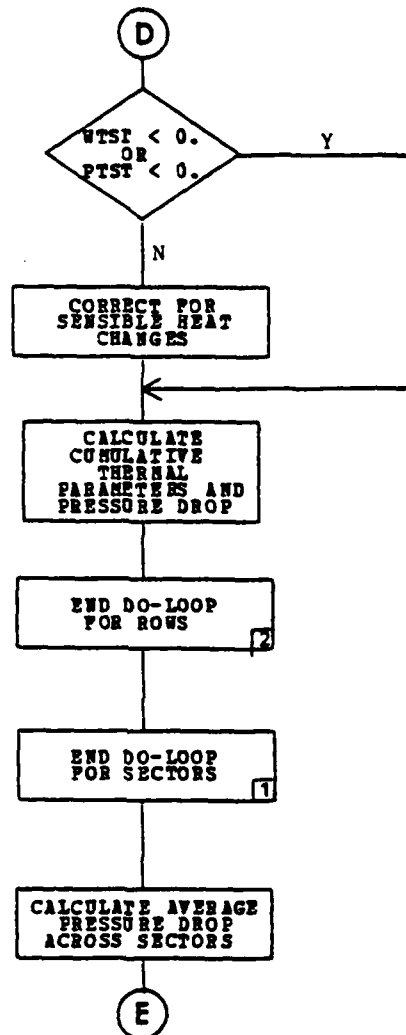
Figure 4.4 Flow Diagram for the SECALC Subroutine.



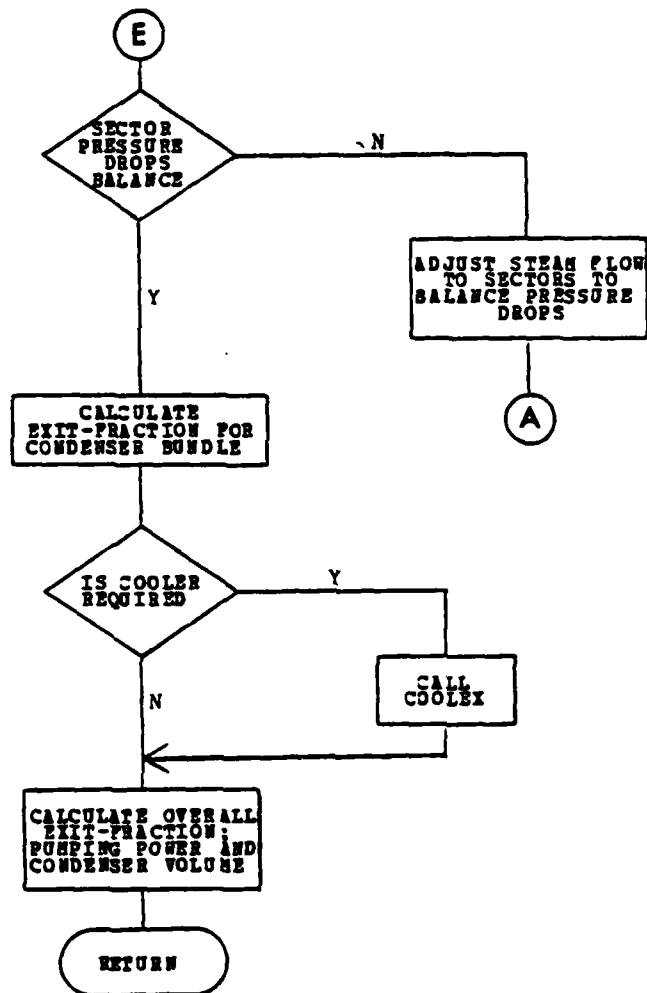
SECALC Flow Diagram (continued)



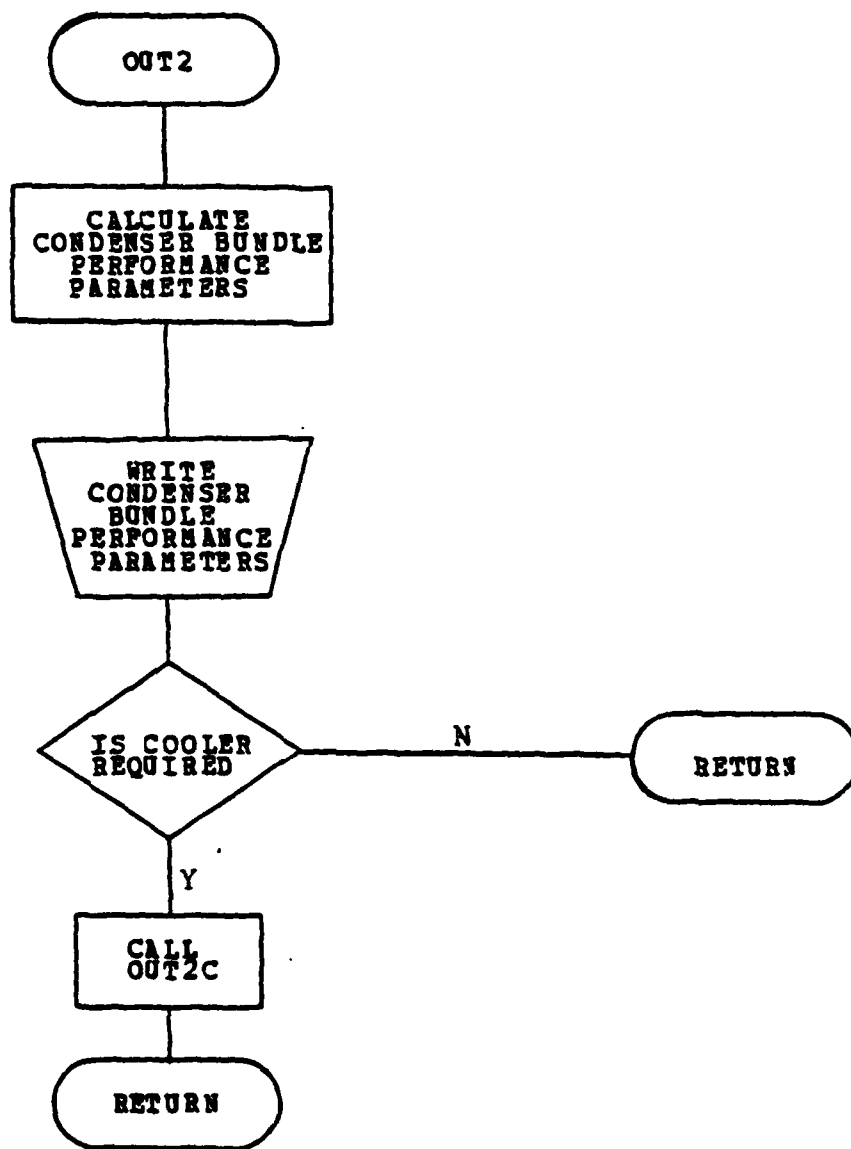
SECALC Flow Diagram (continued)



SECALC Flow Diagram (continued)



SECALC Flow Diagram (continued)



Flow Diagram for the OUT2 Subroutine

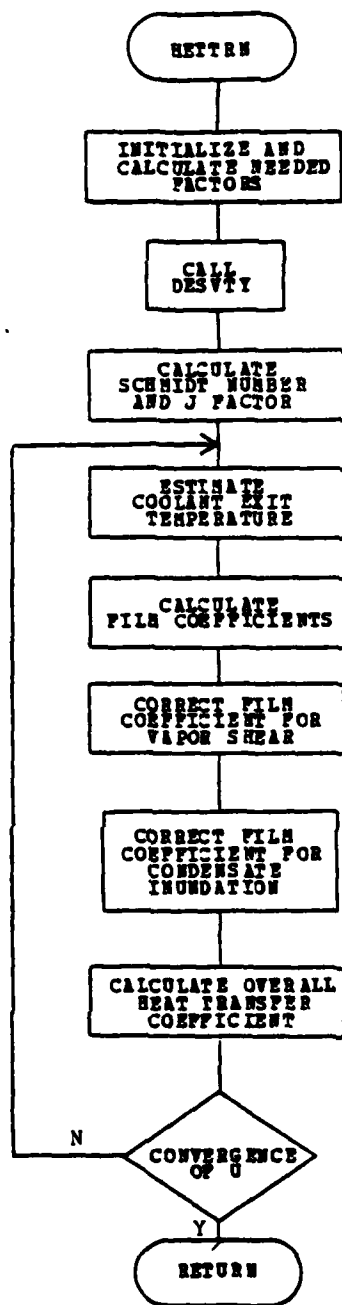


Figure 4.5 Flow Diagram for the HETTRN Subroutine.

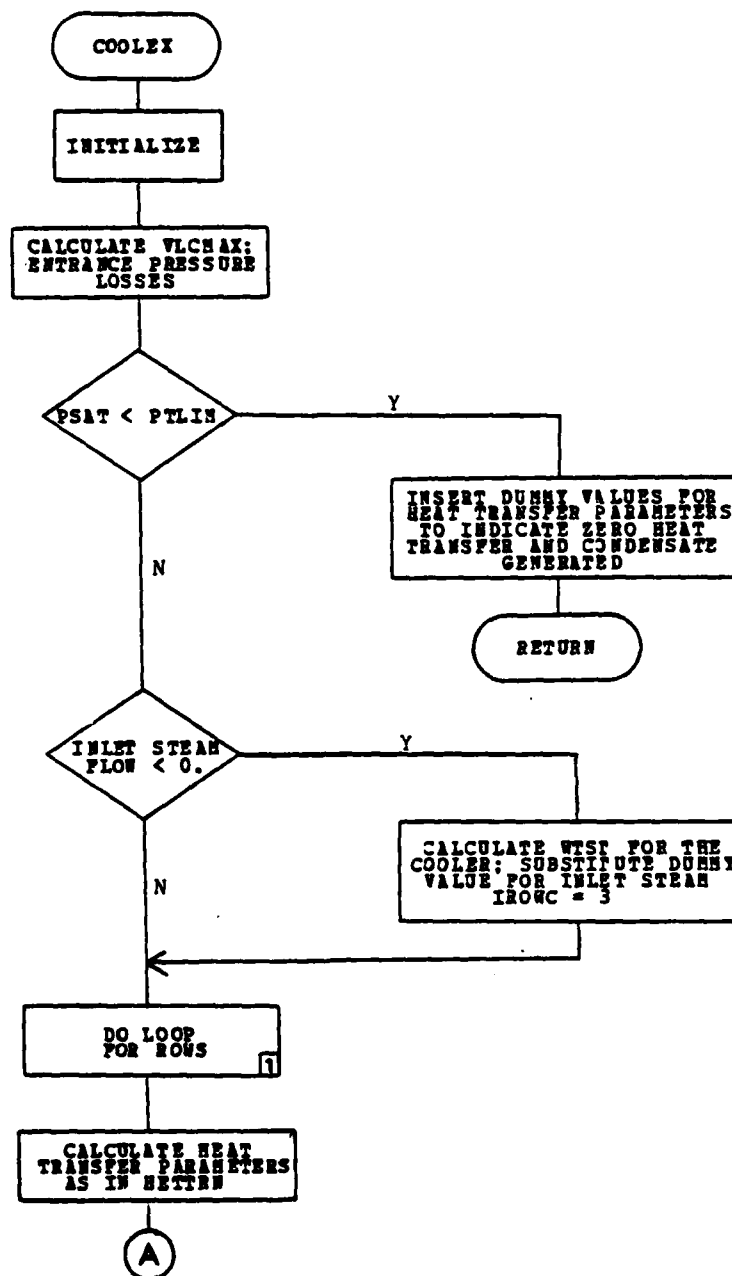
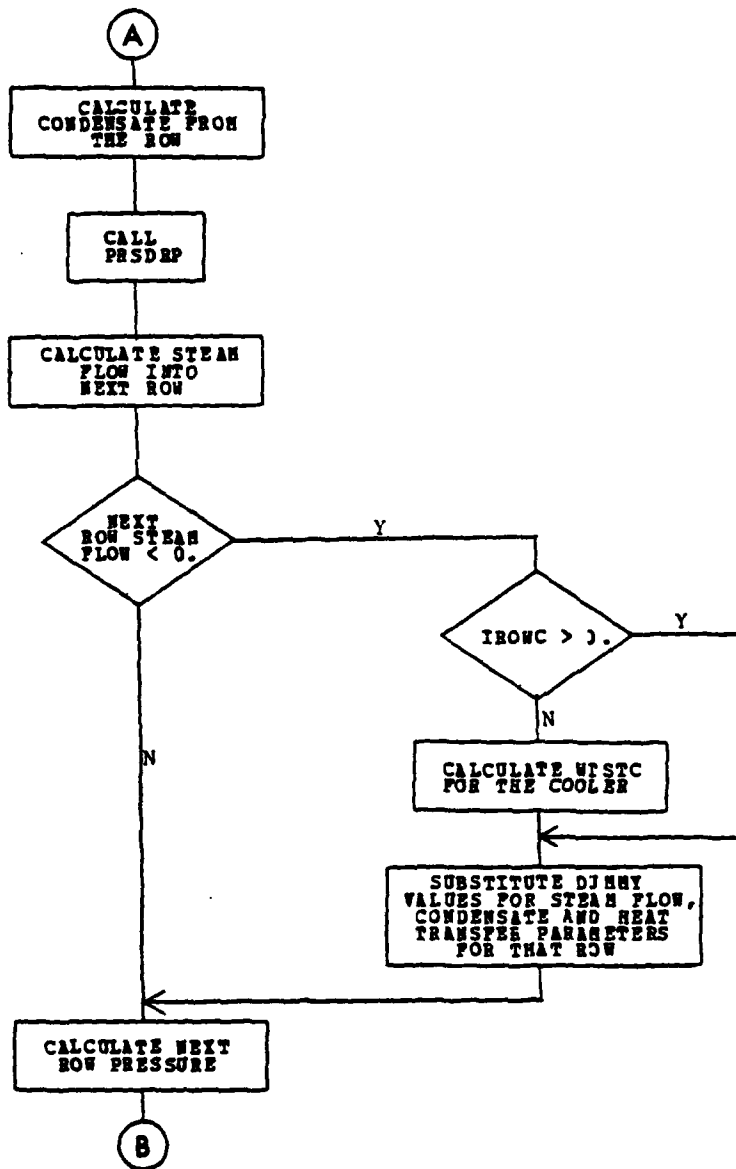
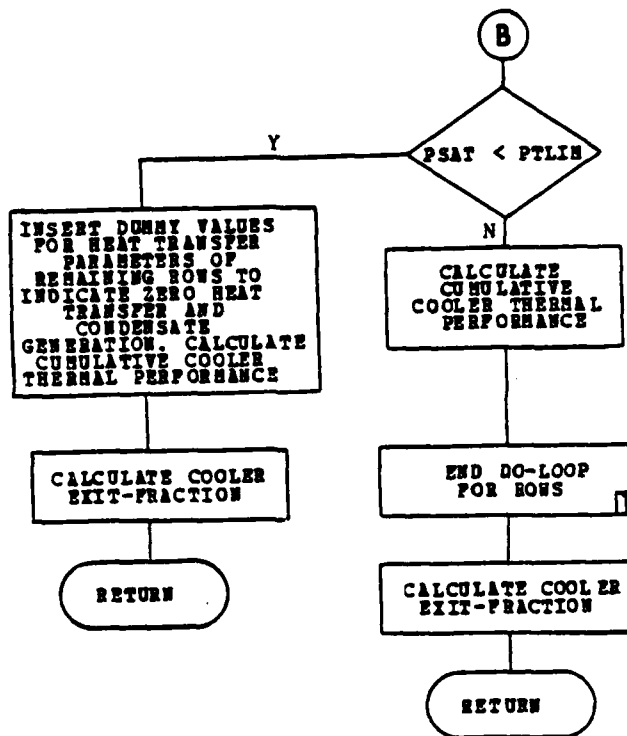


Figure 4.6 Flow Diagram for the COOLEX Subroutine.



COOLEX Flow Diagram (continued)



COOLEX Flow Diagram (continued)

V. RESULTS

A. CONDIP VERIFICATION

It was desirable to verify the single pass capability of CONDIP (i.e. without optimization) as a predictor of condenser performance by comparison with actual experimental data. However, complete and accurate data on condenser design and corresponding performance is not always readily available. Lynch [Ref. 18] encountered this same problem in attempting to verify ORCON1. However, he did manage to locate some actual experimental condenser data, obtained during a test conducted to determine the general performance of the DDG-37 class propulsion machinery [Ref. 16]. The test took place at the Naval Boiler and Turbine Laboratory and was conducted primarily to determine the performance of the turbine and reduction gears. Some limited condenser data was taken as a by-product. The various measurements were obtained as described below:

1. Steam flow measurements were made by weighing the condensate.
2. Cooling water inlet and outlet temperatures were measured by thermometers installed in the inlet and discharge lines.
3. The heat load is calculated based on total steam flow into the condenser multiplied by the difference between inlet steam and condensate enthalpies.
4. Circulating water flow was determined from a heat balance around the condenser. The total heat load was divided by the circulating water heat capacity and temperature rise to obtain flow rate.

5. Condenser inlet pressure was determined by pressure instruments located above the condenser inlet flanges.

6. Non-condensable gas flow was measured by a flowrator.

7. Pressure at the air ejector was measured directly. This pressure and the inlet pressure determined the pressure drop across the condenser.

It should be pointed out that this data were not recorded with the care that normally accompanies scientific data collection. Neither the instruments nor the techniques employed were particularly accurate. The possibility that this observed data are in error casts a cloud over the credibility of the corresponding condenser performance, which was calculated based on those values. However, for a lack of better alternatives, this data and the resulting condenser analysis will be used to determine the reliability of CONDIP.

The DDG-37 condenser geometric design variables obtained from the technical manual [Ref. 15] and input parameters corresponding to a full speed run are presented in Table I. An attempt was made to repeat the design using CONDIP. The results of CONDIP's proposed design as well as the experimental performance are presented for comparison in Table II. Percentages were calculated to quantify the differences between the actual and hypothetical performance.

Before elaborating on the results of this verification, some notable differences between the two designs must be clarified. First, a specific fouling factor was not determined at the time of the experiment and was therefore not provided. A somewhat realistic cleanliness factor of 87.5 percent (fouling factor of .0002) was utilized.

Second, in the DDG-37 condenser the rectangular cooler appears to be inserted directly into the condenser bundle.

However, in order to accomodate the cooler, the bundle must expand or distort. In addition, a void of some dimensions must be provided-for in the center of the bundle to collect any uncondensed steam and non-condensable gases. Diagrams in [Ref. 15] indicate that the DDG-37 condenser is indeed nearly elliptical in shape with bundle axes of 5.67 and 7.17 feet. Although it is apparent that a void does exist, exact dimensions can not be readily determined from the available information.

CONDIP approximates this design by creating separately a circular condenser bundle and a rectangular cooler, the height of which cannot exceed the difference between the outer and inner bundle radii. A circular void of pre-determined size is provided-for when determining the condenser bundle geometry. Subsequent volume calculations are performed on the condenser bundle and cooler separately and the overall condenser volume is computed as simply their sum.

Although CONDIP does not exactly duplicate the geometric configuration of the DDG-37 condenser, it was possible to manipulate certain initial design variables in order to cause CONDIP to develop an approximately equivalent configuration. These variables were chosen because, for small changes in their values, there is a rather significant change in the bundle geometry with relatively small effects on the overall condenser performance. Since there are no specific dimensions provided for the inner void in the DDG-37 technical manual, it was picked to be one of the design variables to be adjusted. Row spacing was also adjusted because it satisfied the conditions described above. Through trial and error a combination of row spacing and inner void radius were determined, from which CONDIP yielded a geometric design similar to the DDG-37 condenser and that satisfied condenser requirements specified in

[Ref. 17]. In this particular case, the void diameter and row spacing were determined to be 1.1 feet and 1.35 inches respectively. This arrangement enabled the condenser model to closely approximate the tube sheet area ratio of the actual DDG-37 condenser. This manipulation, however, must be interpreted as another source of error and innacuracy when comparing CONDIP's condenser performance with the experimental results.

Lastly, condenser designs in [Ref. 15] reveal that three different tube patterns were employed in the DDG-37 condenser. In addition, two different values for tube pitch were used - a pitch of 1.4 in the condenser bundle and a pitch of 1.3 in the cooler. This situation cannot be duplicated in CONDIP. Therefore a constant pitch of 1.40 and a uniform tube pattern were utilized throughout the condenser.

The design approximations utilized in CONDIP to try to geometrically simulate the actual DDG-37 condenser introduce significant uncertainty into subsequent design comparisons. This, coupled with the fact that the data collected is also suspect, would imply that it is rather difficult to verify CONDIP's analysis with the information available. It should also be noted that CONDIP is sensitive to even small variance in either the data collected (i.e. steam inlet temperature) or the approximated design variables. However, despite the above-mentioned problems associated with equating CONDIP's condenser to the DDG-37 condenser, the experimental data obtained from the DDG-37 condenser still provide the best available base upon which to make a reasonable determination of CONDIP's capabilities and limitations.

In comparing the results in Table II, it is immediately clear that there is significant difference between certain condenser performance parameters predicted by CONDIP and the corresponding experimentally derived condenser performance. Already, much has been said about the numerous geometric

approximations used to model the DDG-37 condenser. But questionable data and geometric manipulations may not completely explain the 13 percent exit-fraction and general poor performance generated in CONDIP's analysis. Its values for the average overall heat transfer coefficient and heat rejected were significantly lower than the experimental results. One source of the problem lies in the actual heat transfer analysis performed in the code. Lynch [Ref. 18] graphically illustrated how sensitive this analysis is to the effects of condensate inundation. In particular, by making small changes - within the allowable ranges - in the constants used in Eissenberg's correlations for condensate rain, significant improvement could be realized in the overall heat transfer characteristics of the condenser. CONDIP's results, when compared to the experimental data support the argument that the values currently used in the inundation correlations are rather conservative in nature, and cause the overall analysis to yield a poor performance for the given steam load and condenser design.

Therefore, in order to present CONDIP with a fair test to determine its credibility as a design predictor, some additional work must be first accomplished. A condenser geometrically identical to the general model created in CONDIP should be constructed with complete and accurate data acquisition systems to establish a thorough data base from which to compare. Also, more research should be performed on the effects of condensate inundation and velocity shear to obtain more precise correlations in determining their overall effects on the film heat transfer coefficients.

One last additional point should be mentioned. In comparing the steam-side pressure drops through the condenser, it was shown that CONDIP's pressure losses were nearly 72 percent larger than the actual physical measurements. However this radical difference is mainly due to the

high pressure losses experienced at the entrance of the cooler as a large volume of steam tried to force its way through the small available area. Therefore, the significance of this large disagreement in results is relatively minor and can be treated simply as a consequence of the more important heat transfer limitations in the comparison run.

Although the goal of verifying CONDIP as a design predictor has proven elusive, it was still possible to demonstrate its capabilities through comparison studies. Therefore, the remaining emphasis in this thesis is to show the ability of CONDIP (in combination with the optimizer COPES/CONMIN) to take an initial design with a given framework of constraints and design variables, and obtain better designs based on a desired objective function.

B. EXPLANATION OF THE CASE STUDIES

The following case studies were devised to best exercise the capabilities of CONDIP. They were made as realistic as possible so as to simulate the problem of condenser design and specification confronting the engineer during the early stages of power plant design. The condenser performance returned by CONDIP during the verification run and contained in Table II will serve as a baseline for comparing the results of each case study. The baseline condenser performance is based on the design parameters from the DDG-37 condenser listed in Table I. It was stated earlier that CONDIP's optimization results are slightly sensitive to the initial design if more than three design variables are used. Since all the cases involve eight or more design variables it would be best, for the purposes of comparison, to start from the same initial design in all cases. Therefore, the initial design variables used for the verification run and contained in Table I will be utilized as the baseline

design. Although many of these initial design variables will be allowed to change during optimization, certain basic condenser requirements will not. They include: steam flow into the condenser, inlet steam saturation pressure and temperature, cooling water injection temperature, the fraction of non-condensable gases in the steam, the tube fouling factor, and the tube material. It should be noted that although there was an initial value for row spacing given in Table I, row spacing was not used as a design variable during any of the optimizations. Instead, the program used the default method of row spacing calculation available in the code where the rows are spaced such that a 60-degree equilateral triangle pattern of concentric rows is obtained. Row spacing is therefore dependent on tube pitch and tube outer diameter by the following relation:

$$RSPA = (SDDO * ODOI) * .866 \quad (\text{eqn } 5.1)$$

where RSPA is row spacing, SDDO is tube pitch, and ODOI is tube outer diameter in inches.

There are a few key points to be kept in mind when comparing the results of the case studies with the baseline. First, the baseline design is an infeasible and inadequate design. Its performance indicates that it is not capable of supporting the required steam load by returning a steam exit-fraction in excess of 13 percent. So any gains in the objective function that were realized in the case studies is even more remarkable since it is a necessary condition that the optimum design be a feasible design, defined as having an exit-fraction not greater than 1 percent. Second, the percent change referred to when analyzing the results is calculated based on the baseline design. Thus the baseline serves as a uniform frame of reference. Next, it should be noted that because of the large number of design variables

and constraints, intuition on how an optimized result will turn out is not always applicable. Finally, it will be easier to understand the effects of the various design parameters by keeping in mind the following, very basic, heat transfer correlation:

$$Q = U * A * LMTD \quad \text{(eqn 5.2)}$$

where Q is the rate of heat released as the steam condenses; U is the overall heat transfer coefficient; A is the heat transfer surface area; and $LMTD$ can be interpreted as the thermal driving force between the steam and the coolant. Q is directly dependent on steam flow and pressure into the condenser, the percentage of that steam that is condensed, and any subcooling of the condensate. For a given steam load and a very small exit-fraction Q is nearly constant as the optimized results in all the case studies will indicate.

1. Constraint Framework for CONDIP

In order to simulate an actual trade-off study, the constraints and their respective limits were kept constant for all the case studies. The condenser was to be designed with a maximum bundle diameter of ten feet, a maximum and minimum tube outer diameter of 0.625 and 1.25 inches respectively, a steam exit-fraction of not more than 1 percent, a maximum cooler inlet velocity ($VLCMAX$) of 200 feet/second, and a ratio of tube sheet hole area to total tube sheet area of less than 0.30.

The constraint on bundle diameter was chosen somewhat arbitrarily. It seems unlikely that this limit would be realistically exceeded, although certainly space requirements would dictate the exact configuration. Tube outer diameter is dependent on the values for tube wall thickness and tube inner diameter. Thus the limits imposed on tube

outer diameter represent realistic restrictions on the possible combinations of inner diameter and wall thickness. These restrictions are based loosely on anticipated tube structural and strength requirements and correspond to values of normally available tubes [Ref. 19]. The maximum limit of 200 feet/second for VLCHMAX was also a somewhat arbitrary but realistic limit. It is assumed that steam velocities often exceed that value in the condenser bundle.

It is recalled that steam exit-fraction will play a significant role in the determination of the final optimum design. The baseline exit-fraction of 13 percent predicted by CONDIP for the DDG-37 condenser is unsatisfactory. Therefore a more reasonable upper limit of 1 percent was placed on this constraint. Although CONDIP will return a much more conservative design if 1 percent vice 13 percent is used as the upper limit, the subsequent design will be much more credible.

Finally, the amount of tube sheet material that can be removed by drilling for the installation of condenser tubes is specified at 24 percent of the total tube sheet area in [Ref. 17]. This area ratio limit represents a structural limit imposed to ensure that the tube sheets do not fail due to heat and pressure stresses in the condenser. However, CONDIP does not take into account the space between the condenser and tube shell normally used in area ratio calculations as blank tube sheet area. For this reason and to allow more flexibility in the design analysis, the constraint limit was set at 30 percent.

In summary, the general design constraints and the associated upper and lower bounds were:

$$0.625 \leq \text{tube outer diameter (inch)} \leq 1.25$$

$$1.0 \leq \text{bundle diameter (feet)} \leq 10.0$$

$$\text{steam exit-fraction (\%)} \leq 1.0$$

$$\text{VLCHMAX (ft/sec)} \leq 200.0$$

$$\text{area ratio} \leq .30$$

These design constraints and associated bounds were used in all the case studies except where specifically modified.

2. Design Variable Framework for CONDIP

At least eight design variables were used in all the case studies. They include tube inner diameter, tube wall thickness, tube pitch, the number of tubes in the condenser, tube length, the inner void radius, the percent of the tubes in the cooler, and cooling water velocity. Side constraints were placed on all of these variables to correspond to either realistic physical limits or available standardized materials.

Tube wall thickness was not allowed to fall below 0.022 inches (BWG 24) or exceed .109 inches (12 BWG), sizes normally available commercially. Tube inner diameter was restricted to values between .407 and 1.206 inches so as to yield tube outer diameters within the limits specified earlier.

Tube pitch is defined as the ratio of the center to center spacing between adjacent tubes in a row to the tube outer diameter. Tube pitch is an accurate measure of how closely packed the tube bundle is. Generally accepted values for pitch lie in the range of 1.3 to 1.7. However, to provide more latitude in the design process this design variable was allowed to vary in the range between 1.1 to 2.0.

There is no guidance available as to the allowable range for tube length in the condenser. Since the lower limit was not expected to be crucial, it was set randomly at 1.0 feet. The upper limit of 25.0 feet was a realistic limit considering the size of the tube diameter being worked with. Inner void radius and the percent of tubes in the cooler were chosen to be design variables simply to enhance the

flexibility of the code in designing the condenser model. The bounds for both variables were entirely arbitrary with only common sense as the determining factor. The upper and lower limits on the percent of tubes in the cooler was established as 10.0 and 2.0 percent respectively. The upper and lower bounds on the inner void radius was set at 1.0 and 0.1 feet.

Cooling water velocity generally ranges from three to nine feet per second in value for all common tube materials, except titanium which has an upper limit of 15 feet per second. Exceeding these upper limits risks excessive tube erosion and material damage. Finally the number of tubes was permitted to vary between 1000 and 8000 tubes for the purpose of improving design flexibility. It is extremely unlikely that, for most propulsion applications, tube number would fall below 1000. The upper limit was simply chosen as a realistic cutoff point in terms of complexity, cost and maintainability.

In summary, the general design variables and the associated side-constraints were:

$$0.407 \leq \text{tube inner diameter (inches)} \leq 1.206$$

$$0.022 \leq \text{tube thickness (inches)} \leq 0.109$$

$$2.0 \leq \text{percent of tubes in cooler} \leq 10.0$$

$$0.10 \leq \text{inner void radius (feet)} \leq 1.0$$

$$3.0 \leq \text{coolant velocity (ft/sec)} \leq 9.0$$

$$1.0 \leq \text{tube length (feet)} \leq 25.0$$

$$1000 \leq \text{tube number} \leq 8000$$

$$1.1 \leq \text{tube pitch} \leq 2.0$$

As in the case of design constraints, these design variables and their respective limits were used consistently in all the case studies unless otherwise specified.

C. CASE STUDIES USING CONDIP

1. Case One

The objective of this case was to minimize condenser volume. The final results of the optimization along with the initial parameters is listed in Table III.

These results show a 16 percent decrease in condenser volume with a corresponding 24 percent increase in pumping power. The source of the improvement can be understood by noting the following:

- 1) Tube wall thickness was reduced from 0.049 to 0.022, the minimum side-constraint, thus allowing tube inner diameter to increase while maintaining a minimum tube outer diameter.

- 2) The number of tubes shrank slightly as did tube length, resulting in a smaller heat transfer surface area.

- 3) Tube pitch increased markedly, causing a reduction in steam pressure losses which then ensured that high values for steam saturation pressure and temperature would be maintained throughout the condenser. The large pitch also reduced steam velocities, allowing the cooler inlet velocity limit to be satisfied. Row spacing decreased from the initial value of 1.35 inches, thus decreasing condenser volume.

- 4) Cooling water velocity increased to the maximum allowable value of 9 ft/sec which correspondingly resulted in larger head losses and coolant flow, causing overall pumping power to increase.

As cooling water velocity increased and tube wall thickness decreased, then their respective thermal resistances were diminished. The cumulative effect was to improve the overall heat transfer coefficient. LMTD rose primarily as a result of the higher steam temperatures throughout the condenser. It is apparent by looking at equation 5.2 that increasing the driving forces for heat

transfer, such as the overall heat transfer coefficient and LMTD, allows the heat transfer surface area to decrease. This resulted in a similar reduction in condenser volume.

The constraint limits that prevented further design improvement were the upper bound on the cooling water velocity, the upper limit on the tube sheet area and the upper limit on VLCMAX.

2. Case Ivo

The objective of this case was to minimize the pumping power required to overcome the tube-side head losses and drive the cooling water through the condenser tubes. The final results of the optimization are presented along with the initial design in Table IV.

The results indicate a dramatic 90 percent reduction in required pumping power with an equally large 120 percent increase in condenser volume. The major factors involved in the design improvement along with their relative effects are briefly explained below:

- 1) Tube inner diameter increased 27 percent while tube thickness remained relatively unchanged. Thus tube outer diameter was caused to increase.

- 2) The number of tubes in the condenser rose significantly, along with tube length. This, coupled with the enlarged tube outer diameter resulted in nearly doubling the heat transfer area.

- 3) Tube pitch increased 29 percent, which allowed steam saturation pressure and temperature to be maintained at consistently large values in the condenser. This had a benefiting effect on the associated LMTD calculation. The large pitch also helped satisfy the steam velocity limit into the cooler. The tube spacing decreased from the initial value of 1.35, but by a smaller amount than the previous case because of the large values for tube pitch and outer diameter.

4) Cooling water velocity dropped to the minimum allowable limit of 3 ft/sec. This had the effect of reducing tube-side head losses and coolant flow through the condenser. Consequently, pumping power was drastically reduced.

The combined effect of all these changes can again be put in perspective by looking at equation 5.2. For the given steam and corresponding heat load, the heat transfer area increased drastically, allowing both LMTD and the overall heat transfer coefficient to decrease. A smaller overall heat transfer implies a smaller convective tube-side contribution which in turn permits coolant velocity to reduce to its lowest allowable value. The LMTD decrease is explained by the fact that cooling water was spending more time in the tubes, thus causing the average cooling water temperature to rise. However, the subsequent reduction in LMTD was minimized by the fact that a high steam temperature was maintained in the condenser.

There were no active constraints in this design outside of cooling water velocity which prevented further design improvement. However, the penalty paid in terms of a huge condenser volume, appears prohibitive.

3. Case Three

The objective of this case was to minimize pumping power while holding condenser volume constant at the initial value of 432 cubic feet. This was a particularly interesting test case as the results in Table V bear out. The required pumping power was reduced by nearly 38 percent with no change in volume. The effects of the design changes which resulted in the design improvement are presented below:

1) Tube inner diameter increased noticeably. However, the effects of this increase on tube outer diameter was minimized by a large drop in tube wall thickness. Thus, tube outer diameter remained relatively unchanged.

2) The number of tubes experienced a minor reduction, while tube length increased. The overall effect was to increase heat transfer surface area.

3) Tube pitch again rose by nearly 25 percent, causing steam saturation temperature and pressure to maintain a nearly constant value throughout the condenser. This had a beneficial effect on the LMTD between the steam and the cooling water. The larger pitch also had the additional effect of reducing steam velocity thus allowing the subsequent design to satisfy the upper limit on steam velocity into the cooler (VLCMAX). The combination of tube pitch and tube outer diameter resulted in a reduction in row spacing from the initial value of 1.35

4) Cooling water velocity decreased by about 21 percent. This effect was manifested in subsequent pressure head, coolant flow and pumping power calculations.

Looking at equation 5.2 we see the same general pattern emerging as in Case 3, but with more subtlety in the changes. Heat transfer increased, but not at the expense of volume. Cooling water velocity was allowed to decrease while the overall heat transfer coefficient actually rose. One explanation is that as the tube wall got thinner its thermal resistance got smaller which more than offset the loss of convective heat transfer contribution from the coolant. The LMTD dropped slightly due to the higher average coolant temperature of the coolant in the tubes.

The constraints which became active and prevented further improvement in the design include tube sheet area ratio as well as tube wall thickness. However, tube wall thickness was particularly crucial because of its related effect on heat transfer.

4. Case Four

The objective of this case was to minimize condenser volume while holding pumping power constant at the initial value of 55.7 horsepower. The results of this case can be found in Table VI. Chosen to contrast the results in Case 4, the relative improvement in this design objective was not nearly so impressive. Condenser volume shrank by only 12 percent. An explanation of the causes and effects is provided below:

1) Tube inner diameter increased, with a corresponding decrease in tube wall thickness to yield the minimum allowable tube outer diameter.

2) The number of tubes decreased noticeably, tending minimize bundle volume. Note, there was only slight increase in tube length. The overall effect was to similarly reduce heat transfer surface area as condenser volume decreased.

3) Tube pitch again increased significantly, having the same effects on steam pressure, temperature and steam velocity into the cooler as discussed earlier. A large tube pitch benefits the LMTD between the steam and the cooling water. Row spacing was again a factor in reducing condenser volume as before.

4) Cooling velocity decreased slightly as did head loss. But overall coolant flow increased due to an increase in tube inner diameter. The net effect was to maintain pumping power.

Again, referring to equation 5.2 , it is clear that the slight decrease in heat transfer area was offset by the slight rise in LMTD resulting from higher condenser steam temperatures. The significant improvement in overall heat transfer coefficient, therefore, is what makes the heat balance work. The large decrease in tube wall thickness and corresponding reduction in thermal resistance contributed heavily to this improvement.

There were several constraint limits which prevented any additional objective optimization. They include the minimum tube wall thickness, tube sheet area ratio and steam velocity entering the cooler.

5. Case Five

The objective of this case was to minimize condenser volume while exercising CONDIP's capabilities to linearly vary tube pitch and tube inner diameter by row. Thirty-five rows were used, which was the identical number as the initial design. Tube pitch and tube inner diameter of both the outermost and innermost rows served as design variables in this case. However - because tube number is now a dependent variable based on the number of rows, tube pitch, and tube diameter - it could not be used as a design variable. The optimized results of this analysis along with the initial design are presented in Table VII.

The results of this test case indicate a condenser volume which is 20 percent smaller than the initial design as compared to a 16 percent decrease in Case 1. The basic reasons and explanations as to why volume was able to be reduced remain fundamentally the same as in Case 1. Attention will therefore be focussed on the effects of linearly varying pitch and tube diameter. Final tube pitch ranged in value from 1.75 in the inner row to 1.44 in the outer row. Similarly, tube inner diameter ranged from .729 in the inner row to .583 in the outer row.

It is believed that smaller pitch and inner diameter were used in the outer row because of the higher available steam saturation pressure and temperature. The resulting higher steam velocities enhanced the beneficial effects of vapor shear on the external heat transfer coefficient thereby improving heat transfer on the outer rows. As steam pressure decreased, then tube pitch and tube inner diameter

increased to compensate and extract all the available heat from the steam. Consequently, steam velocity decreased and was able to satisfy to the limit imposed on the cooler entrance velocity. The end result is a condenser geometry that makes complete use of the available resources and conforms to the geometry to take advantage of the thermal conditions in the condenser. The big limitation with this approach is that the number of rows is held constant. Thus the subsequent condenser is designed around that value and the subsequent optimum design is a function of the number of rows specified.

TABLE I
Input Design Data

PARAMETER	VALUE
Total number of tubes	5230
Tube length (feet)	10.3
Tube inner diameter (inches)	0.527
Tube wall thickness (inches)	0.049
Tube outer diameter (inches)	0.625
Tube mat'l thermal conductivity btu/(ft-hr-°F)	25.0
Tube pitch	1.38
Percent of tubes in the cooler	7.0
Steam inlet flow (lbm/hr)	161,961
Fraction of non-condensable gas (ppm)	37.1
Steam inlet pressure (psia)	1.294
Steam inlet temperature (°F)	110.52
Coolant inlet velocity (ft/sec)	8.473
Coolant inlet temperature (°F)	75.66
Fouling factor	.0002
Inner void diameter (feet)	1.1
Row spacing (inches)	1.35

TABLE II
CONDIP Verification Results

PARAMETER	EXPERIMENT RESULTS	CONDIP RESULTS	CHANGE (%)
Heat transfer area (sq.ft.)	8805	8814	+0.10
Overall heat transfer coefficient btu/(hr-sq.ft.-°F)	635.2	547.9	-9.5
Log mean temperature difference (°F)	28.24	28.62	+1.3
Coolant temperature rise (°F)	10.61	9.90	-6.7
Coolant mass flow rate (10 ⁷ lbm/hr)	1.503	1.540	+2.5
Condenser volume (cu.ft.)	-----	432.3	-----
Bundle diameter (ft)	5.7 7.2	7.17	-----
Shell-side pressure drop (psia)	0.751	1.29	+71.8
Steam exit-fraction (% of input)	-----	13.3	-----
Heat rejected (10 ⁶ btu/hr)	1.595	1.451	-9.03
Area ratio	0.291	0.266	-8.59

TABLE III
Volume Minimization

PARAMETER	BASELINE RESULTS	OPTIMIZED RESULTS	CHANGE (%)
Total number of tubes	5230	5117	-2.2
% of tubes in cocler	7.0	7.01	+0.1
Tube length (ft)	10.3	9.92	-3.7
Tube inner diam. (in)	.527	.582	+10.4
Tube wall thick. (in)	.049	.022	-55.1
Tube outer diam. (in)	.625	.626	+0.2
Tube pitch	1.4	1.73	+23.6
Void diameter (ft)	1.10	1.34	+21.8
Bundle diameter (ft)	7.17	6.59	-8.1
Condenser volume (cu.ft.)	432.3	362.2	-16.2
Area ratio	0.266	0.300	+12.7
Coolant inlet vel. (ft./sec)	8.473	9.00	+6.2
Coolant mass flow rate (10^7 lbm/hr)	1.540	1.955	+26.9
Head loss (ft H ₂ O)	7.35	7.18	-2.3
Pumping power (hp)	55.69	68.99	+23.9
Coolant temperature rise (°F)	9.90	9.00	-9.1
Log mean temperature difference (°F)	28.62	29.13	+1.8
Heat transfer area (sq.ft.)	8814.	8320.	-5.6
Average overall heat transfer coefficient (btu/(hr-sq.ft.-°F))	574.9	689.9	+20.0
Steam exit-fraction (% of input)	13.3	0.0	-100.
Heat rejected (10^6 btu/hr)	1.451	1.672	+15.2

TABLE IV
Power Minimization

PARAMETER	BASELINE RESULTS	OPTIMIZED RESULTS	CHANGE (%)
Total number of tubes	5230	6393	+22.2
% of tubes in cocler	7.0	7.4	+5.7
Tube length (ft)	10.3	13.34	+29.5
Tube inner diam. (in)	.527	.667	+26.6
Tube wall thick. (in)	.049	.0455	-7.1
Tube outer diam. (in)	.625	.758	+21.3
Tube pitch	1.4	1.812	+29.4
Void diameter (ft)	1.10	1.13	+2.7
Bundle diameter (ft)	7.17	9.25	+29.0
Condenser volume (cu.ft.)	432.3	964.4	+123.1
Area ratio	0.266	0.277	+4.1
Coolant inlet vel. (ft./sec)	8.473	3.00	-64.6
Coolant mass flow rate (10 ⁷ lbm/hr)	1.540	1.067	-30.7
Head loss (ft H ₂ O)	7.35	1.11	-84.9
Pumping power (hp)	55.69	5.84	-89.5
Coolant temperature rise (°F)	9.90	16.3	+64.6
Lcg mean temperature difference (°F)	28.62	24.82	-13.3
Heat transfer area (sq.ft.)	8814.	16,921	+92.0
Average overall heat transfer coefficient (btu/(hr-sq.ft.-°F))	574.9	393.8	-31.5
Steam exit-fraction (% of input)	13.3	1.0	-92.5
Heat rejected (10 ⁸ btu/hr)	1.451	1.654	+14.0

TABLE V
Power Minimization With Volume Constant

PARAMETER	BASLINE RESULTS	OPTIMIZED RESULTS	CHANGE (%)
Total number of tubes	5230	5062	+3.2
% of tubes in cocler	7.0	6.7	-4.3
Tube length (ft)	10.3	11.39	+10.6
Tube inner diam. (in)	.527	.594	+12.7
Tube wall thick. (in)	.049	.022	-55.1
Tube outer diam. (in)	.625	.638	+2.1
Tube pitch	1.4	1.753	+25.2
Void diameter (ft)	1.10	1.14	+3.6
Bundle diameter (ft)	7.17	6.73	-6.1
Condenser volume (cu.ft.)	432.3	431.6	-0.2
Area ratio	0.266	0.297	+11.7
Coolant inlet vel. (ft./sec)	8.473	6.74	-20.5
Coolant mass flow rate (10^7 lbm/hr)	1.540	1.508	-2.1
Head loss (ft H ₂ O)	7.35	4.69	-36.2
Pumping power (hp)	55.69	34.77	-37.6
Coolant temperature rise (°F)	9.90	11.6	+17.2
Log mean temperature difference (°F)	28.62	27.63	-3.5
Heat transfer area (sq.ft.)	8814.	9631.4	+9.3
Average overall heat transfer coefficient (btu/(hr-sq.ft.-°F))	574.9	627.3	+9.1
Steam exit-fraction (% of input)	13.3	0.0	-100.
Heat rejected (10^6 btu/hr)	1.451	1.669	+15.0

TABLE VI
Volume Minimization With Power Constant

PARAMETER	BASELINE RESULTS	OPTIMIZED RESULTS	CHANGE (%)
Total number of tubes	5230	4867	-6.9
% of tubes in cocler	7.0	7.2	+2.9
Tube length (ft)	10.3	10.92	+6.0
Tube inner diam. (in)	.527	.581	+10.2
Tube wall thick. (in)	.049	.022	-55.1
Tube outer diam. (in)	.625	.625	0.0
Tube pitch	1.4	1.739	+24.2
Void diameter (ft)	1.10	1.20	+9.1
Bundle diameter (ft)	7.17	6.41	-10.6
Condenser volume (cu.ft.)	432.3	378.4	-12.4
Area ratio	0.266	0.299	+12.4
Coolant inlet vel. (ft./sec)	8.473	8.27	-2.4
Coolant mass flow rate (10^7 lbm/hr)	1.540	1.701	+10.5
Head loss (ft H ₂ O)	7.35	6.67	-9.3
Pumping power (hp)	55.69	55.80	+0.2
Coolant temperature rise (°F)	9.90	10.34	+4.4
Log mean temperature difference (°F)	28.62	28.38	-0.8
Heat transfer area (sq.ft.)	8814.	8697.	-1.3
Average overall heat transfer coefficient btu/(hr-sq.ft.-°F)	574.9	677.4	+17.5
Steam exit-fraction (% of input)	13.3	0.0	-100.
Heat rejected (10^6 btu/hr)	1.451	1.672	+15.2

TABLE VII
Volume Minimization With Linear Variations

PARAMETER	BASELINE RESULTS	OPTIMIZED RESULTS	CHANGE (%)
Total number of tubes	5230	5348	+2.3
% of tubes in cocler	7.0	7.3	+4.3
Tube length (ft)	10.3	8.7	-15.5
Tube inner diam. (in)	.527	*.729 .583	----
Tube wall thick. (in)	.049	.022	-55.1
Tube outer diam. (in)	.625	*.773 .627	----
Tube pitch	1.4	*1.75 1.44	----
Void diameter (ft)	1.10	1.28	+16.4
Bundle diameter (ft)	7.17	6.8	-5.2
Condenser volume (cu.ft.)	432.3	345.8	-20.0
Area ratio	0.266	0.298	+12.0
Coolant inlet vel. (ft./sec)	8.473	9.0	+6.2
Coolant mass flow rate (10^7 lbm/hr)	1.540	2.48	+61.0
Head loss (ft H ₂ O)	7.35	5.84	-20.5
Pumping power (hp)	55.69	71.1	+27.7
Coolant temperature rise (°F)	9.90	7.1	-28.8
Log mean temperature difference (°F)	28.62	30.14	+5.3
Heat transfer area (sq.ft.)	8814.	7746.	-12.1
Average overall heat transfer coefficient btu/(hr-sq.ft.-°F)	574.9	713.1	+24.0
Steam exit-fraction (% of input)	13.3	0.5	-96.2
Heat rejected (10^6 btu/hr)	1.451	1.665	+14.7

* Inner row values followed by outer row values.

VI. CONCLUSIONS

The intent of this research was to create a detailed condenser analysis code capable of being coupled with a numerical optimizer and to test the program to prove its versatility. An additional objective was to validate the analysis with existing data. The results of the test cases were presented in Chapter Five; the resulting conclusions are summarized here.

A. There were significant difficulties encountered in formulating the complex condenser design analysis, CONDIP, in a way that was compatible with the optimizer COPES/CONMIN. However, the majority of those problems were overcome resulting in the creation of a program which, when combined with the optimizer, is capable of taking any initial design, no matter how impractical or infeasible, and solving for an optimum solution based on a set of pre-determined constraints and design variables. There are still some minor limitations as to the degree of optimization, but the final design is usually within 10 percent of the single best optimum. In addition, the test cases indicate that as many as ten design variables and six constraints can be used simultaneously in the design optimization with CONDIP.

B. The test cases demonstrated the effectiveness of CONDIP as a design tool for not only the conceptual design of a condenser, but also in evaluating comparison studies based on any number of design variable combinations. The number of possible combinations of design objectives, design variables and design constraints implies limitless possibilities to be explored and evaluated.

C. An attempt was made to verify CONDIP with existing data with inconclusive results. Part of the blame can be placed on the rather inadequate quality and quantity of the data, but the general performance of CONDIP's condenser indicates a weakness in the analysis. As stated earlier, the source of this weakness may be found in the correlations used for condensate inundation. The constants used in the expression for correcting shell-side heat transfer coefficients are based somewhat on conjecture. Yet they play a significant role in the overall condenser performance. Despite this limitation, the ability to optimize CONDIP's detailed analysis is a significant step forward over using the traditional and limited HEI method.

D. CONDIP incorporates features that further increase its appeal as a design tool. By possessing the ability to linearly vary pitch and tube diameter, a better understanding of how to improve condenser performance based on its configuration is realized. The capability to incorporate shell-side tube enhancement is another added plus. The possibilities that can now be investigated are limitless.

VII. RECOMMENDATIONS

In addition to the insight that this investigation has given into the generation of automated condenser design programs, it has specifically addressed the shortcomings and pitfalls which may be encountered along the way and offered possible solutions to overcome them. Presented below are recommendations for furthering the development of CONDIP as a completely versatile and accepted design program.

A. Since the weak link and the most significant unknown in condenser analysis is the effect of condensate rain in typical condenser environments, subsequent research should be devoted to investigating this phenomenon and developing more precise analytic correlations. In particular, the effects of velocity and flow direction on the condensate film should be attended to.

B. Perhaps in conjunction with the above, a test condenser should be constructed which is geometrically similar to the model proposed in CONDIP in order to physically observe and record the condenser performance. This data could then be used to either verify CONDIP or strengthen some of its analysis. In addition, this condenser should be built such that the tube bank can be arranged in any combination of pitch, tube diameter and row spacing to fully appreciate the effects of these variables.

C. A series of sensitivity studies should be conducted on CONDIP to fully exercise its capabilities and determine the relative effects of various design variables on condenser performance. Tradeoff studies similar to those performed in this research would be most beneficial to fully understand condenser behavior.

D. Additional subroutines should be created which would allow tube enhancement to be a design variable. This involves developing correlations between heat transfer enhancement and associated frictional losses. This type of relationship can be developed for both tube-side and shell-side enhancement.

E. Finally, it is recommended that additional refinement be performed on the code to increase its capability and flexibility. One such way is to somehow allow pitch, tube diameter and tube wall thickness to vary linearly by row while still allowing the number of tubes to be a design variable. The options available are limitless.

APPENDIX A

GLOSSARY

While it would most beneficial to present a complete glossary of all the variables used in CONDIP, the sheer number makes it difficult to present a comprehensive list. However, CONDIP makes liberal use of comment cards to define as many variables as possible to make the code easier to follow. Therefore, the computer listing in Appendix C is available for reference. A list of the possible design variables and constraints is provided here along with its corresponding position in the GLOBCM common block for easy reference in writing the appropriate COPES data cards. In addition, it will be specified whether these variables can be used as design constraints or design variables.

1. ALST: The length of the condenser and cooler tubes in feet. ALST is to be used only as a design variable.
2. DELWP: The pressure difference between the inlet and outlet coclant headers of the condenser bundle in psi. DELWP is to be used only as a design variable.
3. DELWPC: The pressure difference between the inlet and outlet coolant headers of the condenser bundle in psi. DELWPC is to be used only as a design constraint.
4. GPLOW: The mass flow rate of the coolant in lbm/hour. GPLOW cannot be used as a design variable simultaneously with VELBI. Otherwise it can be used as a design variable or a design constraint.
5. SIDI: The tube inner diameter of the innermost row of

the condenser bundle in inches. SIDI is to be used only as a design variable.

7. SIDO: The tube inner diameter of the outermost row of the condenser bundle in inches. If there is no linear variation of tube inner diameter then this variable represents the tube inner diameter of the entire condenser bundle. SIDO is to be used only as a design variable.

8. PHP: The coolant pumping power in horsepower. PHP is to be used only as a design constraint.

9. RSPA: The spacing between concentric rows in the condenser bundle in inches. RSPA is to be used only as a design variable.

10. RADINS: The inner void radius of the condenser bundle in feet. RADINS is to be used only as a design variable.

11. REWI: The tube-side Reynolds number of the coolant in the innermost row of the condenser bundle. REWI is to be used only as a design constraint.

12. REWO: The tube-side Reynolds number of the coolant in the outermost row of the condenser bundle. If there is no linear variation of tube inner diameter then this variable represents the tube-side Reynolds number of the entire condenser bundle. REWO is to be used only as a constraint.

13. SDDI: Tube pitch (tube spacing/tube outer diameter) of the innermost row of the condenser bundle. SDDI is to be used only as a design variable.

14. SDDO: The tube pitch of the outermost row of the condenser bundle. If there is no linear variation of tube pitch then this variable represents the tube pitch for the entire condenser bundle. SDDO is to be used only as a design variable.

15. SLDI: Ratio of tube length to tube outer diameter of the outermost row of the condenser bundle. SLDI is to be used only as a design constraint.
16. SLDO: Ratio of tube length to tube outer diameter of the outermost row of the condenser bundle. If there is no linear variation of tube pitch then this variable represents the tube pitch for the entire condenser bundle. SLDO is to be used only as a design constraint.
17. VELBI: The velocity of the coolant in feet/sec. VELBI cannot be used as a design variable simultaneously with GFLOW. Otherwise it can be used as either a design constraint or as a design variable.
18. XW1: The ratio of tube thickness to tube inner diameter. XW1 can be used only as a design variable.
19. XW2: Tube thickness in inches. XW2 is to be used only as a design variable. XW2 and XW1 cannot be used simultaneously.
20. VOL1: The overall condenser and cooler volume in cubic feet. VOL1 is to be used only as a design constraint.
21. VOL2: The volume occupied by the tube bank, excluding the volume of the inner void, in cubic feet. VOL2 is to be used only as a design constraint.
22. TNOTOT: The total number of tubes in the condenser and cooler combined. If Option 1 is being used then TNOTOT is to be used only as a design constraint. If Option 2 is being used then TNOTOT is to be used only as a design variable.
23. BNDRAD: The condenser bundle in feet. BNDRAD is to be used only as a design constraint.
24. ARATIO: The ratio of the total cross-sectional area of

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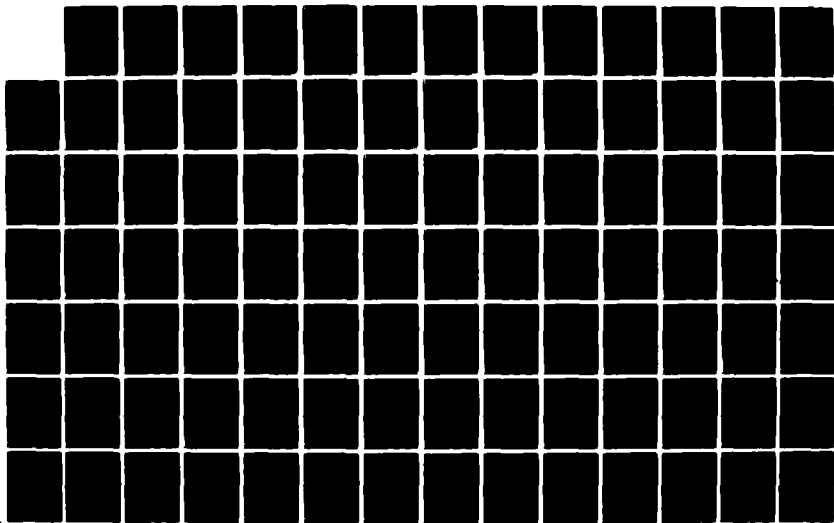
MARINE STEAM CONDENSER DESIGN OPTIMIZATION(U) NAVAL
POSTGRADUATE SCHOOL MONTEREY CA T M BUCKINGHAM DEC 83

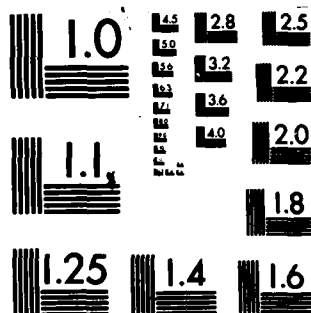
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the tubes (based on the tube outer diameter) to the tube sheet area. ARATIO is to be used only as a design constraint.

25. ODII: The tube outer diameter of the innermost row in inches. ODII is to be used only as a design constraint.

26. ODOI: The tube outer diameter of the outermost row in inches. If there is no linear variation of tube inner diameter then this variable represents the tube outer diameter of the entire condenser bundle. ODOI is to be used only as a design constraint.

27. VLCMAX: The maximum allowable steam velocity into the cooler. VLCMAX can be used only as a design constraint and only when a cooler is being designed in the system.

28. PRCCLR: The percent of the total number of tubes in the cooler. PRCCLR can be used only as a design variable.

APPENDIX B

USERS MANUAL FOR CONDIP

This appendix describes the data cards that are necessary in order to couple any design program with COPES/CONMIN. Also described are cards illustrating data input required by CONDIP to initiate analysis. Thus, the data is divided into the COPES/CONMIN program section and the CONDIP-based condenser design program section.

The COPES data is segmented into "blocks" for convenience. All formats are alphanumeric for title, end and stop cards; F10 for real data; and I10 for integer data. The formatted input may be overridden by inserting commas between data entries. Comment cards may be inserted anywhere in the data stack prior to the end card and are identified by a dollar sign (\$) in column 1. The COPES data stack must terminate with an end card containing the word "END" in column 1-3. It should be noted that information pertaining only to single analysis and optimization is presented here. Information concerning the other options available in COPES along with further explanation of COI&S capabilities can be found in [Ref. 13].

The analysis data is also segmented into blocks for convenience and they begin immediately following the "END" card in the COPES data. No comment cards are permitted here, and the analysis data stack must terminate with the word "STOP" in columns 1-4. This is where the initial design values are placed for entry into CONDIP.

Default values are recommended for use in the following COPES data cards unless otherwise noted. It is recommended that these values in the COPES data blocks be used until the user becomes familiar with the program. In addition a

sample data input is illustrated in figure B.1 at the end of this appendix.

DATA BLOCK A

DESCRIPTION: COPES Title Card

FORMAT: 20A4

1	2	3	4	5	6	7	8
TITLE							

REMARKS:

- 1) This line is available for a brief description.

DATA BLOCK B

DESCRIPTION: COPES Program Control Parameters

FORMAT: 7I10

1	2	3	4	5	6	7	8
NCALC	NDV						

FIELD

CONTENTS

- | | | |
|---|--------|--|
| 1 | NCALC: | Calculation control |
| 0 | | Read input and stop. Data of blocks A-B is required. Remaining data is optional. |
| 1 | | One cycle through the program. Data of blocks A-B is required. Remaining data is optional. |
| 2 | | Optimization. Data of blocks A-I is required. Remaining data is optional. |
| 2 | NDV: | Number of independent design variables in optimization or optimum sensitivity study. |

REMARKS:

- 1) Field 1 determines program execution
- 2) Fields 3-8 are to be left blank for the CONDIP application of COPES/CONMIN.

DATA BLOCK C

DESCRIPTION: COPS Integer Optimization Control Parameters

FORMAT: 8I10

1	2	3	4	5	6	7	8
IPRINT	ITMAX	ICNDIR	NSCAL	ITRH	LINOBJ	NACHX1	NFDG

FIELD

CONTENTS

- 1 IPRINT: Print control used in optimization program, CONMIN.
0 No print during optimization.
1 Print initial and final optimization information.
2 Print above plus function value and design variable values at each iteration.
3 Print above plus constraint values, direction vector and move parameter at each iteration.
4 Print above plus gradient information.
5 Print above plus each proposed design vector, objective function and constraints during the one-dimensional search. required. Remaining data is optional.
- 2 ITMAX: Maximum number of optimization iterations allowed. DEFAULT = 20.
- 3 ICNDIR: Conjugate direction restart parameter. DEFAULT = NDV+1.
- 4 NSCAL: Scaling parameter. GT.0 - Scale design variables to order of magnitude one every NSCAL iterations. LT.0 - Scale design variables according to scaling values input. DEFAULT = No scaling.
- 5 ITRH: Number of subsequent iterations which must satisfy relative or absolute convergence criterion before optimization process is terminated. DEFAULT = 3.
- 6 LINOBJ: Linear objective function identifier. If the optimization objective is known to be a linear function of the design variables, set LINOBJ = 1. DEFAULT = Non-Linear.
- 7 NACHX1: one plus the maximum number of active constraints anticipated. DEFAULT = NDV+2.

DATA BLOCK C (Continued)

FIELD	CONTENTS
8	MFDG: Finite difference gradient identifier.
0	All gradient information is computed by finite difference.
1	Gradient of objective is computed analytically. Gradients of constraints are computed by finite difference.
2	All gradient information is computed analytically

REMARKS:

- 1) The value of NSCAL = 0 is suggested and ITRN = NACMX1 = 0 should be used.
- 2) The value of IPRINT may be reduced when the user becomes familiar with the optimization output.
- 3) The default values will be used if the card is either left blank or a value of zero is entered.
- 4) Because of the complexity of the problem it is necessary to have a large value for ITMAX so the problem will not be terminated prematurely. Recommended value is ITMAX = 40
- 5) The complexity of the condenser analysis ensure that no function can be considered linearly dependent on any combination of variables. This justifies using the DEFAULT value for LINOBJ.

DATA BLOCK D

DESCRIPTION: COPES Floating Point Optimization Program
Parameters

FORMAT: 8F10

1	2	3	4	5	6	7	8
PDCH	PDCHN	CT	CTMIN	CTL	CTLMIN	THETA	PHI

FIELD

CONTENTS

- | | | |
|---|---------|---|
| 1 | PDCH: | Relative change in design variables in calculating finite difference gradients.
DEFAULT = 0.01 |
| 2 | PDCHN: | Minimum absolute step in finite difference gradient calculations. DEFAULT = 0.001. |
| 3 | CT: | Constraint thickness parameter.
DEFAULT = -0.1. |
| 4 | CTMI: | Minimum absolute value of CT considered in the optimization process.
DEFAULT = 0.004 |
| 5 | CTL: | Constraint thickness parameter for linear and side constraints. |
| 6 | CTLMIN: | Minimum absolute value of CTL considered in the optimization process.
DEFAULT = 0.001 |
| 7 | THETA: | Mean value of push-off factor in the method of feasible directions.
DEFAULT = 1.0 |
| 8 | PHI: | Participation coefficient, used if one or more constraints are violated.
DEFAULT = 5.0. |

DATA BLOCK D (continued)

FORMAT: 2F10

1	2	3	4	5	6	7	8
DELPUN	DABFUN						

FIELD

CONTENTS

- 1 DELPUN: Minimum relative change in objective function to indicate convergence of optimization process. DEFAULT = 0.001.
- 2 DABFUN: Minimum absolute change in objective function to indicate convergence of the optimization process. DEFAULT = 0.001 times the initial objective value.

REMARKS:

- 1) Note that data for Data Block D is entered on two separate cards. A blank card indicates the default value is to be used.
- 2) If the NDV is greater than 3, the recommended value for FDCH is between 0.05 and 0.10.

DATA BLOCK E

DESCRIPTION: Total Number of Design Variables, Design Objective Identification and Sign on Design Objective.

FORMAT: 2I10, F10

1	2	3	4	5	6	7	8
NDVTOT	IOBJ	SGNOPT					

FIELD

CONTENTS

- 1 **NDVTOT:** Total number of variables linked to the design variables. NDVTOT must be greater or equal to NDV. This option allows two or more parameters to be assigned to a single design variable. The value of each parameter is the value of the design variable times a multiplier which may be different for each parameter.
DEFAULT = NDV.
- 2 **IOBJ:** Global variable number associated with objective function in optimization or optimum sensitivity analysis.
- 3 **SGNOPT:** Sign used on objective of optimization to identify whether function is to be maximized or minimized. +1.0 indicates maximization; -1.0 indicates minimization.
DEFAULT = -1.0

REMARKS:

1) Currently there are not any variables in CONDIP which are linked to any of the design variables. Therefore the DEFAULT value is used for NDVTOT.

DATA BLOCK F

DESCRIPTION: Design Variable Bounds, Initial Values, and Scaling Factors.

FORMAT: 4F10

1	2	3	4	5	6	7	8
VLB	VUB	X	SCAL				

FIELD

CONTENTS

- | | | |
|---|-------|---|
| 1 | VLB: | Lower bound on the design variable. |
| 2 | VUB: | Upper bound on the design variable. |
| 3 | X: | Initial value of the design variable.
If X is non-zero, this will supercede the
value initialized by subroutine ANALIZ. |
| 4 | SCAL: | Design variable scale factor. Not
used if NSCAL \geq 0 in Block C |

REMARKS:

- 1) There must be one separate data card for each design variable. Therefore there will be NDV data cards.
- 2) For all applications with CONDIP, initial values for the design variables will be entered through the INPUT subroutine called in ANALIZ.

DATA BLOCK G

DESCRIPTION: Design Variable Identification

FORMAT: 2I10,F10

1	2	3	4	5	6	7	8
NDSGN	IDSGN	AMULT					

FIELD

CONTENTS

- | | | |
|---|--------|---|
| 1 | NDSGN: | Design variable number associated with the variable. |
| 2 | IDSGN: | Global variable number associated with the variable. |
| 3 | AMULT: | Constant multiplier on the variable. The value of the variable will be the value of the design variable, NDSGN, times AMULT. DEFAULT = 1.0. |

REMARKS:

1) There must be one separate card for each of the NDVTOT design variables. These data cards must follow the same order as the corresponding design variable parameter cards in Block F.

DATA BLOCK H

DESCRIPTION: Number of Constrained Parameters.

FORMAT: I10

1	2	3	4	5	6	7	8
NCONS							

FIELD

CONTENTS

1 NCONS: Number of constraint SETS in the
 optimization problem.

REMARKS:

1) If two or more adjacent parameters in the Global common block have the same limits imposed, these are part of the same constraint set.

DATA BLOCK I

DESCRIPTION: Constraint Identification and Bounds.

FORMAT: 3I10

1	2	3	4	5	6	7	8
ICON	JCON	LCON					

FIELD

CONTENTS

- | | | |
|---|-------|--|
| 1 | ICCN: | First Global number corresponding to the constraint set. |
| 2 | JCON: | Last Global number corresponding to the constraint set. DEFAULT = ICCN. |
| 3 | LCON: | Linear constraint identifier for this set of constrained variables.
LCCN = 1 indicates linear constraints.
DEFAULT = 0 = Nonlinear constraint. |

REMARKS:

- 1) In CONDIP there is only Global number and thus one constraint that comprise a constraint set. Therefore the DEFAULT value is used for JCON.
- 2) All the constraints in this analysis are nonlinear. The DEFAULT value was therefore used for LCON as well.
- 3) This is the first card of a two card set which must be read together.

DATA BLOCK I (Continued)

FORMAT: 4F10

1	2	3	4	5	6	7	8
BL	SCAL1	BU	SCAL2				

FIELD

CONTENTS

- | | | |
|---|--------|---|
| 1 | BL: | Lower bound on the constrained variables.
Value less than $-2.0E+15$ is assumed
unbounded |
| 2 | SCAL1: | Normalization factor on lower bound.
DEFAULT = Max of ABS(BL) or 0.1. |
| 3 | BU: | Upper bound on the constrained variables.
Value greater than $+2.0E+15$ is assumed
unbounded. |
| 4 | SCAL2 | Normalization factor on upper bound.
DEFAULT = Max of ABS(BU) or 0.1. |

REMARKS:

1) The normalization factor can usually be defaulted, with the notable exception of exit-fraction. the normalization factor used for this constraint is usually ten times the upper bound.

DATA BLOCK P

DESCRIPTION: COPES Data 'END' Card.

FORMAT: 3A1

1	2	3	4	5	6	7	8
END							

FIELD

CONTENTS

1

The word 'END' in column 1-3.

REMARKS:

- 1) This card must appear at the end of the COPES data.
- 2) This ends the COPES input deck.

DATA BLOCK AA

DESCRIPTION: Geometry Option

FORMAT: I5

	1	2	3	4	5	6	7	8
IOPT								

FIELD

CONTENTS

1	IOPT	Two condenser geometric options
	1	IOPT = 1. Number of condenser rows is a input as a constant; the number of tubes is a dependant variable. Use data blocks EE, FF, and GG.
	2	IOPT = 2. Number of tubes is allowed to be an independent variable and the number of rows is a dependant variable. Use data blocks HH and II. DEFAULT value is IOPT = 2.

REMARKS:

1) Data is right-justified and blanks will be interpreted as zeros.

2) If IOPT = 1, a smaller finite difference (FDCH) can be utilized in data Block D. This is because with this option the design analysis is less sensitive to the problems discussed earlier. Recommended using the DEFAULT value of 0.01 for FDCH.

DATA BLOCK BB

DESCRIPTION: Condenser Orientation

FORMAT: 1I5,3F10

1	2	3	4	5	6	7	8
ISEC	SECWID	PHI	PRCCLR				

FIELD

CONTENTS

- | | | |
|---|--------|---|
| 1 | ISEC | The number of sectors in the condenser. |
| 2 | SECWID | Sector width in degrees of arc. |
| 3 | PHI | Symmetry angle measure from the vertical. |
| 4 | PRCCLR | The percent of the tubes in the cooler. |

REMARKS:

- 1) Data BB is required, no matter what geometry option is chosen.
- 2) The only limitation on ISEC and SECWID is that their product is less than 360 degrees. If the product is exactly 360 degrees, certain trigonometric functions will return a singularity.
- 3) PHI is that angle from the vertical that cuts the condenser in half.
- 4) Data is right-justified and blanks will be interpreted as zeros.

DATA BLOCK CC

DESCRIPTION: Void Size, Tube Length, Row Spacing

FORMAT: 3F10

1	2	3	4	5	6	7	8
RADINS	ALST	RSPA					

FIELD

CONTENTS

- | | | |
|---|--------|---|
| 1 | RADINS | The inner void radius; feet. |
| 2 | ALST | The tube length; feet. |
| 3 | RSPA | Concentric row spacing about the void;
inches. |

REMARKS:

- 1) Data CC is required, no matter what geometry option is chosen.

DATA BLOCK DD

DESCRIPTION: Tube Material Parameters

FORMAT: I5,4F10

1	2	3	4	5	6	7	8
IWALL	XW	TUBESW	SKW	FOUL			

FIELD

CONTENTS

- | | | |
|---|--------|---|
| 1 | IWALL | A Flag indicating the tube thickness specification.
1 IWALL = 1. Tube thickness is input as ratio of tube thickness to tube inner diameter.
2 IWALL = 2. Tube thickness is input in inches. |
| 2 | XW | The input for wall thickness, dependent on the value for IWALL. |
| 3 | TUBESW | Specific weight of the tube material:
lbm/(cu.ft.) |
| 4 | SKW | Tube material thermal conductivity:
(btu-ft)/(sq.ft.-hr-°F) |
| 5 | FOUL | Tube fouling factor. |

REMARKS:

- 1) Data DD is required, no matter what geometry option is chosen.
- 2) Data is right-justified and blanks will be interpreted as zeros.

DATA BLOCK EE

DESCRIPTION: Number of Rows

FORMAT: I5

1	2	3	4	5	6	7	8
NOROWS							

FIELD

CONTENTS

1	NOROWS	The number of concentric rows in the condenser bundle built around the center void
---	--------	--

REMARKS:

- 1) Data EE is used only when IOPT = 1
- 2) Data is right-justified and blanks will be interpreted as zeros.

DATA BLOCK FF

DESCRIPTION: Tube Inner Diameter

FORMAT: 1I5,2F10

1	2	3	4	5	6	7	8
MDIAM	SIDO	SIDI					

FIELD

CONTENTS

- | | | |
|---|-------|--|
| 1 | MDIAM | A flag to indicate whether tube inner diameter will linearly vary by row through the condenser bundle.
1 MDIAM = 1. Tube inner diameter is uniform through the condenser bundle.
2 MDIAM = 2. Tube inner diameter varies linearly through the bundle by row. |
| 2 | SIDO | Tube inner diameter of the outer row; inches. |
| 3 | SIDI | Tube inner diameter of the inner row; inches. |

REMARKS:

- 1) Data FF is used only when IOPT = 1
- 2) Data is right-justified and blanks will be interpreted as zeros.
- 3) Cooler tubes use the inner diameter of the innermost bundle row.
- 4) The DEFAULT value is MDIAM = 1

DATA BLOCK GG

DESCRIPTION: Tube Pitch

FORMAT: 1I5,2F10

1	2	3	4	5	6	7	8
MPITCH	SDDO	SDDI					

FIELD

CONTENTS

- | | | |
|---|--------|---|
| 1 | MPITCH | A flag to indicate whether tube pitch will linearly vary by row through the condenser bundle.
1 MPITCH = 1. Tube pitch is uniform through the condenser bundle.
2 MPITCH = 2. Tube pitch varies linearly through the bundle by row. |
| 2 | SDDO | Tube pitch of the outer row; |
| 3 | SDDI | Tube pitch of the inner row; |

REMARKS:

- 1) Data GG is used only when IOPT = 1
- 2) Data is right-justified and blanks will be interpreted as zeros.
- 3) Cooler tubes use the pitch of the innermost bundle row.
- 4) The DEFAULT value is MPITCH = 1

DATA BLOCK HH

DESCRIPTION: Tube Inner Diameter and Tube Pitch

FORMAT: 2F10

1	2	3	4	5	6	7	8
SIDO	SDDO						

FIELD

CONTENTS

- | | | |
|---|------|--|
| 1 | SIDO | Tube inner diameter for the entire condenser; inches |
| 2 | SDDO | Tube pitch for the entire condenser |

REMARKS:

- 1) Data HH is used only when IOPT = 2.
- 2) Data is right-justified and blanks will be interpreted as zeros.
- 3) In the calculations, SIDI is set equal to SIDO and SDDI is set equal to SDDO. This avoids the need for two systems of nomenclature for each geometry option.

DATA BLOCK II

DESCRIPTION: Total Number of Tubes in the Condenser

FORMAT: F12

1	2	3	4	5	6	7	8
TNOTOT							

FIELD

CONTENTS

1	TNOTOT	The total number of tubes in the condenser (cooler and the bundle).
---	--------	---

REMARKS:

- 1) Data II is used only when IOPT = 2.
- 2) Data is right-justified and blanks will be interpreted as zeros.

DATA BLOCK JJ

DESCRIPTION: Inlet Steam Mixture.

FORMAT: 15,2F10

1	2	3	4	5	6	7	8
JGAS	WSI	WNCIR					

FIELD

CONTENTS

- | | | |
|---|-------|---|
| 1 | JGAS | A Flag indicating the type of non-condensable gas entering the system.
1 JGAS = 1. This indicates that the gas is air.
2 JGAS = 2. This indicates that the gas is carbon dioxide.
3 JGAS = 3. This indicates that the gas is a mixture of the two. |
| 2 | WSI | Steam flow rate entering the condenser; lbm/hr. |
| 3 | WNCIR | Ratio of the non-condensable gas flow to inlet steam flow; lbm/hr. |

REMARKS:

- 1) Data JJ is required, no matter what geometry option is chosen.
- 2) Data is right-justified and blanks will be interpreted as zeros.

DATA BLOCK KK

DESCRIPTION: Inlet Temperatures.

FORMAT: 2F10

1	2	3	4	5	6	7	8
STBI	STSAT1						

FIELD

CONTENTS

- | | | |
|---|--------|--|
| 1 | STBI | Coclant inlet temperature; °F. |
| 2 | STSAT1 | Inlet steam saturation temperature;
°F. |

REMARKS:

- 1) Data KK is required no matter, what geometry option is chosen.
- 2) Data is right-justified and blanks will be interpreted as zeros.

DATA BLOCK LL

DESCRIPTION: Cooling Water Parameters

FORMAT: 2F10

1	2	3	4	5	6	7	8
IFLOW	X5						

FIELD

CONTENTS

- | | | |
|---|-------|--|
| 1 | IFLOW | A control flag for cooling water specifications.
IFLOW = 1. Input pressure drop across cooling water headers in psia.
IFLOW = 2. Input cooling water velocity in ft/sec.
IFLOW = 3. Input coolant flow in lbm/hr. |
| 2 | X5 | Actually input the value for flow into this variable. The specification for flow to be determined by IFLOW |

REMARKS:

- 1) Data LL is required, no matter what geometry option is chosen.
- 2) Data is right-justified and blanks will be interpreted as zeros.
- 3) X5 acts as a temporary all-purpose storage variable for whatever expression for coolant flow is used.

DATA BLOCK MM

DESCRIPTION: Internal Enhancement Regions

FORMAT: 15

1	2	3	4	5	6	7	8
NEI							

FIELD

CONTENTS

1 NEI Number of internal enhancement regions.
A value between 1 and 6.

REMARKS:

- 1) Data MM is optional. There must be NEI subsequent data cards providing the necessary parameters for each region.
- 2) enhancement can only be used if IOPT = 1.
- 3) Data is right-justified and blanks will be interpreted as zeros.
- 4) This value was zero for all runs.

DATA BLOCK NN

DESCRIPTION: Internal Enhancement Parameters

FORMAT: 2I5,3F10

1	2	3	4	5	6	7	8
NRNI	NETI	ENI	BC	BE			

FIELD

CONTENTS

- | | | |
|---|------|--|
| 1 | NRNI | Row number of first row in internal enhancement region. |
| 2 | NETI | Number of tubes in each internal enhancement region. |
| 3 | ENI | Internal heat transfer enhancement factor. |
| 4 | BC | Coefficient in internally enhanced tube coolant pressure drop calculation. |
| 5 | BE | Exponent in coolant pressure drop calculation. |

REMARKS:

- 1) Data NN is optional. However, if NEI is greater than zero then there must NEI "NN" data cards to provide the necessary data for each enhancement region.
- 2) enhancement can only be used if IOPT = 1.
- 3) Data is right-justified and blanks will be interpreted as zeros.
- 4) These values are constant for entire run and cannot be changed by the optimizer.
- 5) This value was zero for all runs.

DATA BLOCK 00

DESCRIPTION: External Enhancement Regions

FORMAT: 15

1	2	3	4	5	6	7	8
NEE							

FIELD

CONTENTS

1 NEE Number of external enhancement regions.
A value between 1 and 6.

REMARKS:

- 1) Data 00 is optional. There must be NEE subsequent data cards providing the necessary parameters for each region.
- 3) Data is right-justified and blanks will be interpreted as zeros.
- 4) This value was zero for all runs.

DATA BLOCK PP

DESCRIPTION: External Enhancement Parameters

FORMAT: 2I5,2F10

1	2	3	4	5	6	7	8
NRNE	NETE	ENO	ENH				

FIELD

CONTENTS

- | | | |
|---|------|---|
| 1 | NRNE | Row number of first row in external enhancement region. |
| 2 | NETE | Number of tubes in each external enhancement region. |
| 3 | ENI | External heat transfer enhancement factor. |
| 4 | ENH | Steam-side pressure drop factors. |

REMARKS:

- 1) Data PP is optional. However, if NEE is greater than zero then there must NEE "PP" data cards to provide the necessary data for each enhancement region.
- 2) Data is right-justified and blanks will be interpreted as zeros.
- 3) Enhancement can only be used if IOPT = 1.
- 4) These values are constant for an entire run and cannot be changed by the optimizer.
- 5) This value was zero for all runs.

DATA BLOCK QQ

DESCRIPTION: Baffle Options

FORMAT: I5

1	2	3	4	5	6	7	8
IBAF							

FIELD

CONTENTS

1	IBAF	A flag to be used to determine baffle number and location.
---	------	--

REMARKS:

- 1) Data QQ is optional.
- 2) Data is right-justified and blanks will be interpreted as zeros.
- 3) These values are constant for an entire run and cannot be changed by the optimizer.
- 4) Additional specified baffles were not used in any of the runs. This value was zero for all runs.

DATA BLOCK RR

DESCRIPTION: Baffle Location

FORMAT: I5

1	2	3	4	5	6	7	8
JBAF							

FIELD

CONTENTS

1 JBAF An array containing baffle locations

REMARKS:

- 1) Data RR is optional.
- 2) Data is right-justified and blanks will be interpreted as zeros.
- 3) These values are constant for an entire run and cannot be changed by the optimizer.
- 4) Additional specified baffles were not used in any of the runs. This value was zero for all runs.

DATA BLOCK SS

DESCRIPTION: Detailed Printout

FORMAT: I5

1	2	3	4	5	6	7	8
IPRT							

FIELD

CONTENTS

1	IPRT	A flag to generate a detailed output of the condenser analysis (OUT3)
---	------	--

REMARKS:

- 1) Data SS is optional.
- 2) Data is right-justified and blanks will be interpreted as zeros.
- 3) These values are constant for an entire run and cannot be changed by the optimizer.
- 4) This value was zero for all runs.

VOLUME MINIMIZATION - CIRCULAR CONDENSOR

```

2.8
1.40,.9,,20
.10

1.20,-1.
1.0,2.0E+15
1000.,8000.
1.1,2.
3.,9.0
.022.,109
.407,1.206
1.1,
2.,10.
1.1
2.22
3.14
4.17
5.19
6.7
7.10
8.29
5
4
-2.0E+15,,.01,.01
23
.5,,5.
24
.1,,.30
26
.625,,1.25
28
-2.E+15,,2.00.
END
2
12 29.99 180. 7.0
0.55 10.3 282. 26.0 .0002
.527 1.40
5230.0
1 161.970 .0000371
76.66 110.52
2 8.473
0
0
0
0
0

```

Figure B.1 Sample Data Input.

APPENDIX C
CONDIP LISTING

The following Appendix contains a complete listing for CONDIP. An effort has been made to make the program as readable as possible through liberal use of comment cards.

CON00490
CON00500
CON00510
CON00520
CON00530
CON00540
CON00550
CON00560
CON00570
CON00580
CON00590
CON00600
CON00610
CON00620
CON00630
CON00640
CON00650
CON00660
CON00670
CON00680
CON00690
CON00700
CON00710
CON00720
CON00730
CON00740
CON00750
CON00760
CON00770
CON00780
CON00790
CON00800
CON00810
CON00820
CON00830
CON00840
CON00850
CON00860
CON00870
CON00880
CON00890
CON00900
CON00910
CON00920
CON00930
CON00940
CON00950
CON00960

FOUL = TUBE FOULING FACTOR.
GFLW = COOLANT MASS FLOW RATE LBM/HR
IBAF = CONTROL FLAG FOR BAFFLE OPTIONS
IPRT = CONTROL FLAG FOR COOLING WATER SPECIFICATION.
ISEC = CONTROL FLAG FOR OUTPUT. (EXTENDED OUTPUT IF IPRT>0.)
JWALL = NO. OF SECTORS IN CONDENSER THICKNESS SPECIFICATION.
JWALL = ARRAY CONTAINING BAFFLE OR
JGAS = N/C GAS IDENTIFIER 1,2,3
MDIAM = CONTROL FLAG FOR LINEAR VARIATION IN TUBE DIAMETER.
MDITCH = CONTROL FLAG FOR LINEAR VARIATION IN TUBE PITCH.
NETE = NUMBER OF EXTERNAL ENHANCEMENT REGIONS.
NETI = NUMBER OF TUBES IN EACH EXTERNAL ENHANCEMENT REGION.
NETI = NUMBER OF TUBES IN THE CONDENSER EXTERNAL ENHANCEMENT REGION.
NOROWS = NUMBER OF ROWS IN THE CONDENSER
NRNE = ROW NUMBER OF FIRST ROW IN EXTERNAL ENHANCEMENT REGION.
SIDDI = TUBE ID AT INSIDE ROW - IN
SIDDI = TUBE ID AT OUTSIDE ROW - IN
SIOP = IF OPT=1 THEN INDICATE WHICH GEOMETRY MODULE IS BEING USED
VARIATION IN PITCH AND TUBE DIAMETER IS PERMITTED.
IF OPT=2 THEN TNOTGT IS A DESIGN VARIABLE AND LINEAR
VARIATION IS NOT PERMITTED.
PHI = SYMMETRY ANGLE MEASURED FROM THE VERTICAL
RADIUS = BUNDLE INSIDE RADIUS - FT
RSPA = TUBE ROW RADIAL SEPARATION - IN
SDDI = PITCH AT INSIDE ROW
SDDO = PITCH AT OUTSIDE ROW
SECMID = TUBE MATERIAL THERMAL CONDUCTIVITY BTU-Ft/HR-Ft*2-F
SKWI = COOLANT INLET TEMP
STSAT1 = INLET STEAM SAT TEMP
TNOTGT = TOTAL NUMBER OF TUBES IN THE CONDENSER/COOLER
TUBESW = SPECIFIC WEIGHT OF THE TUBE MATERIAL LBM/CU FT
VELBI = COOLANT FLOW VELOCITY FT/SEC
WNCIR = RATIO OF N/C MASS FLOW TO STEAM MASS FLOW
WSI = STEAM FLOW RATE LBM/HR
XW1 = TEMP INPUT VALUE OF XW1 AND XW2
XW1 = RATIO OF TUBE WALL THICKNESS TO TUBE ID
XW2 = TUBE WALL THICKNESS INCHES

ZZZ INP-2

READ (5,330) IOPT
READ (5,340) ISEC, SECWID, PHI, PRCCLR
READ (5,360) RADINS, ALST, RSPA

CON00970
CON00580
CON00990
CON01000
CON01010
CON01020
CON01030
CON01040
CON01050
CON01060
CON01070
CON01080
CON01090
CON01100
CON01110
CON01120
CON01130
CON01140
CON01150
CON01160
CON01170
CON01180
CON01190
CON01200
CON01210
CON01220
CON01230
CON01240
CON01250
CON01260
CON01270
CON01280
CON01290
CON01300
CON01310
CON01320
CON01330
CON01340
CON01350
CON01360
CON01370
CON01380
CON01390
CON01400
CON01410
CON01420
CON01430
CON01440

```

C      READ (5,400) IWALL,XW,TUBESW,SKW,FOUL
C      IF ((IOPT.GE.2).OR.(IOPT.LT.1)) GO TO 10

      READ (5,380) NOROWS
      READ (5,370) MDIAM,SID0,SID1
      GO TO 20
      READ (5,360) SID0,SDD0
      MPITCH=1
      MDIAM=1

C      IF (MDIAM.EQ.1) SID1=SID0
      IF (MPITCH.EQ.1) SDD1=SDD0
      IF (IWALL.NE.2) IW=1
      XW1=0.
      XW2=0.
      IF (IW.EQ.1) XW1=XW
      IF (IW.EQ.2) XW2=XW
      READ (5,350) JGAS,WSI,WNCIR
      READ (5,410) STBI,STSAT1
      READ (5,420) IFLOW,X5
      IFL=IFLOW
      GFLOW=0.
      VELBI=0.
      DELWP=0.
      IF (IFLOW.EQ.1) DELWP=X5
      IF (IFLOW.EQ.2) VELBI=X5
      IF (IFLOW.EQ.3) GFLOW=X5
      READ (5,430) NEI
      IF (NEI.EQ.0) GO TO 40
      IF ((NEI.LT.0).AND.(NEI.GT.6)) GO TO 120
      DO 30 I=1,NEI
      READ (5,440) NRNI(1),NETI(1),ENI(1),BC(1),BE(1)
      READ (5,430) NEE
      IF (NEE.EQ.0) GO TO 60
      IF ((NEE.LE.0).OR.(NEE.GT.6)) GO TO 120
      DO 50 I=1,NEE
      READ (5,450) NRNE(1),NETE(1),END(1),ENH(1)
      READ (5,430) IBAF
      IF ((IBAF.LE.-2).OR.(IBAF.GT.1SEC)) GO TO 120
      IF ((IBAF.EQ.2).OR.(IBAF.EQ.-1)) GO TO 80
      DO 70 I=1,IBAF
      READ (5,430) JBAF(1)
      CONTINUE
      READ (5,430) IPRT

```



```

C$-----
C INP 3
C
C ZZZ INP-3
C-----
IF ((IOPT.EQ.1).OR.(IOPT.EQ.2)) GO TO 90
WRITE (6,460)
WRITE (6,470) IOPT
IOPT=2
IF ((IOPT.EQ.2) GO TO 110
IF ((MDIAM.EQ.2).OR.(MDIAM.EQ.1)) GO TO 100
WRITE (6,460)
WRITE (6,480) MDIAM
WRITE (6,510)
MDIAM=1
IF ((MPITCH.EQ.1).OR.(MPITCH.EQ.2)) GO TO 110
WRITE (6,460)
WRITE (6,490) MPITCH
WRITE (6,510)
MPITCH=1
IF ((IWALL.EQ.1).OR.(IWALL.EQ.2)) GO TO 120
WRITE (6,460)
WRITE (6,500) IWALL
WRITE (6,510)
IWALL=1
C$-----
C INP 4
C
C ZZZ INP-4
C-----
IERR=0
IF ((ISEC.GT.0).AND.(ISEC.LE.15)) GO TO 130
IERR=1
WRITE (6,520)
WRITE (6,530) ISEC
X2=SECWID*FLOAT(ISEC)
IF ((X2.LE.360.).AND.(X2.GT.0.)) GO TO 140
WRITE (6,520) X2
WRITE (6,540) ISEC,SECWID
IERR=1
IF ((IOPT.EQ.2) GO TO 150
IF ((NROWS.GT.0).AND.(NROWS.LE.99)) GO TO 100
IERR=1
WRITE (6,520)

```

LOCATE NON-RECOVERABLE INPUT ERRORS

CON01450
CON01460
CON01470
CON01480
CON01490
CON01500
CON01510
CON01520
CON01530
CON01540
CON01550
CON01560
CON01570
CON01580
CON01590
CON01600
CON01610
CON01620
CON01630
CON01640
CON01650
CON01660
CON01670
CON01680
CON01690
CON01700
CON01710
CON01720
CON01730
CON01740
CON01750
CON01760
CON01770
CON01780
CON01790
CON01800
CON01810
CON01820
CON01830
CON01840
CON01850
CON01860
CON01870
CON01880
CON01890
CON01900
CON01910
CON01920

CON01530
CON01540
CON01550
CON01560
CON01570
CON01580
CON01590
CON01600
CON02010
CON02020
CON02030
CON02040
CON02050
CON02060
CON02070
CON02080
CON02090
CON02100
CON02110
CON02120
CON02130
CON02140
CON02150
CON02160
CON02170
CON02180
CON02190
CON02200
CON02210
CON02220
CON02230
CON02240
CON02250
CON02260
CON02270
CON02280
CON02290
CON02300
CON02310
CON02320
CON02330
CON02340
CON02350
CON02360
CON02370
CON02380
CON02390
CON02400

```

C 150      WRITE (6,560) NCROWS
          GO TO 160
          IF (TNOTOT.GT.0) GO TO 160
          IERR=1
          WRITE (6,520)
          WRITE (6,570) TNOTOT
C 160      IF (RADINS.GT.0.) GO TO 170
          IERR=1
          WRITE (6,520)
          WRITE (6,580) RADINS
          IF (ALST.GT.0.) GO TO 180
          IERR=1
          WRITE (6,520)
          WRITE (6,590) ALST
          IF (SIDD.GT.0.) GO TO 190
          IERR=1
          WRITE (6,520)
          WRITE (6,600) SIDD
          IF ((MDIAM.EQ.1).OR.(SIDI.GT.0.)) GO TO 200
          IERR=1
          WRITE (6,520)
          WRITE (6,610) SIDI
          IF (SDDO.GT.1.) GO TO 210
          IERR=1
          WRITE (6,520)
          WRITE (6,620) SDDO
          IF ((MPTCH.EQ.1).OR.(SDDI.GT.1.)) GO TO 220
          IERR=1
          WRITE (6,520)
          WRITE (6,630) SDDI
          IF ((XW1.EQ.2) GO TO 230
          IF (XW1.GT.0.) GO TO 240
          IERR=1
          WRITE (6,520)
          WRITE (6,640) XW1
          GO TO 240
          X=XW2
          IF (X.GT.0.) GO TO 240
          IERR=1
          WRITE (6,520)
          WRITE (6,650) XW2
          IF ((WNCIR.GE.0.).AND.(WNCIR.LT.1.)) GO TO 250
          IERR=1
          WRITE (6,520)
          WRITE (6,660) WNCIR
          IF ((STBI.GT.-32.).AND.(STBI.LT.212)) GO TO 260

```

```

260      IERR=1 (6,520) STBI
      WRITE (6,670) STBI
      IF (STBI.LT.STSAT) GO TO 270
      IERR=1
      WRITE (6,520) STBI,STSATI
      WRITE (6,680) STBI,STSATI
      IF ((IFLOW.GT.0).OR.(IFLOW.LE.3)) GO TO 280
      IERR=1
      WRITE (6,520) IFLOW
      WRITE (6,690) IFLOW
      IF ((NEI.GE.0).AND.(NEI.LE.6)) GO TO 290
      IERR=1
      WRITE (6,520) NEI
      WRITE (6,700) NEI
      IF ((NEE.GE.0).AND.(NEE.LE.6)) GO TO 300
      IERR=1
      WRITE (6,520) NEE
      WRITE (6,710) NEE
      IF ((IBAF.GE.-1).AND.(IBAF.LE.ISEC)) GO TO 310
      IERR=1
      WRITE (6,520) IBAF,ISEC
      WRITE (6,720) IBAF,ISEC
      WRITE (6,730)
      IF (IERR.EQ.0) GO TO 320
      STOP
      RETURN
320      FORMAT (15,3F10.5)
330      FORMAT (15,F10.5,F10.7)
340      FORMAT (4F10.5)
350      FORMAT (15,F10.5,F10.5)
360      FORMAT (15)
370      FORMAT (F12.5)
380      FORMAT (15,4F10.5)
390      FORMAT (2F10.5)
400      FORMAT (15,F10.5)
410      FORMAT (15)
420      FORMAT (215,3F10.5)
430      FORMAT (215,2F10.5)
440      FORMAT (1H0,31H**)
450      FORMAT (1H,22H INPUT VALUE OF OPT =,15,27H OUT OF RANGE, OPT SET
460      1 TO 2)
470      1 FORMAT (1H,21H INPUT VALUE OF MDIAM=,15,29H OUT OF RANGE, MDIAM SEC
480      1 TO 1)
490      1 FORMAT (1H,22H INPUT VALUE OF MPITCH=,15,30H OUT OF RANGE, MPITCH
500      1 SET TO 1)
510      1 FORMAT (1H,21H INPUT VALUE OF IWALL=,15,29H OUT OF RANGE, IWALL SEC

```


C----- COMMON /GLOBCH/ ALST; DELWP, DELWPC, EXITQA, GFLOW, SIU1, SIDD, PHP, RSPA,
1RA DINS, REWI, RENW, SDDI, SDDO, SLDI, SLDI, SLDI, VOL1, VOL2, TNOTD,
2T, BNDRAD, ARATI, QDI, SDDC, VLCMAX, PRCCCLR
COMMON /INPT/ BC(6), BE(6), ENI(6), ENQ(6), FOU, PHI, SKW, SIBI, S
1TSATI, TUBESW, NCI, IOPI, PST(15), SECWID, IBAF, ISEC, JBAF(16), JBAS, MD
2IAM, MPITCH, NEE, NEI, NETE(6), NETI(6), NRNE(6), NRNI(6), NOROWS, WTST(15)
3WSSI, PFI, IFLW, IWALL
COMMON /INPT1/ IFLW, IWALL
WRITE (6,60)
WRITE (6,70)
WRITE (6,80)
WRITE (6,90)
WRITE (6,100)
WRITE (6,80)
WRITE (6,110)
WRITE (6,120)
WRITE (6,130)
WRITE (6,140)
WRITE (6,150)
WRITE (6,160)
WRITE (6,170) TNOTGT
IF (I) OPT.EQ.2) GO TO 10
IF (I) OPT.EQ.2) GO TO 10
WRITE (6,160) NOROWS
WRITE (6,180) RADINS
WRITE (6,190) ALST
WRITE (6,200) ADIAM
IF (MDIAM.EQ.3) GO TO 20
WRITE (6,210) SIDD
WRITE (6,240)
GO TO 30
WRITE (6,220) SIDD, SIDI
WRITE (6,230) MPITCH
IF (MPITCH.EJ.0) GO TO 40
WRITE (6,260) SDDO
WRITE (6,280)
GO TO 50
WRITE (6,270) SDDO, SDDI
WRITE (6,250) IWALL
IF (IWALL.EQ.1) WRITE (6,300) XW1
IF (IWALL.EQ.2) WRITE (6,290) XW2
WRITE (6,310) TUBESW
WRITE (6,320) SKW
WRITE (6,330) FCUL
WRITE (6,340) FSI
IF (JGAS.EQ.1) WRITE (6,360)
IF (JGAS.EQ.2) WRITE (6,370)
IF (JGAS.EQ.3) WRITE (6,380)
WRITE (6,340) WSI
CONO3370
CONO3380
CONO3390
CONO3400
CONO3410
CONO3420
CONO3430
CONO3440
CONO3450
CONO3460
CONO3470
CONO3480
CONO3490
CONO3500
CONO3510
CONO3520
CONO3530
CONO3540
CONO3550
CONO3560
CONO3570
CONO3580
CONO3590
CONO3600
CONO3610
CONO3620
CONO3630
CONO3640
CONO3650
CONO3660
CONO3670
CONO3680
CONO3690
CONO3700
CONO3710
CONO3720
CONO3730
CONO3740
CONO3750
CONO3760
CONO3770
CONO3780
CONO3790
CONO3800
CONO3810
CONO3820
CONO3830
CONO3840

```

60 70 160 170 180 190 200 210 220 230 240 250 260 270 280 290 300 310
WR ITE (6.350) WNCIR
WR ITE (6.390) STBI
WR ITE (6.400) SISA T1
WR ITE (6.410) I FLOW
IF (I FLOW.EQ.3) WRITE (6.420) GFLOW
IF (I FLOW.EQ.2) WRITE (6.430) VELBI
IF (I FLOW.EQ.1) WRITE (6.440) DELWP
WR ITE (6.450) NEI
WR ITE (6.460) NEE
WR ITE (6.470) IBAF
RETURN (1H1)
FORMAT (1H,51H
1/62H ALST 3 GLOBAL COMMON BLOCK
2/62H DELWP DELWPC EXITOA GFLOW SDOI SDOO PHP RSPA
3//62H 11 12 13 14 15 16 17 18
4//62H RADINS REWI REMO SDDI SDOO SLDI SLDO VELBI XWI
5//62H 19 20 21 22 23 24 25 26
6//56H XA2 VOL1 VOL2 TNOTOT BNDRAD ARATIO OUII UDOI//
FORMAT (1H,15X,28H*****
FORMAT (1H,15X,16X,1H*,26X,1H*)
FORMAT (1H,15X,16X,28H* CONDIP ENTERING DATA SET *)
FORMAT (1H,15X,17HNUMBER OF SECTORS,12X,18)
FORMAT (1H,15X,12HSECTOR WIDTH,18X,F9.1,10X,11HDEG. OF ARC)
FORMAT (1H,15X,24HNBUNDLE ORIENTATION ANGLE,6X,F9.1,7X,14HDEG. FRQ
1M VERT, (1H,15X,53H% OF TOTAL TUBES ASSIGNED TO COOLER IS PRCLR
1 F5.2//
FORMAT (1H,15X,19HNUMBER OF TUBE ROWS,13X,15)
FORMAT (1H,15X,32HNBUNDLE OF TUBES IN THE CONDENSOR,8X,F12.5)
FORMAT (1H,15X,20HNBUNDLE INSIDE RADIUS,12X,F10.4,16X,4HFEET)
FORMAT (1H,15X,11HTUBE LENGTH,19X,F10.2,5X,11X,4HFEET//)
FORMAT (1H,15X,37HFLAG FOR TUBE OD VARIATION IS MDIAM =,12)
FORMAT (1H,15X,20HTUBE INSIDE DIAMETER,9X,F10.4,14X,8HINCHES)
FORMAT (1H,15X,20HTUBE INSIDE DIAMETER,15X,13X,11HOUTSIDE ROW,7X,
1F10.2,14X,6HINCHES//)
FORMAT (1H,15X,10HTUBE INSIDE DIAMETER,17X,F10.2,14X,6HINCHES//)
FORMAT (1H,15X,36HFLAG FOR PITCH VARIATION IS MPITCH =,12)
FORMAT (1H,15X,40HFLAG FOR TUBE WALL INPUT UNIT IS WALL =,12)
FORMAT (1H,15X,26HTUBE CIRCUMFERENTIAL PITCH,4X,F10.2,11HOUTSIDE R
FORMAT (1H,15X,26HTUBE CIRCUMFERENTIAL PITCH,15X,13X,11HOUTSIDE R
1OW 7X,11H,15X,14X,10HINCHES//)
FORMAT (1H,15X,29HTUBE INSIDE DIAMETER,11X,F13.5,11X,6HINCHES)
FORMAT (1H,15X,19HTUBE WALL THICKNESS,10X,F10.3,11X,6HINCHES)
FORMAT (1H,15X,31H WALL THICKNESS,10X,F10.3,11X,6HINCHES)
FORMAT (1H,15X,25HTUBE WALL SPECIFIC WEIGHT,5X,F10.2,9X,8HMLB/FT**
13)
CONO 3850
CONO 3860
CONO 3870
CONO 3880
CONO 3890
CONO 3900
CONO 3910
CONO 3920
CONO 3930
CONO 3940
CONO 3950
CONO 3960
CONO 3970
CONO 3980
CONO 3990
CONO 4000
CONO 4010
CONO 4020
CONO 4030
CONO 4040
CONO 4050
CONO 4060
CONO 4070
CONO 4080
CONO 4090
CONO 4100
CONO 4110
CONO 4120
CONO 4130
CONO 4140
CONO 4150
CONO 4160
CONO 4170
CONO 4180
CONO 4190
CONO 4200
CONO 4210
CONO 4220
CONO 4230
CONO 4240
CONO 4250
CONO 4260
CONO 4270
CONO 4280
CONO 4290
CONO 4300
CONO 4310
CONO 4320

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320 1-HR-F) (1H ,15X,25HTUBE THERMAL CONDUCTIVITY,5X,F10.2,9X,11HBTU/FI CON04330
330 1-HR-F) (1H ,15X,19HTUBE FOULING FACTOR,11X,F13.5/ CON04340
340 1-HR-F) (1H ,15X,20HSTEAM FLOW RATE,9X,F9.0,16X,6HLBM/HR/ CON04350
350 1-HR-F) (1H ,15X,27HWEIGHT FRACTION OF N/C FLOW,3X,1PE13.5/ CON04360
360 1-HR-F) (1H ,15X,14HN/C GAS IS AIR/ CON04370
370 1-HR-F) (1H ,15X,25HN/C GAS IS CARBON DIOXIDE/ CON04380
380 1-HR-F) (1H ,15X,46HN/C GAS IS A MISTURE OF AIR AND CARBON DIOXIDE/ CON04390
390 1-HR-F) (1H ,15X,29HCOOLANT INJECTION TEMPERATURE,F10.1,16X,5HDEG F/ CON04400
400 1-HR-F) (1H ,15X,26HENTERING STEAM TEMPERATURE,4X,F9.2,16X,5HDEG F/ CON04410
410 1-HR-F) (1H ,15X,28HCHW FLOW SPECIFIER IS IFLOW =,12) CON04420
420 1-HR-F) (1H ,15X,22HCOOLANT MASS FLOW RATE,15X,F9.1,15X,6HLBM/HR/ CON04430
430 1-HR-F) (1H ,15X,16HCOOLANT VELOCITY,14X,F9.1,15X,6HFT/SEC/ CON04440
440 1-HR-F) (1H ,15X,21HCOOLANT PRESSURE DROP,9X,F11.3,16X,3HPS/ CON04450
450 1-HR-F) (1H ,15X,38HNO. OF INTERNAL ENHANCEMENT REGIONS IS,12) CON04460
460 1-HR-F) (1H ,15X,38HNO. OF EXTERNAL ENHANCEMENT REGIONS IS,12) CON04470
470 1-HR-F) (1H ,15X,26HFLAG FOR BAFFLE IS IBAF = ,15) CON04480
C ***** CON04490
C ***** CON04500
C ***** CON04510
C ***** CON04520
C ***** CON04530
C ***** CON04540
C ***** CON04550
C ***** CON04560
C ***** CON04570
C ***** CON04580
C ***** CON04590
C ***** CON04600
C ***** CON04610
C ***** CON04620
C ***** CON04630
C ***** CON04640
C ***** CON04650
C ***** CON04660
C ***** CON04670
C ***** CON04680
C ***** CON04690
C ***** CON04700
C ***** CON04710
C ***** CON04720
C ***** CON04730
C ***** CON04740
C ***** CON04750
C ***** CON04760
C ***** CON04770
C ***** CON04780
C ***** CON04790
C ***** CON04800

SUBROUTINE ORCON (ICALC)
ORC 1
SUBROUTINE ORCON
DIMENSION SIZE
X = NO. OF ROWS + 1
Y = NO. OF SECTORS
Z = NO. OF ENHANCEMENT REGIONS
TPAR(X) AOTFLW(X) RADIUS(X) TBNPR(X) VM(X) SID(X)
SECANG(Y) WGAS(Y) JBAF(Y+1)
ANT(X,Y) WS(X,Y) VEL(X,Y) PMIX(X,Y)
BC(Z) BE(Z) ENI(Z) ENO(Z) NETI(Z) NETE(Z)
NRNE(Z) NRNI(Z)
COMMON /GLOBCH/ ALST,DELWP,DELWPC,EXITQA,GFLOW,SID1,SIDU,PHP,RSPA,
1RADINS,REWI,REWO,SDD1,SDD2,SLDI,SLDO,VELBI,XW1,XW2,VOL1,VOL2,TNUTU,
2T,BNDRAD,ARATIO,JOI1,JOI2,SDDC,VLCMAX,PACCLR
COMMON /INPT/ BC(6),BE(6),ENH(6),ENI(6),ENO(6),FDOUL,PHI,SKW,STBI,SCON04780
1TSATI,TUBESW,WNCIR,IOPT,PSI(15),SECHID,IBAF,ISEC,JBAF(16),JGAS,MDCON04790
2IAH,MPITCH,NEE,NEI,NETE(6),NETI(6),NRNE(6),NRNI(6),NOROWS,WTST(15) CON04800
ZZZ ORC-1

```

```

3 WSI,PFILL
COMMON /OROL/ AOTFLW(100),SID(100),TBNPR(100),ADFLW(100),CMDUT(100)
10
COMMON /ORC2/ ANTI(100,15),STB2ES,VW(100)
COMMON /OUT/ DELOD,SM181,SM182,SMWB,SUMQ,TNO,VEL2,FR
COMMON /CONST/ AMWNC,CBI,CPB,PI,SG,IFIRST
COMMON /SEC/ ALMTD(100,15),PCUMDP(100,15),DELPL(15),GFLW(100,15),HEFCON(487)
1F(100,15),PMIX(100,15),PSA(100,15),QQA(100,15),RC(100,15),ROU(100,15)
20,15),SH(100,15),SHW(100,15),STSA(100,15),UN(100,15),VEL(100,15)
3 VNR(100,15),VPSHH(100,15),WCND(100,15),WGAS(15),WP(15),WS(100,15)
4 WSP(15)
COMMON /OUT2/ RCDOR,RSFF,PHPCON,VCLIC
DIMENSION TPAR(100),RADIUS(100),SECANG(15),BAFA(16)
C
C$-----
C ORC 2
C-----
DATA INITIALIZATION
AMWNC = MOLECULAR WEIGHT OF N/C GAS PRESENT
IFIRST IS A FLAG TO HETRN TO INDICATE FIRST EXECUTION
CBI = SALT CONCENTRATION OF COOLANT WT. PRCT
CPB = COOLANT SPECIFIC HEAT (UNITS?)
PTST AND WTST ARE CONSTRAINTS USED IN SEC-6
VW(1) = IS INITIALIZED AS A SEED FOR AN ITERATIVE
CALCULATION IN ORC-9
C
C-----
C ZZZ ORC-2
C-----
IF (ICALC.EQ.2) GO TO 20
SG=32.174
PY=3.14159
CBI=.035
CPB=1
SECFLG=FLOAT(1 SEC)
WNCI=WSI*WNCIR
A=1,10 I=1,1 SEC
DO 10 I=1,1 SEC
WS(1,1)=WSI/SECFLG*A
WGAS(1,1)=WNCI/SECFLG*A
IFIRST=1
IF (JGAS.EQ.1) AMWNC=28.965
IF (JGAS.EQ.2) AMWNC=44.
IF (JGAS.EQ.3) AMWNC=36.5
VW(1)=10.
GO TO 20
C$-----

```


CON06730
CON06740
CON06750
CON06760
CON06770
CON06780
CON06790
CON06800
CON06810
CON06820
CON06830
CON06840
CON06850
CON06860
CON06870
CON06880
CON06890
CON06900
CON06910
CON06920
CON06930
CON06940
CON06950
CON06960
CON06970
CON06980
CON06990
CON07000
CON07010
CON07020
CON07030
CON07040
CON07050
CON07060
CON07070
CON07080
CON07090
CON07100
CON07110
CON07120
CON07130
CON07140
CON07150
CON07160
CON07170
CON07180
CON07190
CON07200

```

TNOG=0.
TNOS=0.
TNR=0.
TDIFF=0.
SIDOF=SI00/12.
SIDIF=SID1/12.
IF (XW2.GT.0) ODOF=SIDOF+XW2/6.
IF (XW2.GT.0) ODI=SIDIF+XW2/6.
IF (XW2.LE.0) ODOF=SIDOF+(2*SIDOF*XW1)
IF (XW2.LE.0) ODI=SIDIF+(2*SIDIF*XW1)
OO1=ODOF*12.
OO1=ODIF*12.
DELODF=0.
DELOD=CELODF
CSPD=SDO*ODOF
CSP1=SDO1*ODIF
DELCSP=0.
RSPF=.866*(CSP0+CSP1)/2.
RSP=RSPP*12.
IF (RSPA.NE.0.) RSP=RSPA
RSPF=RSP/12.

      DETERMINE THE NUMBER OF TUBES IN THE CONDENSOR
      ALL SECTORS ARE IDENTICAL IN GEOMETRY
      BEGINNING WITH THE INNERMOST ROW, CALCULATE THE NUMBER
      OF ROWS IN THE CONDENSOR

I=1
NOROWS=1
TNO=TNUT*(100.-PRCCLR)/100.
RADIUS(1)=RADINS
SID(1)=SIDOF
TNR=(ARCPR*RADIUS(1))/CSPD
TNOS=TNOS+TNR

      CHECK TO ENSURE THAT THE NUMBER OF TUBES IN THE SECTOR
      HAS NOT EXCEEDED THE NUMBER OF TUBES AVAILABLE

IF (TNOS.LT.(TNO/SECFLG)) GO TO 70
TNOS=TNOS-TNR
TNOC=TNOS*SECFLG
TDIFF=TNO-TNOC
TNPR(1)=TDIFF/SECFLG
PEILL=TNPR(1)/TNR
GO TO 80

TPAR(1)=1./(CSPD*RSPF)

```

C C C C C C 60 C C C C 70

```

C      ADFLW(I)=(CSPO-ODOF)*TNR
C      AOTFLW(I)=AOLFLW(I)*ALST
C      TBNPR(I)=TNR
C      RADIUS(I+1)=RADIUS(I)+RSPF
C      I=I+1
C      NOROWS=NOROWS+1
C
C      CHECK TO SEE THAT THE NUMBER OF ROWS DOESNOT EXCEED 199
C      BECAUSE 200 IS THE LIMIT FOR THE DIMENSIONS OF NUMEROUS ARRAYS
C
C      IF (NOROWS.LT.100) GO TO 60
C      ERR1=TNO-(TNO*SECFLG)
C      TNO=TNO*SECFLG
C      WRITE (6,640)
C      NOROWS=NOROWS-1
C      GO TO 90
C
C      IF LAST ROW IS INCOMPLETE, FIND ITS PERTINENT GEOMETRY
C
C      SDDL=(RADIUS(I)*ARCPR)/(ODOF*TBNPR(I))
C      CSPL=SDCL*ODOF
C      TPAR(I)=1/(CSPL*RSPF)
C      ADFLW(I)=(CSPL-ODOF)*TBNPR(I)
C      AOTFLW(I)=AOLFLW(I)*ALST
C      TNO=TNO+TBNPR(I)
C      CONTINUE
C      AHOLE=PI*(ODOF**2)*TNO/4.
C      ROWS=FLCAT(NOROWS)
C      BNDRAD=RADINS+RSPF*(ROWS-1.)
C
C      THIS NEXT SUBROUTINE SWITCHES THE ARRAYS SO THE ARRAY VALUES
C      START WITH THE OUTSIDE ROW AND WORK TOWARDS THE CENTER.
C      THIS WILL MAKE THE GEOMETRY VALUES COMPATIBLE WITH THE REST
C      OF THE PROGRAM.
C
C      CALL SWITCH (RADIUS,NOROWS)
C      CALL SWITCH (SID,NOROWS)
C      CALL SWITCH (TBNPR,NOROWS)
C      CALL SWITCH (TPAR,NOROWS)
C      CALL SWITCH (AOLFLW,NOROWS)
C      CALL SWITCH (AOTFLW,NOROWS)
C
C      CONTINUE
C
C      AOTFLW(NOROWS+1)=ALST*(RADINS-SDI*ODI/24.)*PI/6.
C      IF (ISEC.EQ.1) SECANG(1)=PHI

```

```

CON07210
CON07220
CON07230
CON07240
CON07250
CON07260
CON07270
CON07280
CON07290
CON07300
CON07310
CON07320
CON07330
CON07340
CON07350
CON07360
CON07370
CON07380
CON07390
CON07400
CON07410
CON07420
CON07430
CON07440
CON07450
CON07460
CON07470
CON07480
CON07490
CON07500
CON07510
CON07520
CON07530
CON07540
CON07550
CON07560
CON07570
CON07580
CON07590
CON07600
CON07610
CON07620
CON07630
CON07640
CON07650
CON07660
CON07670
CON07680

```

```

IF (ISEC.EQ.1) GO TO 110
FCWID=SECMID*(SECFLG-1.)
DO 110 I=1,ISEC
  SECA=(PI-FCWID/2.)*SECMID*(I-1)
  IF (SECA.GT.360.) SECA=SECA-360.
  SECANG(I)=SECA
DUMMY=ALST*PI*SECMID*SECFLG/360.
BNDRA1=BNDRAD
VOL1=DUMMY*BNDRA1**2
VOLLIC=VCL1
      IF TNOTOT IS A DESIGN VARIABLE THEN THE INCREASE OF VOLUME AND
      OUTSIDE BUNDLE RADIUS MUST BE A GRADUAL PROCESS AND NOT A STEP
      INCREASE OR DECREASE
IF (IOPT.EQ.1) GO TO 120
RCORR=RSPF
PCORR=RCORR*((1.-PFI))
BNDRAD=BNDRAD-RCORR
VOL1=DUMMY*BNDRAD**2
VOLLIC=VCL1
VOL2=DUMMY*(BNDRAD**2-RADINS**2)
      COMPUTE THE AREA RATIO WHICH IS THE AREA OF TUBE HOLES DIVIDED
      BY THE TUBE SHEET AREA
TSAREA=PI*(BNDRAD**2)*SECFLG*SECMID/360.
ARATIO=AHOLE/TSAREA
A4-----
TEMP OUTPUT SECTION
THIS SECTION FOR DEBUGGING AID
ORC-A4-----
ORCA4=0.
IF (ORCA4.NE.1.) GO TO 150
WRITE(6,650)
WRITE(6,660)
WRITE(6,700)
WRITE(6,670)
WRITE(6,700)
WRITE(6,680)
WRITE(6,700)
WRITE(6,700)

```

[illegible]

CUN08650
 CUN08660
 CUN08670
 CUN08680
 CUN08690
 CUN08700
 CUN08710
 CUN08720
 CUN08730
 CUN08740
 CUN08750
 CUN08760
 CUN08770
 CUN08780
 CUN08790
 CUN08800
 CUN08810
 CUN08820
 CUN08830
 CUN08840
 CUN08850
 CUN08860
 CUN08870
 CUN08880
 CUN08890
 CUN08900
 CUN08910
 CUN08920
 CUN08930
 CUN08940
 CUN08950
 CUN08960
 CUN08970
 CUN08980
 CUN08990
 CUN09000
 CUN09010
 CUN09020
 CUN09030
 CUN09040
 CUN09050
 CUN09060
 CUN09070
 CUN09080
 CUN09090
 CUN09100
 CUN09110
 CUN09120

```

190      IT=JBFAF(1)
      BAFA(1)=PHI1-FCW1+SECI*FLOAT(IT-1)
      GO TO 210
200      BAFA(1)=PHI1-FCW1
      BAFA(2)=PHI1+FCW1
      IBAF=2
      JBFAF(1)=1
      JBFAF(2)=ISEC+1
      CONTINUE
210 C-----
C$ ORC A5
C
C ZZZ ORC-A5
C-----
      ORCA5=9
      IF (ORCA5,NE,1) GO TO 240
      WRITE (6,750) IBAF,IBAF
      WRITE (6,770)
      DO 220 I=1,IBAF
      WRITE (6,780) I,JBFAF(I)
220      WRITE (6,790)
      DO 230 I=1,IBAF
      X=BAFA(I)*180./PI
230      WRITE (6,800) X,BAFA(I)
240      CONTINUE
C$-----
C$ ORC 6
C
C ZZZ ORC-6
C-----
      DO 430 IS=1,ISEC
      SECA=SECANG(1S)*PI/180.
      SEC=PI/2.-SECA
      IF ((SECA.GT.0.) .AND. (SECA.LT.PI)) GO TO 270
      DO 250 I=1,IBAF
      BAFAI=BAFA(I)
      IF (BAFAI.GT.SECA) GO TO 260
      CONTINUE
250      BAFAI=PI/2.-BAFAI
260      IF ((BAFAI.GT.0.) .AND. (SECA.LT.0.)) BAFAI=PI/2.
      GO TO 300
270      DO 280 I=1,IBAF
      J=IBAFI+1-I
      BAFAI=BAFA(J)
      IF (BAFAI.LT.SECA) GO TO 290
      CONTINUE
280

```

LOCATE ACTIVE BAFFLE FOR EACH SECTOR


```

BAF=PI/2.
GO TO 300
BAF=PI/2.-BAFAT
CONTINUE
IF (BAFAT.LT.0.) BAF=PI/2.

C$-----
C  ORC A6
C  ZZZ ORC-A6
C-----
ORCA6=C
IF (ORCA6.NE.1.) GO TO 310
WRITE (6,810)
WRITE (6,820)
X=SEC*180./PI
WRITE (6,830)
X=BAF*180./PI
WRITE (6,840) X,BAF
CONTINUE

310-----
C$ ORC 7
C-----

```

TEMP OUTPUT SECTION

```

C-----
C  ZZZ ORC-A6
C-----

```

CALCULATE FLOWING FACTORS

```

AN = SUMMING REGISTER FOR NO. OF TUBES
ANT = NO. OF TUBES OVER THE TARGET TUBE
BAF = ANGLE ABOUT HORIZONTAL OF 1ST BAFFLE ABOVE CURRENT SECTOR
DELODF = SEE ORC-4
D1 = FARTHEST DIST FROM HORIZONTAL TO CURRENT ROW INTERSECTION
D2 = SHORTEST DIST FROM HORIZONTAL TO CURRENT ROW INTERSECTION
IR = ROW NO. OF CURRENT TARGET TUBE
IS = SECTOR NO. OF CURRENT TARGET TUBE
ITR = ROW NO. OF 1ST ROW TO BE SUMMED IN UPPER QUADRANT
I1 = ROW WHOSE CONTRIB TO ANT IS BEING CALCULATED
I2 = LOOP COUNTER IN UPPER QUADRANT CALCULATION
NOROWS = NO. OF ROWS IN THE CONDENSER
OD = TUBE OD IN ROW BEING CONDENSED - FT
ODDF = TUBE DIA METER IN OUTERMOST (IR = 1) ROW OF TUBES
RADDIUS = RADIUS OF EACH TUBE ROW - FT
RSPF = ROW RADIAL SEPARATION - FT
R1 = RADIUS OF UPPER OR LOWER BOUNDARY OF ROW 1
SEC = ANGLE FROM HORIZONTAL OF CURRENT SECTOR MIDPOINT
SECA = ANGLE FROM HORIZONTAL OF CURRENT SECTOR MIDPOINT
TEST = TEST FOR VERTICAL BAFFLES
TPAR = TUBE DENSITY PER UNIT AREA PFOR EACH ROW - TUBES/FT**2
XC = HORIZONTAL DIST OR CURRENT TUBE FROM COND CENTER
XCS = XC SQUARED
YC = VERTICAL (+/-) DIST OF CURRENT TUBE FROM COND CNTR - FT

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C      ZT = VERT DIST FROM TARGET TUBE TO BAFFLE INTERSECTION - FT
C      ZZZ ORC-7
C-----
      ORCA7=0.
      IF (ORCA7.EQ.1.) WRITE (6,860)
      DO 420 IR=1,NROWS
      IF (IS.EQ.1SEC.AND.IR.GE.20)ORCA7 = 1.
      ITR=IR
      AN=0.
      DD=DDOF-DELODF*FLOAT(IR-1)
      RI=RADIUS(IR)
      YC=RI*SIN(SEC)
      XC=RI*CCS(SEC)
      XCS=XC*XC
      TEST=ABS(ABS(BAF)-PI/2.)
      X=DD*12.
      IF (ORCA7.EQ.1.) WRITE (6,870) IR,IS
      IF (ORCA7.EQ.1.) WRITE (6,880) X,RI,YC,XC,TEST
      ZT=1E10
      GO TO 330
      GO TO 330
      ZT=XC*TAN(BAF)
      XC=ABS(XC)
      IF (YC.GT.0.) GO TO 370
      IF (ORCA7.EQ.1.) WRITE (6,890) ZT
      D1=YC
      DO 340 I1=1,NROWS
      RI=RADIUS(I1-RSPF/2.
      IF (RI.LE.XC) GO TO 350
      D2=-1.*SQRT(RI*RI-XCS)
      IF (ORCA7.EQ.1.) WRITE (6,900) I1,RI,D2
      IF (D2.GT.ZT) GO TO 360
      IF (ORCA7.EQ.1.) WRITE (6,910)
      AN=AN+(D2-D1)/(RSPF*2.)
      IF (ORCA7.EQ.1.) WRITE (6,920) D1,D2,AN
      D1=D2
      CONTINUE
      D2=-D2
      IF (ORCA7.EQ.1.) WRITE (6,940)
      IF (D2.GT.ZT) GO TO 410
      ITR=NORCWS
      D1=D2
      IF (ORCA7.EQ.1.) WRITE (6,950)
      GO TO 380
      AN=AN-D1/(RSPF*2.)
      D1=0.
      ITR=I1

```

CON1 0090
CON1 0100
CON1 0110
CON1 0120
CON1 0130
CON1 0140
CON1 0150
CON1 0160
CON1 0170
CON1 0180
CON1 0190
CON1 0200
CON1 0210
CON1 0220
CON1 0230
CON1 0240
CON1 0250
CON1 0260
CON1 0270
CON1 0280
CON1 0290
CON1 0300
CON1 0310
CON1 0320
CON1 0330
CON1 0340
CON1 0350
CON1 0360
CON1 0370
CON1 0380
CON1 0390
CON1 0400
CON1 0410
CON1 0420
CON1 0430
CON1 0440
CON1 0450
CON1 0460
CON1 0470
CON1 0480
CON1 0490
CON1 0500
CON1 0510
CON1 0520
CON1 0530
CON1 0540
CON1 0550
CON1 0560

```

IF (ORCA7.EQ.1.) WRITE (6,930) AN, ITR
GO TO 380
AN=AN+(ZT-D1)/(RSPF*2.)
IF (ORCA7.EQ.1.) WRITE (6,960)
GO TO 410
D1=YC
IF (ORCA7.EQ.1.) WRITE (6,970) D1
DO 390 I=1, ITR
  I1=ITR-I2+1
  R1=RADIUS(I1)+RSPF/2.
  D2=SQRT(R1*R1-XCS)
  IF (ORCA7.EQ.1.) WRITE (6,980) IR, I1, R1
  IF (ORCA7.EQ.1.) WRITE (6,990) D1, D2, ZT
  IF (D2.GT.ZT) GO TO 400
  AN=AN+(D2-D1)/(RSPF*2.)
  IF (ORCA7.EQ.1.) WRITE (6,1000) AN
  D1=D2
GO TO 410
AN=AN+(ZT-D1)/(RSPF*2.)
IF (ORCA7.EQ.1.) WRITE (6,1010)
NF=AN+1.0
RNF=NF
ANT (IR, I, IS)=RNF
IF (ORCA7.EQ.1.) WRITE (6,1020) IS, IR, AN
CONTINUE
ORCA7=0.
IF (ORCA7.NE.1.) GO TO 450
DO 440 I=1, NOROWS
  WRITE (6,850) I, (ANT(I, J), J=1, ISEC)
CONTINUE
C$-----
C$ ORC 9
C$-----
PUMPING POWER CALCULATION
ALST = TUBE LENGTH FT
AI = COEF IN FF CALCULATION
BI = EXP IN FF CALCULATION
CBI = COOLANT SALT CONCENTRATION IN WT PRCNT
CMOT = COOLANT MASS FLOW/TUBE IN EACH ROW LBM/SEC
CMTOT = TOTAL COOLANT MASS FLOW THROUGH CONDENSER LBM/SEC
DELWP = HEADER PRESSURE DIFFERENCE PSI
FF = TUBE FRICTION FACTORS
HEAD = FT*2/SEC**
SID = STORED INNER TUBE DIAMETER
TID = TEMPORARY VALUE FOR TUBE INNER DIAMETER
SLD = STORED LENGTH/TUBE INNER DIAMETER RATIO
SLDO = SLD RATIO OF TUBES IN OUTER ROW

```


CON11050
CON11060
CON11070
CON11080
CON11090
CON11100
CON11110
CON11120
CON11130
CON11140
CON11150
CON11160
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CON11180
CON11190
CON11200
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CON11230
CON11240
CON11250
CON11260
CON11270
CON11280
CON11290
CON11300
CON11310
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CON11330
CON11340
CON11350
CON11360
CON11370
CON11380
CON11390
CON11400
CON11410
CON11420
CON11430
CON11440
CON11450
CON11460
CON11470
CON11480
CON11490
CON11500
CON11510
CON11520

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500 IF (REW.GE.51904.4) GO TO 500
    AL=.3164
    BI=-.25
    GO TO 510
510 AL=.184
    BI=-.2
    CONTINUE
    IF (ORCA9.EQ.1.) WRITE (6,1070) AL,BI,REW
    HLOSS=(1.1+FF*SLO)
    IF (ORCA9.EQ.1.) WRITE (6,1080) FF,SLO,HLOSS,HEAD
    VG1=SQRTH(HEAD/HLOSS)
    TEST=ABS(VG-VG1)/VG
    IF (ORCA9.EQ.1.) WRITE (6,1090) TEST,VG,VG1
    VG=VG1
    IF (TEST.GT.0.01) GO TO 490
    IF (IR.EQ.1) REMO=REW
    IF (IR.EQ.NORDWS) REWI=REW
    CM DOT (IR)=PI*TID**2*VG*RHOW/4.
    VW (IR)=VG
    CM TOT=SECFLG*CM DOT (IR)*TBNPR (IR)+CMTOT
    PHPCON=PHP
    DELMPC=DELP
    GO TO 600
520 A=0.540 IR=1.NORDWS
    TID=SI C (IR)
    IF (IR.EQ.1) SLD=ALST/TID
    IF (IR.EQ.NORDWS) SLDI=ALST/TID
    A=A+TID*PI*TBNPR (IR)/4.
    SLD=(SLD+SLDI)/2.
    TID=ALST/SLD
    IF (GFLOW.LE.0.) GO TO 550
    VX=GFLOW/((RHOW*A*SECFLG)*3600.)
    CM TOT=GFLOW/3600.
    GO TO 560
    CM TOT=VELBI*RHOW*A*SECFLG
    VX=VELBI
    REW=VX*TID/XNJW
    IF (REW.GT.51904.4) GO TO 570
    FF=.3164*REW**(-.25)
    GO TO 580
    FF=.184*REW**(-.2)
    DELMPC=(1.1+FF*SLD)*VX**2*RHOW/(2.*SG*144.)
    DO 590 IR=1,NORDWS
    CM DOT (IR)=PI*SID (IR)**2*VX*RHOW/4.
    VW (IR)=VX
530
540
550
560
570
580
590

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CON11530
CON11540
CON11550
CON11560
CON11570
CON11580
CON11590
CON11600
CON11610
CON11620
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CON11640
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CON11670
CON11680
CON11690
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CON11800
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CON11870
CON11880
CON11890
CON11900
CON11910
CON11920
CON11930
CON11940
CON11950
CON11960
CON11970
CON11980
CON11990
CON12000

REMO=VX*SID(I)/XNUM
REMI=VX*SID(NROWS)/XNUM
HEAD=2*DELWPC*144*(SG/RHOW
PHP=CHTCT*DELWPC*144/(RHOW*550.)
PHPCON=PHP
DELWPC=DELWPC
CONTINUE
HFG=HFGFN(STSAT1)
STB2ES=(WSI*HFG)/(CPB*CMTUT*3600.*1*STBI

600

C\$

C ORC A9

C ZZZ ORC-A9

TEMP OUTPUT SECTION

ORCA9=0
IF (ORCA9.NE.1.) GO TO 630
WRITE (6,1100) RHOW
WRITE (6,1110) XNUM
WRITE (6,1120) XNUM
WRITE (6,1130) HEAD
WRITE (6,1140) HEAD
WRITE (6,1150) DELWPC
WRITE (6,1160) DELWPC
WRITE (6,1170) SLDI,SLDO
WRITE (6,1180) REMI,REMO
WRITE (6,1190) CMTOT
WRITE (6,1200) PHP
WRITE (6,1210) QWS
DO 610 I=1,NORQWS
WRITE (6,1220) I,VW(I)
DO 620 I=1,NORQWS
WRITE (6,1220) I,CMDOT(I)
CONTINUE

610

620

630

C\$

C ORC 10

C ZZZ ORC-10

CALL TO SECALC

CALL SECALC (ARCPR,DELODF,ODIF,ODOF)

RETURN
FORMAT (1H0,24H THE NUMBER OF ROWS EXCEEDS THE MAXIMUM ALLOWED)
FORMAT (1H0,10H OUTFUT SECTION FOR ORC-4)
FORMAT (1H0,10H ODOF
FORMAT (1H0,10H CSPI
FORMAT (1H0,10H RSP
FORMAT (1H0,10H AHLES
FORMAT (1H,3F10.5)
FORMAT (1H0,10H AOTFLW
FORMAT (1H0,10H RADIUS
FORMAT (1H0,10H BNPR
FORMAT (1H0,10H TPAR

640

650

660

670

680

690

700

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720 1) FORMAT (1H0,10HSECANG , )
730 1) FORMAT (1H ,F10.6)
740 1) FORMAT (1H ,F10.5)
750 1) FORMAT (1H1,24HOUTPUT FOR SECTION ORC-5)
760 1) FORMAT (1H0,7HIBAF = ,I4,5X,8HIBAFI = ,I4)
770 1) FORMAT (1H0,22HFOR I = ,I4)
780 1) FORMAT (1H ,3X ,I4,8X ,I4)
790 1) FORMAT (1H0,36HBAFFLE ANGLES IN DEGREES AND RADIAN)
800 1) FORMAT (1H ,3X ,F6.1,3X ,F6.4)
810 1) FORMAT (1H1,24HOUTPUT FOR SECTION ORC-6)
820 1) FORMAT (1H0,50HANGLES ARE MEASURED CNTR-CLK WISE FROM HORIZONTAL)
830 1) FORMAT (1H0,16HCURRENT SECTOR = ,I3,16H ANGLE IN DEG = ,F6.1,21H A
      INGLE IN RADIAN = ,F6.4)
840 1) FORMAT (1H0,32HANGLE OF ACTIVE BAFFLE IN DEG. = ,F6.1,14H IN RADIA
      INS = ,F6.4)
850 1) FORMAT (1H ,13,2X,6(F5.2,2X) )
860 1) FORMAT (1H0,28H*** OUTPUT FOR ORC-7 *** )
870 1) FORMAT (1H0,5HROW = ,I4,11H SECTOR = ,I4)
880 1) FORMAT (1H ,4HOD = ,F6.4,10H RADIUS = ,F6.2,6H XC = ,
      TEST = ,E10.3)
890 1) FORMAT (1H0,36HTARGET TUBE IN LOWER QUADRANT, ZI = ,F20.4)
900 1) FORMAT (1H ,15HLOWR QUAD - ROW = ,I3,5H RI = ,F7.3,5H D2 = ,F7.3)
910 1) FORMAT (1H ,18HBAFFLE WAS NOT HIT)
920 1) FORMAT (1H ,15HSTILL LWR - DI = ,F7.3,5H D2 = ,F7.3,5H AN = ,F6.2)
930 1) FORMAT (1H ,34HPASSING INTO UPPER QUADRANT - AN = ,F6.2,15H CURREN
      IT ROW = ,I4)
940 1) FORMAT (1H ,30HMOVING THRU VOID TO UPPER QUAD)
950 1) FORMAT (1H ,22HBAFFLE NOT HIT IN VOID)
960 1) FORMAT (1H ,28HBAFFLE HIT IN LOWER QUADRANT)
970 1) FORMAT (1H ,35HTARGET TUBE IS IN UPPER QUAD - DI = ,F8.4)
980 1) FORMAT (1H ,37HCALCULATING IN UPPER QUAD - TRGET RW = ,I4,12H CALC
      ROW = ,I4,11H CORR RAD = ,F8.4)
990 1) FORMAT (1H ,4HDI = ,F6.3,6H D2 = ,F6.3,6H ZI = ,E10.3)
1000 1) FORMAT (1H ,34HUPPER QUAD - BAFFLE NOT HIT - AN = ,F6.2)
1010 1) FORMAT (1H ,23HUPPER QUAD - BAFFLE HIT)
1020 1) FORMAT (1H0,26H** FINAL FOR TARGET ** IS = ,I4,4H IR = ,I4,5H ANT = ,F8.
      12)
1030 1) FORMAT (1H ,16HAT DO LOOP - IR = ,I4)
1040 1) FORMAT (1H ,9HTEMP IR = ,I4,7H ITEM = ,I4,5H VG = ,E10.3)
1050 1) FORMAT (1H ,16HABOVE 380 - TID = ,E10.3,6H SLD = ,E10.3,5H IR = ,I4)
1060 1) FORMAT (1H ,16HBELOW 380 - REW = ,E10.3,6H TID = ,E10.3,7H XNUM = ,E10
      1,3)
1070 1) FORMAT (1H ,12HAT 400 - A1 = ,E10.3,5H B1 = ,E10.3,6H REW = ,E10.3)
1080 1) FORMAT (1H ,3HFF = ,E10.3,5H SLD = ,E10.3,7H HLCSS = ,E10.3,6H HEAD = ,E10
      1,3)
1090 1) FORMAT (1H ,5HTEST = ,E10.3,5H VG = ,E10.3,6H VGL = ,E10.3)
1100 1) FORMAT (1H1,16HOUTPUT FOR ORC-9)

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1110 FORMAT (1H,8H RHG = ,E10.3,10H LBM/FT**3) CON12490
1120 FORMAT (1H,8H MU = ,E10.3,10H LBM/SEC-FT) CON12500
1130 FORMAT (1H,8H NU = ,E10.3,10H FT**2/SEC) CON12510
1140 FORMAT (1H,8H HEAD = ,E10.3,13H FT**2/SEC**2) CON12520
1150 FORMAT (1H,8H REW = ,E10.3,3X,6HFF = ,E10.3) CON12530
1160 FORMAT (1H,8H DELWLP = ,E10.3,4H,PSI) CON12540
1170 FORMAT (1H,39H LENGTH = ,F6.2) CON12550
1 OUTSIDE ROW = ,F6.2) CON12560
1180 FORMAT (1H,27H REYNOLDS NO. - INSIDE ROW = ,E10.3,15H OUTSIDE ROW CON12570
1 = ,E10.3) CON12580
1190 FORMAT (1H,24H COOLANT MASS FLOW RATE = ,F15.3,8H LBM/SEC) CON12590
1200 FORMAT (1H,24H PUMPING POWER REQUIRED = ,F10.2,3H HP) CON12600
1210 FORMAT (1H,37H COOLANT VELOCITY IN EACH ROW = FT/SEC) CON12610
1220 FORMAT (1H,14,3X,F10.3) CON12620
END CON12630
C***** CON12640
C***** CON12650
C***** CON12660
C***** CON12670
C***** CON12680
C***** CON12690
C***** CON12700
C***** CON12710
C***** CON12720
C***** CON12730
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C***** CON12770
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C***** CON12950
C***** CON12960
C***** CON12970
C***** CON12980
C***** CON12990
C***** CON13000

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CON12970
CON12980
CON12990
CON13000
CON13010
CON13020
CON13030
CON13040
CON13050
CON13060
CON13070
CON13080
CON13090
CON13100
CON13110
CON13120
CON13130
CON13140
CON13150
CON13160
CON13170
CON13180
CON13190
CON13200
CON13210
CON13220
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CON13290
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CON13350
CON13360
CON13370
CON13380
CON13390
CON13400
CON13410
CON13420
CON13430
CON13440

4) HSP(15)
COMMON /CONST/ AMWNC,CBI,CPB,PI,SG,IFIRST
COMMON /COOL1/ VELC(100),PMIXC(100),PSATC(100),WSC(100)
1) ALMTDC(100),SHMC(100),SHNFC(100),RCC(100),ROUTC(100),VNKEC(100)
2) VPSHC(100),HEFFC(100),UNC(100),WCNDC(100),GLOWC(100),QDAC(100)
3) SUMDPC(100)
COMMON /COOL2/ IVNOC,HNOC,INOC,TSATEX,PMXEXT,AMLEX,WMSEXIT,VELEXT,T
1B2C,ENHIC,ENHOC,ENHFC,SHWINC,WBC
DIMENSION C(15)

SEC 2

CC

INITIALIZE :OLD ORC 8,9
PART - 1

ALST = TUBE LENGTH FT
AMOLNC = TOTAL MOLES OF N/C GAS ENTERING CONDENSER
AMOLSS = MOLES OF STM ENTERING COND
AMOLST = SUM OF MOLES OF STM AND N/C ENTERING COND
AMWNC = MOLECULAR WEIGHT OF N/C
ANAT = TOTAL NO OF TUBE IN 360 DEG COND
ARCPR = RATIO OF OUTSIDE ROW MIN FLOW AREA TO SECTOR FACE AREA
ADTFW = CIRCUMFERENTIAL ARC LENGTH PER UNIT RADIUS
BNDRAD = AREA OPEN TO FLOW IN A ROW OF TUBES IN A SECTOR FT*2
DELODF = TUBE BUNDLE OD PER ROW FT
DELODF = CHANGE IN TUBE OD PER ROW FT
DELP12 = ENTRANCE STM PRESS LOSS PSI
DELP23 = STM PRESS LOSS AS STM IS ACCEL INTO FIRST ROW PSI
G2 =
HFG = STEAM LATENT HEAT OF VAPORIZATION BTU/LBM
NOROWS = NO. OF ROWS IN THE CONDENSER
ODOFF = TUBE OD, OUTSIDE ROW FT
ODQIF = TUBE OD, INSIDE ROW FT
ODQI1 = TUBE OD, OUTSIDE ROW IN
ODQI1 = TUBE OD, INSIDE ROW IN
PMIX1 = PRESS OF STM - N/C MIXTURE ENTERING COND PSIA
PSATI = ENTERING STEAM SAT PRESSURE PSIA
PTLIM = LOWEST SATURATION TEMPERATURE FALLS BELOW INLET
PTLIM = CORRESPONDING SATURATION TEMPERATURE FALLS BELOW INLET
RADIUS = CONDENSER RADIUS FT
RADIUS = BUNDLE VOID RADIUS FT
ROWS = NO OF ROWS IN THE CONDENSER
SECFAR = FACE AREA FOR ONE SECTOR
SECFLG = NO. OF SECTORS IN THE CONDENSER MODEL
SMTB1 = ROW BY ROW SUM OF (COOLANT INLET TEMP * FLOW RATE)
SMTB2 = ROW BY ROW SUM OF (COOLANT FLOW
SUMC = ROW BY ROW SUM OF (COOLANT GUTLET TEMP * FLOW RATE)
SG = GRAVITY FACTOR 32.2

CON13450
CON13460
CON13470
CON13480
CON13490
CON13500
CON13510
CON13520
CON13530
CON13540
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CON13580
CON13590
CON13600
CON13610
CON13620
CON13630
CON13640
CON13650
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CON13670
CON13680
CON13690
CON13700
CON13710
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CON13730
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CON13790
CON13800
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CON13820
CON13830
CON13840
CON13850
CON13860
CON13870
CON13880
CON13890
CON13900
CON13910
CON13920

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C  STSAT1 = ENTERING STM SAT TEMP F
C  SVMIX1 = ENTERING MIXTURE SPECIFIC VOL FT**3/LBM
C  SVNCL1 = ENTERING N/C GAS SATURATION TEMP FT**3/LBM
C  TSAT1 = ENTERING STEAM SATURATION TEMP R
C  WGA1 = N/C GAS FLOW TO EACH CONDENSER LBM/HR
C  WNC1 = N/C GAS FLOW TO CONDENSER LBM/HR
C  WNC1R = RATIO OF MASS FLOW OF N/C TO MASS FLOW OF STEAM
C  WS1 = STEAM FLOW TO EACH SECTOR LBM/HR
C  WS1 = TOTAL STM FLOW TO CONDENSER LBM/HR
C  VEL1 = MIXTURE VELOCITY PRIOR TO ENTERING FIRST ROW FT/SEC
C  VEL2 = MIXTURE VELOCITY IN FIRST ROW OF TUBES FT/SEC
C  IVNOC = THE NUMBER OF VERTICAL TUBES IN THE COOLER
C  IHNOC = THE NUMBER OF HORIZONTAL TUBES IN THE COOLER
C  HTC1R = THE HEIGHT OF THE COOLER FT**3/LBM
C  VGI = ENTERING STM SPECIFIC VOL FT**3/LBM

C 222 SEC-2
C  ROWS=FLOAT(NROWS)
C  TNOC=0.
C  IVNOC=1.
C  IF (PRCCLR.EQ.0.0) GO TO 10
C  COMPUTE THE NUMBER OF VERTICAL AND HORIZONTAL ROWS IN THE COOLER
C  IF THERE IS ONE
C  SDDC=SDDI
C  TNOC=(PRCCLR/(100.-PRCCLR))*TNOC
C  HTC1R=BNDRAD-RADINS
C  VNOC=(HTCLR/(SDDC*ODIF*0.886))+1.
C  IHNOC=TNOC/VNOC
C  HNOC=FLOAT(IHNOC)
C  VNOC=TNOC/HNOC
C  IVNOC=VNOC+.5
C  VNOC=FLOAT(IVNOC)
C  KSTOP=NCROWS+1
C  SECFLG=FLOAT(1 SEC)
C  WNCI=WS1*WNC1R
C  IPLOOP=0
C  WSAVE=(WS1+WNCI)/SECFLG
C  INITIALIZE TEST VARIABLES TO 0
C  CONTINUE
C  STMSUM=0.
C  WTSV=0.

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CON1 3530
CON1 3940
CON1 3950
CON1 3960
CON1 3970
CON1 3980
CON1 3990
CON1 4000
CON1 4010
CON1 4020
CON1 4030
CON1 4040
CON1 4050
CON1 4060
CON1 4070
CON1 4080
CON1 4090
CON1 4100
CON1 4110
CON1 4120
CON1 4130
CON1 4140
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CON1 4270
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CON1 4330
CON1 4340
CON1 4350
CON1 4360
CON1 4370
CON1 4380
CON1 4390
CON1 4400

STBIR=STBI+459.69
PTLIM=PSATFN(STBIR)
TSATI=TSATI+459.69
PSATI=PSATFN(TSATI)
AMOLNC=LNCI/AMWNC
HFG=HFGFN(STSATI)
AMOLSS=WSI/18.015
AMOLST=AMOLSS+AMOLNC
PMIXI=PSATI*(AMOLST/AMOLSS)
VGI=VGFN(TSATI,PMIXI)
SVNCI=10.729*TSATI*(AMWNC*PMIXI)
SVMIXI=1.0/(AMOLSS/(AMOLST*VGI)+AMOLNC/(SVNCI*AMOLST))
G2=288.0*SG*SVMIXI
SMTBI=0.0
SMWB=0.0
WB=0.
SMTB2=0.0
SMHQ=0.0
CUMDRY=0.
SUBFLO=0.
NBAD=0
WCNDAY=0.
SUBAVE=0.

COMPUTE THE PRESSURE LOSSES AT THE ENTRANCE OF THE SECTOR

SECFAR=ARCP*(BNDRAD+ODOF/2.)*ALST
ARAT=AOTFLW(1)/SECFAR
VEL1=(WSI+WNCI)*SVMIXI/(3600.0*SECFAR*SECFLG)
VEL2=VEL1/ARAT
IF (ARAT-0.715) 30,30,40
DELP12=0.4*(1.25-ARAT)*VEL2**2/G2
GO TO 50
DELP12=0.75*(1.0-ARAT)*VEL2**2/G2
DELP23=(VEL2**2-VEL1**2)/G2

TEMP OUTPUT SECTION

SEC A2

ZZZ SEC-A2

SECA2=0.
IF (SECA2.EQ.0.) GO TO 70
DO 60 I=1,ISEC
WRITE (6,610)
WRITE (6,620) WSI,WNCI

CON14410
CON14420
CON14430
CON14440
CON14450
CON14460
CON14470
CON14480
CON14490
CON14500
CON14510
CON14520
CON14530
CON14540
CON14550
CON14560
CON14570
CON14580
CON14590
CON14600
CON14610
CON14620
CON14630
CON14640
CON14650
CON14660
CON14670
CON14680
CON14690
CON14700
CON14710
CON14720
CON14730
CON14740
CON14750
CON14760
CON14770
CON14780
CON14790
CON14800
CON14810
CON14820
CON14830
CON14840
CON14850
CON14860
CON14870
CON14880

```

60 70 65-----
      SEC 3
      WS(1,I),WGAS(I)
      HFG,AOTFLW(I)
      TSAT1,STSAT1
      PSAT1,PMIX1
      AMOLNC,AMOLSS,AMULST
      SVNC1,SVNIX1
      VGI,G2
      SECFAR,ARAT
      VELL,VEL2
      DELP12,DELP23
      CONTINUE
      DO LOOP ON SECTORS - HEREAFTER REFERRED TO AS
      MAIN SECTOR LOOP
      PROGRAM ENTERS SEC-3 FROM SEC-2 AND ALWAYS EXITS
      TO SEC-4.
      THIS SECTION STARTS THE J LOOP AND ESTABLISHES
      SOME OF THE INITIAL CONDITIONS FOR THE FIRST
      ROW OF THE CURRENT SECTOR CALCULATION.
      SUBSCRIPTED QUANTITIES ARE SET UP AS
      VARIABLE (SUB1,SUB2) WHERE SUB1 IS
      THE ROW NUMBER, AND SUB2 IS THE SECTOR
      NUMBER.
      PMIX = PRESSURE OF STM-N/C MIXTURE ENTERING SECTOR
      PMIX1 = PRESSURE OF STM-N/C MIXTURE ENTERING SECTOR
      J=DUMMY VARIABLE REPRESENTING SECTOR NUMBER
      SECF1G = NO OF SECTORS IN THE CONDENSER
      DELP12 = PRESSURE DROP ACROSS A SECTOR
      DELP23 = ENTRANCE PRESSURE LOSS IN THE CONDENSER
      AMOLSS = PRESSURE LOSS AT BUNDLE DUE TO VELOCITY CHANGE
      AMOLST = MOLES OF STEAM ENTERING THE CONDENSER
      AMOLAC = TOTAL MOLES OF STEAM AND N/C ENTERING CONDENSER
      AMOLAC = MOLES OF N/C GASSES ENTERING THE CONDENSER

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CON15370
CON15380
CON15390
CON15400
CON15410
CON15420
CON15430
CON15440
CON15450
CON15460
CON15470
CON15480
CON15490
CON15500
CON15510
CON15520
CON15530
CON15540
CON15550
CON15560
CON15570
CON15580
CON15590
CON15600
CON15610
CON15620
CON15630
CON15640
CON15650
CON15660
CON15670
CON15680
CON15690
CON15700
CON15710
CON15720
CON15730
CON15740
CON15750
CON15760
CON15770
CON15780
CON15790
CON15800
CON15810
CON15820
CON15830
CON15840

NRWSP3=NOROWS+1
DELPP=PTLIM/(RTG+1.)
CHECK2=-2.
DO 80 M=1,NRWSP3
  PSAT(M,J)=PTLIM-(M-1)*DELPP
CONTINUE
PMIX(1,J)=PSAT(1,J)/(AMOLSS/AMOLST)

PAL=PSAT(1,J)
TAL=TSATFN(PAL)
STSAT(1,J)=TAL-459.69
VG=VGFN(TAL,PMIX(1,J))
VN=(10.729*TAL)/((AMWNC*PMIX(1,J))+((AMOLNC/(VNC*AMOLST))))
VMIX=1.0/((AMOLSS/(VG*AMOLST))+((AMOLNC/(3600.0*AOTFLW(1))))
VEL(1,J)=(WS(1,J)+WGAS(J))*VMIX/(3600.0*AOTFLW(1))
WNC=WGAS(J)
AMOLSC=WNC/AMWNC

C$-----
C SEC A3
C
C TEMP OUTPUT SECTION
C
C ZZZ SEC-A3
C-----
SEC A3=0.
IF (SECA3.NE.1.) GO TO 100
WRITE (6,760) J
PMIX(1,J),PSAT(1,J)
WRITE (6,770) STSAT(1,J),TAL
WRITE (6,780) VG,VNC,VMIX
WRITE (6,790) VEL(1,J)
CONTINUE
100
C$-----
C SEC 4
C
C DO LOOP ON ROWS - HEREFTER REFERRED TO AS
C MAIN ROW LOOP
C
C THIS SECTION IS INSIDE THE MAIN SECTOR LOOP. IT
C INITIALIZES SOME VARIABLES PRIOR TO CALLING HELTRN
C IN SEC-5.
C
C I = ROW NUMBER
C IL = ROW NUMBER
C AXO = AREA OPEN TO FLOW IN A ROW OF TUBES FT**2
C AOTFLW = AREA AS AXO
C L = SECTOR NUMBER
C J = SECTOR NUMBER
C NRQMS = NUMBER OF ROWS OF TUBES IN A SECTOR
C DELODF = CHANGE IN TUBE OD / ROW FT

```


CONI 6330
CONI 6340
CONI 6350
CONI 6360
CONI 6370
CONI 6380
CONI 6390
CONI 6400
CONI 6410
CONI 6420
CONI 6430
CONI 6440
CONI 6450
CONI 6500
CONI 6510
CONI 6520
CONI 6530
CONI 6540
CONI 6550
CONI 6560
CONI 6570
CONI 6580
CONI 6590
CONI 6600
CONI 6610
CONI 6620
CONI 6630
CONI 6640
CONI 6650
CONI 6660
CONI 6670
CONI 6680
CONI 6690
CONI 6700
CONI 6710
CONI 6720
CONI 6730
CONI 6740
CONI 6750
CONI 6760
CONI 6770
CONI 6780
CONI 6790
CONI 6800

CALL TO HETTRN AND PRSDRP

THIS SECTION INSIDE BOTH MAIN ROW AND SECTOR LOUPS

```

ST$AT = STEAM SATURATION TEMP F
TAN = TARGET TUBE LOCATION IN VERTICAL RCW
AWS = STEAM FLOW TO A ROW OF A SECTOR LBM/HR
NWC = N/C FLOW TO A ROW OF A SECTOR LBM/HR
UN = OVERALL HEAT TRANSFER COEFF FOR ONE ROW OF TUBES IN A SECT.
HMTD = LMTD FOR A ROW IN A SECTOR F
HOMCI = ST$AT - COOLANT INLET TEMP
HOMCO = ST$AT - COOLANT OUTLET TEMP
ST$FO = AVE TEMP OF OUTER TUBE FILM
SHI = INTERNAL TUBE FILM HEAT TRANSFER COEFF.
SHN = INTERNAL TUBE FILM HEAT TRANSFER COEFF.
SRC = RATIO OF N/C GAS TO STM AT ONE ROW OF TUBES
AROU = EXTERNAL HEAT TRANSFER COEFF
AXO = AREA OPEN TO FLOW ON VAPOR SIDE AT A ROW IN A SECTOR
VWRE = REYNOLDS NUMBER
DUMNY = NUSSELT NUMBER
VWPSHH = OUTLET COOLANT TEMP F
VWPSHF = N/C GAS FILM HEAT TRANSFER COEFF
L = SECTOR NUMBER
HFG = STEAM LATENT HEAT OF VAPORIZATION BTU/LBM
WNCN = COND ENSATE FROM ONE ROW OF TUBES IN A SECTOR LBM/HR
WACD = OUTER SURFACE AREA OF A TUBE FT**2
LIM = LOWEST SATURATION PRESSURE THE STEAM CAN GO BEFORE THE
CORRESPONDING SATURATION TEMPERATURE IS 0 HEAT TRANSFER
COOLANT TEMPER OF TUBES IN A GIVEN ROW OF A SECTOR
TBNPR = NUMBER OF TUBES IN A GIVEN ROW OF A SECTOR
TAL = SATURATED STEAM TEMP R
VMIX = SPECIFIC VOLUME OF STM-N/C MIXTURE FT**3/LBM
SDO = TUBE OD
FRICTION FACTOR USED IN PRESSURE DROP CALC
VWPSH = FRICTION DROP ACROSS A ROW OF TUBES PSI
DELPTP = PRESSURE DROP ACROSS A ROW OF TUBES PSI
DENHFF = PRESSURE DROP FRICTION FACTOR ENHANCEMENT
ENHFF = PRESSURE DROP FRICTION FACTOR ENHANCEMENT FACTOR, STM SIDE.

```

5-335 777

CHECK TO ENSURE THAT THE SATURATION PRESSURE IN AN EARLIER ROW


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C      CALCULATION HAS NOT DROPPED BELOW THE SATURATION PRESSURE
C      CORRESPONDING TO THAT OF THE INLET COOLANT TEMPERATURE (PTLIM) FOR
C      A GIVEN SECTOR. IF IT HAS, CHECK2<0 AND WE SKIP HETTRN CALCS SINCE
C      DUMMY VARIABLES HAVE BEEN INSERTED FOR PSAT
C      IF (CHECK2.LT.0) GO TO 120
C
C      CALL HETTRN (ALST,AXO,I,L,OD,WB,SHWINV,STSAT(I,L),TID,WNC,WST,ALMT
C      10(I,L),ENHF,HEFF(I,L),HOMCI,HOMCO,RC(I,L),RCUT(I,L),SHI(I,L),SHN(I
C      2,L),STFO,VPSHH(I,L),UN(I,L),VNRE(I,L),ENHI,ENHO,SDDO)
C
C      CHECK TO SEE IF THE FIRST ROW IN THE SECTOR HAS STEAM SATURATION
C      HAS DROPPED BELOW PTLIM. IF IT HAS THEN CHECK2<0 AND I=1.
C      DUMMY VALUES MUST THEN BE PLACED IN THOSE VARIABLES NORMALLY
C      RETURNED BY HETTRN SINCE HETTRN HAS BEEN BYPASSED.
C      IF ((CHECK2.GE.0).OR.(I.NE.1)) GO TO 130
C
C      SINCE THE SATURATION STEAM PRESSURE IS BELOW PTLIM THEN THE STEAM
C      TEMPERATURE IS BELOW COOLANT INLET TEMPERATURE. THIS MEANS NO
C      HEAT IS REMOVED FROM THE STEAM AND THE ALMTD IS 0. THE COOLANT
C      OUTLET TEMP IS THE SAME AS THE COOLANT INLET TEMP AND THE TUBE
C      FILM TEMP IS THE SAME AS COOLANT INLET TEMPS. THE REMAINING
C      VARIABLE VALUES ARE APPROXIMATED.
C      ALMTD(1,J)=0.
C      HOMCI=0.
C      HOMCO=0.
C      VPSHH(1,J)=STB1
C      HEFF(1,J)=1.E+8
C      RC(1,J)=.161E-3
C      VNRE(1,J)=.9E+5
C      SHI(1,J)=.136E+4
C      SHN(1,J)=.136E+5
C      UN(1,J)=655.
C      ROUT(1,J)=.136E+5
C      STFO=STB1
C      GO TO 150
C
C      CHECK TO SEE IF A ROW OTHER THAN THE FIRST ONE IN THE SECTOR HAS
C      HAD STEAM SATURATION DROP BELOW PTLIM. IF IT HAS THEN CHECK2<0.
C      DUMMY VALUES MUST THEN BE PLACED IN THOSE VARIABLES NORMALLY
C      RETURNED BY HETTRN SINCE HETTRN HAS BEEN BYPASSED.
C      IF (CHECK2.LT.0) GO TO 140
C      ENHFSV=ENHF
C      GO TO 150
C
C      120
C      130
C

```

```

C 140
C IF CHECK2 < 0, THAT INDICATES THAT THE SATURATION STEAM PRESSURE
C IS BELOW PTLIM AND THUS THE STEAM TEMPERATURE IS BELOW COOLANT
C INLET TEMPERATURE. THIS MEANS THAT NO HEAT IS REMOVED FROM THE
C STEAM AND THE ALMTD IS 0. THE COOLANT OUTLET TEMP EQUALS THE
C COOLANT INLET TEMP AND THE TUBE FILM TEMP IS THE SAME AS THE
C COOLANT INLET TEMP. THE REMAINING VARIABLES ARE GIVEN THE LAST
C GOOD VALUES RETURNED BY HETTRN.
C
C ALMTD(I,J)=0.
C HOMCI=0.
C HOMCO=0.
C VPSHH(I,J)=STBI
C HEFF(I,J)=HEFF(I-1,J)
C RC(I,J)=RC(I-1,J)
C VNRE(I,J)=VNRE(I-1,J)
C SHN(I,J)=SHN(I-1,J)
C SHN(I,J)=SHN(I-1,J)
C UN(I,J)=UN(I-1,J)
C ROUT(I,J)=ROUT(I-1,J)
C STFO=STBI
C ENHF=ENHFSV
C
C 150
C TB2=VPSHH(I,J)
C HFG=HFGFN(STSAT(I,J))
C
C CHECK TO SEE IF STEAM FLOW IN A SECTOR HAS ALREADY GONE TO 0
C IF IT HAS CHECK1<0 AND DUMMY VALUES HAVE ALREADY BEEN ASSIGNED
C TO WCNC.
C
C IF (CHECK1.LT.0.) GO TO 160
C
C WCND(I,J)=UN(I,J)*AD*ALMTD(I,J)/HFG*TBNPR(I)
C
C CHECK TC SEE IF SATURATION PRESSURE HAS ALREADY GONE BELOW PTLIM
C AND DUMMY VARIABLES HAVE BEEN ASSIGNED TO DELPTP
C
C IF (CHECK2.LT.0) GO TO 170
C
C 160 CALL PRSDRP (IAL,VMIX,WS(I,J),WNC,AXO,OD,VPSH,DELPTP,ENHF)
C 170 CONTINUE
C JX=0
C
C -----
C SEC A5
C
C TEMP OUTPUT SECTION
C
C ZZZSEC=A5
C -----
C SECA5=0.

```

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CON17290
CON17300
CON17310
CON17320
CON17330
CON17340
CON17350
CON17360
CON17370
CON17380
CON17390
CON17400
CON17410
CON17420
CON17430
CON17440
CON17450
CON17460
CON17470
CON17480
CON17490
CON17500
CON17510
CON17520
CON17530
CON17540
CON17550
CON17560
CON17570
CON17580
CON17590
CON17600
CON17610
CON17620
CON17630
CON17640
CON17650
CON17660
CON17670
CON17680
CON17690
CON17700
CON17710
CON17720
CON17730
CON17740
CON17750
CON17760

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CON17770
CON17780
CON17790
CON17800
CON17810
CON17820
CON17830
CON17840
CON17850
CON17860
CON17870
CON17880
CON17890
CON17900
CON17910
CON17920
CON17930
CON17940
CON17950
CON17960
CON17970
CON17980
CON17990
CON18000
CON18010
CON18020
CON18030
CON18040
CON18050
CON18060
CON18070
CON18080
CON18090
CON18100
CON18110
CON18120
CON18130
CON18140
CON18150
CON18160
CON18170
CON18180
CON18190
CON18200
CON18210
CON18220
CON18230
CON18240

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IF (SECA5.NE.1) GO TO 170
WRITE (6.860) I,J
WRITE (6.910) T82, UN(I,L), VNRE(I,L)
WRITE (6.870) ALMTD(I,L), HEFF(I,L)
WRITE (6.880) HOMCI, HOMCO
WRITE (6.890) RC(I,L), ROU(I,L)
WRITE (6.900) SH(I,L), SHN(I,L)
WRITE (6.920) WNC, WS(I,L)
WRITE (6.930) DELPTP, VPSH
WRITE (6.940) WCND(I,J), HFG
WRITE (6.950) AO, TBNPR(I)

```

SEC 6

TEST FOR POSITIVE STM FLOW AND SAT PRESS

```

WS = STM FLOW TO ONE ROW IN A SECTOR LB/HR
WCND = CONDENSATE FROM ONE ROW OF TUBES IN A SECTOR LB/HR
WNC = N/C GAS FLOW TO ONE ROW OF TUBES IN A SECTOR LB/HR
AXU = AREA OPEN TO FLOW IN A ROW OF A SECTOR
GFLW = MASS FLOW RATE OF MIXTURE IN A TUBE BUNDLE LB/(HR-FT**2)
I = ROW NUMBER
AMOLS = MOLES OF STEAM IN A ROW OF A SECTOR
PMIX = PRESS OF STM - N/C MIXTURE
DELPTP = PRESS DROP ACROSS A ROW OF TUBES
AMWNC = MOLECULAR WEIGHT OF N/C
PSAT = SATURATED STEAM PRESS
J = SECTOR NUMBER
TSAT = SATURATED STEAM TEMP - F
TSAT = SATURATED STEAM TEMP - R
PAL = DUMMY FOR PSAT
CHECK1 = INDICATOR THAT NEG. STEAM FLOW HAS BEEN ENCOUNTERED
CHECK2 = INDICATOR ANALYSIS
        IN SECTOR THAT PRESSCP SATFN(STB) HAS BEEN
        ENCOUNTERED IN SECTOR ANALYSIS
PIEST = NEXT ROW PRESSURE VALUE TO CHECK FOR A BAD VALUE
WTST = NEXT ROW STEAM FLOW TO CHECK FOR A NEGATIVE VALUE
WTST = TEST VARIABLE WHICH IS NEGATIVE WHEN NEGATIVE STEAM FLOW
        IS ENCOUNTERED IN A SECTOR
PTST = TEST VARIABLE WHICH IS A NEGATIVE WHEN PSAT DROPS BELOW
        PTLM IN A SECTOR

```

ZZZ SEC-6

CHECK TO SEE IF STEAM FLOW HAS ALREADY GONE TO 0 IN AN EARLIER
ROW CALCULATIO AND FIXUP HAS BEEN MADE TO WS AND WCND

170 IF (CHECK1.LT.0) GO TO 180
WS(I+1,J)=WS(I,J)-WCND(I,J)


```

C      AMOLS = MOLES OF STEAM IN A ROW OF A SECTOR
C      PMIX = PRESSURE OF STEAM - NYC MIXTURE
C      PSAT = SATURATED STEAM PRESS
C      TSAT = SATURATED STEAM TEMP
C      STSAT = SATURATED STEAM TEMP F
C
C      ZZZ SEC-7
C-----
230    TSAT=TSATFN(PAL)
C      SECAT=0.
C      STSAT(I+1,J)=TSAT-459.69
C      IF (STSAT(I+1,J)-STFO) 240,240,250
C      STSAT(I+1,J)=STFO
C      TSAT=STSAT(I+1,J)+459.69
C      CONTINUE
C      WCNDP=FUN(I,J)*AO*ALMIG(I,J)*IBNPR(I)-((WS(I,J)*CPSFN(TSAT))/18.015+
1      MN C*CPAFN(TSAT,JGASI/AMWNC))*((TAL-TSAT))/HFG
C      IF (SECAT.EQ.1) WRITE (6,1070) WCND(I,J),WCNDP
C      IF (SECAT.EQ.1) WRITE (6,1080) TAL,TSAT
C
C      CHECK TO SEE IF WCND IS 0 WHICH CAN OCCUR IF PSAT HAS DRIPPED
C      BELOW PTLIM (CHECK2<0). IF IT HAS THERE IS NO HEAT TRANSFER FROM
C      THE STEAM AND NO NEED TO CORRECT FOR SENSIBLE HEAT
C
C      IF (CHECK2.LT.0) WCNDP=WCND(I,J)
C
C      CHECK TO SEE IF STEAM FLOW HAS ALREADY GONE TO 0 (CHECK<0)
C      AND WCND HAS BEEN FIXED UP WITH DUMMY VALUES
C
C      IF (CHECK1.LT.0) WCNDP=WCND(I,J)
C
C      IF CONDENSATE FLOW HAS GONE TO 0 AVOID ITERATIONS
C
C      IF (WCND(I,J).EQ.0.) GO TO 290
C
C      IF EITHER CHECK IS TRUE THEN AVOID CORRECTIVE ITERATION TO WCND
C
C      IF (ABS(WCNDP/WCND(I,J)-1.0)-.005) 290,260,260
C      JX=JX+1
C      IF (JX-50) 280,280,270
C      IF (SECAT.EQ.1) WRITE (6,1120) IDENT,I,J,I,J
C      GO TO 250
C      WCND(I,J)=WCNDP
C      GO TO 170
C      CONTINUE
C      SECAT=0.

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CON20650
CON20660
CON20670
CON20680
CON20690
CON20700
CON20710
CON20720
CON20730
CON20740
CON20750
CON20760
CON20770
CON20780
CON20790
CON20800
CON20810
CON20820
CON20830
CON20840
CON20850
CON20860
CON20870
CON20880
CON20890
CON20900
CON20910
CON20920
CON20930
CON20940
CON20950
CON20960
CON20970
CON20980
CON20990
CON21000
CON21010
CON21020
CON21030
CON21040
CON21050
CON21060
CON21070
CON21080
CON21090
CON21100
CON21110
CON21120

AMOLS = MOLES OF STM TO A ROW
TSAT = STM SATURATION TEMP
PMIX = ST-N/C MIXTURE PRESSURE
AMWNC = MOLECULAR WEIGHT OF N/C GASSES
VNC = SPECIFIC VOLUME OF N/C GASSES
WNC = N/C FLOW TO A ROW OF A SECTOR
AMOLSC = MOLES OF A N/C TO A SECTOR
VEL = STM-N/C MIXTURE VELOCITY IN A ROW OF TUBES
WS = STM FLOW TO A ROW IN A SECTOR LB/HR
AOTFLW = AREA OPEN TO STM FLOW IN A ROW OF TUBES
SMTB1 = SUM OF (COOLANT INLET TEMP*COOLANT FLOW RATE)
WB = COLLANT FLOW TO ONE TUBE IN THE CONDENSER
STB1 = COOLANT INLET TEMP
TBNPR = NUMBER OF TUBES IN A ROW OF A SECTOR
SMBR = ROW BY ROW SUM OF COOLANT FLOW
SMTB2 = ROW SUM OF (COOLANT OUTLET TEMP*FLOW RATE)
T82 = COOLANT OUTLET TEMP FOR A TUBE
SUMQ = SUM OF HEAT DUTY ON ROWS OF TUBES
UN = OVERALL HEAT X-FER COEF FOR A ROW
AO = TUBE OUTER SURFACE AREA
ALMTC = LMTD
QOA = HEAT FLUX ACROSS TUBE WALL
CUMCP = ACCUMULATED PRESS DROP FROM INLET TO CURRENT ROW
PMIX = PRESS OF STM-N/C MIXTURE
PHP = OVERALL POWER TO DRIVE THE COOLANT THROUGH THE CONDENSER
AND THE COOLER TUBES IN HP.
DELP = PRESSURE DROP ACROSS A SECTOR
DELPTP = PRESSURE DROP ACROSS A ROW
TAL = SAT STEAM TEMP
I = ROW NUMBER
IT = DUMMY LOOP VARIABLE (IT = 1)
SVMIX1 = SPECIFIC VOLUME OF STM-N/C MIXTURE ENTERING CONDENSER
WGAS = FLOW OF N/C GAS TO A SECTOR
AOTFLW = AREA OPEN TO STEAM FLOW IN A ROW OF TUBES
C = USED TO ADJUST STEAM FLOW TO MATCH PRESS DROPS IN SEC-10

370

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370

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380      QQA(I,J)=UN(I,J)*ALMTD(I,J)
      CUMDP(I,J)=(PMIX(I)-PMIX(I+1,J)
      DELP(J)=DELP(J)+DELP(T)
      TAL=TSAT
      CONTINUE
      C(I,J)=(WS(1,J)+WGAS(J))/SQRT(DELP(J))
      C
      C INCLUDE ONLY THOSE SECTORS WHERE STEAM FLOW HAS NOT GONE TO 0
      C IN STMSUM SO AS NOT TO INCLUDE DUMMY VALUES IN THE CALCULATION
      C OF EXIT STEAM FRACTION
      C
      IF (ICHECK1.GE.0) STMSUM=STMSUM+WS(NOROWS+1,J)
      CONTINUE
390      C$-----
      C SEC A8
      C ZZZ SEC-A8
      C-----
      SEC A8=0
      IF (SEC A8.NE.1.) GO TO 410
      WRITE (6,1050)
      DO 400 I=1,ISEC
      WRITE (6,1100) WTST(I),PTST(I)
400      CONTINUE
410      C$-----
      C SEC 9
      C ZZZ SEC-9
      C-----
      PMXEXT=0.
      DELPVE=0.
      PSUM=0.
      VELEXI=0.
      DO 420 I=1,ISEC
      PAL=PSAT(KSTOP,I)
      PSUM=PSUM+PAL/SECF LG
      VELEXI=VELEXI+VEL(NOROWS+1,I)
      DELPVE=DELPVE+DELP(I)
      PMXEXT=PMXEXT+PMIX(NOROWS+1,I)
420      C
      C MAKE PTST AND EXIT STEAM FRACTION VARIABLES CONTINUOUS
      C THIS IS DONE TO SATISFY AND ENHANCE OPTIMIZER CALCULATIONS. IF
      C THE VARIABLE PTST IS GIVEN THE LAST ROW+1 PRESSURE VALUES. IF
      C IT IS NON-NEGATIVE. IN ORDER TO MAKE EXIT STEAM FRACTION
      C (EXIT FR) CONTINUOUS. THE VARIABLE FR IS CREATED WHICH INCORPORATES
      C WTST OF ALL THE SECTORS. IF THE WTST VALUES ARE LARGE NEGATIVE
      C NUMBERS THEN FR-->-1. AS WTST VALUES APPROACH 0 INDICATING STEAM
      C THROUGHOUT THE CONDENSOR THEN FR-->0. FR IS THEN ADDED TO EXITFR

```

CON21130
 CON21140
 CON21150
 CON21160
 CON21170
 CON21180
 CON21190
 CON21200
 CON21210
 CON21220
 CON21230
 CON21240
 CON21250
 CON21260
 CON21270
 CON21280
 CON21290
 CON21300
 CON21310
 CON21320
 CON21330
 CON21340
 CON21350
 CON21360
 CON21370
 CON21380
 CON21390
 CON21400
 CON21410
 CON21420
 CON21430
 CON21440
 CON21450
 CON21460
 CON21470
 CON21480
 CON21490
 CON21500
 CON21510
 CON21520
 CON21530
 CON21540
 CON21550
 CON21560
 CON21570
 CON21580
 CON21590
 CON21600

CON22090
CON22100
CON22110
CON22120
CON22130
CON22140
CON22150
CON22160
CON22170
CON22180
CON22190
CON22200
CON22210
CON22220
CON22230
CON22240
CON22250
CON22260
CON22270
CON22280
CON22290
CON22300
CON22310
CON22320
CON22330
CON22340
CON22350
CON22360
CON22370
CON22380
CON22390
CON22400
CON22410
CON22420
CON22430
CON22440
CON22450
CON22460
CON22470
CON22480
CON22490
CON22500
CON22510
CON22520
CON22530
CON22540
CON22550
CON22560

```

500      WPT=WPT+WP(J)
        CONTINUE
        WSP(JMAX)=WSI-WSPT
        WSPT=WSPT+WSP(JMAX)
        WGAS(JMAX)=WSP(JMAX)*WNCFR
        WP(JMAX)=WSP(JMAX)+WGAS(JMAX)
        WPT=WPT+WP(JMAX)
        ILOOP=ILOOP+1

        CHECK FOR STEAM ADJUSTMENTS WHICH TRY TO PUT TO LOW A STEAM
        VALUE INTO A SECTOR

510      IFAIL=0
        DO 520 K=1,ISEC
          COMP=WSI/200.
          IF (WSP(K).LT.COMP) IFAIL=K
          IF (WSP(K).LT.COMP) WRITE (6,999)
          FORMAT (1X,'STEAM FLOW ADJUSTMENT WAS REQUIRED')
          IF (WSP(K).LT.COMP) GO TO 530
        CONTINUE
        GO TO 550
530      DIFF=2.*COMP-WSP(IFAIL)
        WSP(IFAIL)=2.*COMP
        ADJ=DIFF/FLOAT(ISEC-1)
        DO 540 J=1,ISEC
          IF (J.EQ.IFAIL) GO TO 540
          WSP(J)=WSP(J)-ADJ
        CONTINUE
        GO TO 510
540      DO 560 J=1,ISEC
          WS(1,J)=WSP(J)
          IF (ILOOP-50) 20,20,570
          WRITE (6,1110) IDENT
550      INCORPORATE FR INTO EXITFR TO MAKE IT CONTINUOUS FROM 1-->-1
        EXITFR=STMSUM/WSI+FR
        WSEXIT=STMSUM
        VELEXIT=VELEXIT/SECFLG
        DELPVE=DELPVE/SECFLG
        PMXEXT=PMXEXT/SECFLG
        TSATEX=TSATFN(PSUM)
        AMLSEX=STMSUM/18.015
        IF ((STMSUM.LE.0.).AND.(PRCCLR.GT.0.)) AMLSEX=1.0/18.015
        EXITFC=1.
        IF (PRCCLR.EQ.0.0) EXITOA=EXITFR

```

```

C          IF (PRCCLR.EQ.0.0) GO TO 590
C          CALL TO COOLER, IF THERE IS ONE
C          ENHIC=ENHI
C          ENHOC=ENHO
C          ENHFC=ENHF
C          SHWINC=SHWINV
C          TB2C=TB2
C          WBC=WB
C          IF (NBAD.GT.0) WCNDAV=SUBAVE/FLOAT(NBAD)
C          CALL COCLEX (TBDRYC,WCNDAY,SBFLOC,WSOUT)
C          CALCULATE OVERALL POWER REQUIRE TO DRIVE THE COOLANT
C          PHP=PHP*(SMWBC/(SMWBC+SMWB)+1.)
C          CALCULATE THE OVERALL COOLER/CONDENSER VOLUME
C          VOL1=(VOL1+VOLC)
C          CALCULATE OVERALL EXIT FRACTION
C          IF ((EXITFR.GT.0.) .AND. (EXITFC.GT.0.)) EXITQA=EXITFK*EXITFC
C          IF ((EXITFR.GT.0.) .AND. (EXITFC.GT.0.)) RETURN
C          EXITQA=WSOUT/WSI+(-(SUBFLO+SBFLOC)/WSI)
C          RETURN
C          (1X,7HSECTOR ,13,2X,5HROW ,14)
C          (1H,37H ***** OUTPUT FOR SEC-2 ***** )
C          (1H,10HWSI ,10HNGC ,10HWGAS(1) ,10HAGOTFLW(1) ,10HSTSAT1 ,10HPMIX1 ,10HAMULST ,10HVMIX1 ,10HG2 ,10HARAT ,5HVEL2 ,5HDELTP2 )
C          (1H,10HWS(1,1) ,10HHTSAT1 ,10HPSAT1 ,10HAMOLNC ,10HHSVNC1 ,1H ,2F10.3)
C          (1H,37H ***** )
C          (1H,10HSEC FAR ,10HSECFAR ,10HVEL1 ,10HDELTP1 ,1H ,2F10.4)
C          (1H,29HPUT FOR SEC-3 -SECTOR NO. ,12)
C          (1H,36HENTERING PRESSURES IN PSI - MIXTURE=,E10.3,13H SATU
C          RATION= ,E10.3)
C          (1H ,21HENTERING STM TEMPS - ,F6.2,4F ,F6.2,2H R)

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CON22570
CON22580
CON22590
CON22600
CON22610
CON22620
CON22630
CON22640
CON22650
CON22660
CON22670
CON22680
CON22690
CON22700
CON22710
CON22720
CON22730
CON22740
CON22750
CON22760
CON22770
CON22780
CON22790
CON22800
CON22810
CON22820
CON22830
CON22840
CON22850
CON22860
CON22870
CON22880
CON22890
CON22900
CON22910
CON22920
CON22930
CON22940
CON22950
CON22960
CON22970
CON22980
CON22990
CON23000
CON23010
CON23020
CON23030
CON23040

```

```

790 FORMAT (1H,32HENT SP. VOL. IN FT**3/LBM - STM=,E10.3,9H N/C GAS=,
1E10.3,1H Mixture=,E10.3) CON23050
800 FORMAT (1H,23HENTERING STM VELOCITY =,E10.3,8H FT/SEC) CON23060
810 FORMAT (1H,33H** OUTPUT FOR SEC-4 - ROW NUMBER,14) CON23070
820 FORMAT (1H,33HTUBE WALL AREA - SQ.FT. - INSIDE=,E10.3,10H OUTSIDE CON23080
1E=,E10.3) CON23090
830 FORMAT (1H,9HTUBE ID=,F6.3,30H' FT - TUBE X-SECTIONAL AREA =,E10 CON23100
1.3,6H FT**2) CON23110
840 FORMAT (1H,24HLOG MEAN TUBE THICKNESS=,E10.3,25H FT - LOG MEAN TUC CON23120
1BE AREA=,E10.3,6H FT**2) CON23130
850 FORMAT (1H,30HINVERSE WALL HEAT X-FER COEF =,E10.3,17H HR-FT**2-F CON23140
1/8 TU) CON23150
860 FORMAT (1H,22HIN SECALC, SEC-5, ROW,,14,9H, SECTOR,,13) CON23160
870 FORMAT (1H,7HALMTD =,E10.3,8H HEFF =,E10.3) CON23170
880 FORMAT (1H,7HOMCI =,E10.3,8H HOMCC =,E10.3) CON23180
890 FORMAT (1H,7HRC =,E10.3,8H ROUT =,E10.3) CON23190
900 FORMAT (1H,7HSH1 =,E10.3,8H SHN =,E10.3,8H VNRE =,E10.3) CON23200
910 FORMAT (1H,7HTB2 =,E10.3,8H UN =,E10.3,8H VNRE =,E10.3) CON23210
920 FORMAT (1H,7HWNC =,E10.3,8H WS =,E10.3,8H VNRE =,E10.3) CON23220
930 FORMAT (1H,7HDELP TP=,E10.3,8H VPSH =,E10.3) CON23230
940 FORMAT (1H,7HWCND =,E10.3,8H HFG =,E10.3) CON23240
950 FORMAT (1H,7HAO =,E10.3,8H TBNPR =,E10.3) CON23250
960 FORMAT (1H,32HNEG STEAM MASS FLOW IN SEC-6 ROW,14,10H UF SECTOR,1 CON23260
14) CON23270
970 FORMAT (1H,18HCURRENT FLOW RATE=,F12.6,17H NEXT FLOW RATE=,F12.6 CON23280
1) CON23290
980 FORMAT (1H,8HWTST(1)=,F12.6) CON23300
990 FORMAT (1H,30HNEGATIVE SAT PRSS IN SEC-6 ROW,14,9H SECTOR,14) CON23310
1000 FORMAT (1H,18HCURRENT SAT PRESS=,E10.3,11H NEXT ROW=,E10.3) CON23320
1010 FORMAT (1H,8HPTST(1)=,E10.3) CON23330
1020 FORMAT (1H,25HNO PROBLEMS IN SE-6, ROW=,14,8H SECTOR=,14) CON23340
1030 FORMAT (1H,23HOUTPUT FROM SEC-7, ROW 14,11H OF SECTOR,14) CON23350
1040 FORMAT (1H,9HWS(1,J) =,E10.3,13H WCNDD(1,J) =,E10.3) CON23360
1050 FORMAT (1H,6HTSAT =,E10.3,14H STSAT(1,J) =,E10.3) CON23370
1060 FORMAT (1H,11HGFLOW(1,J) =,E10.3,13H PSAT(1,J) =,E10.3) CON23380
1070 FORMAT (1H,28HSEC-7, BELOW 130, WCNDD(1,J) =,E10.3,8H WCNUP=,E10.3 CON23390
1) CON23400
1080 FORMAT (1H,22HSEC-7, BELOW 130, TAL=,E10.3,6H TSAT=,E10.3) CON23410
1090 FORMAT (1H,3X,4HWTST,8X,4HPTST/1) CON23420
1100 FORMAT (1H,E10.3,2X,E10.3,2X,E10.3) CON23430
1110 - FORMAT (1H,19A4,A3,40HNO CONVERGENCE IN COND. DELTA P (1PLOOPI) CON23440
1120 FORMAT (1H,19A4,A3,40HNO CONVERGENCE IN COND. DELTA P (1PLOOPI) CON23450
1E FOR WCNDD(12,1H,11,1H) CON23460
END CON23470
C ***** CON23480
C ***** CON23490
C ***** CON23500
C ***** CON23510
C ***** CON23520

```

```

SUBROUTINE HETTRN (ALST,AXO,IR,LJ,CD,MB,SHWINV,STSAT,TID,WNC,WST,A
1LMTD,ENHF,HEFF,HOMCI,HOMCO,RC,ROUF,SHI,SHNF,STFO,TB2,VNF,XNRE,ENH
2,ENHO,SDD)
C-----
HET 1
C-----
SUBROUTINE HETTRN
HETTRN CALLED BY: SECALC
SUBROUTINES CALLED BY HETTRN:
DSFVTV,
FUNCTION ROUTINES CALLED BY HETTRN:
, PSATFN, SMUFN, AMUFN, HFCFN, SKBFN,
, BMUFN, CPFN, ROEFN,
C-----
DEC 69 REV. COLBJ,FDAVE
COMMON /INPT/ BC(6),BE(6),ENH(6),ENI(6),END(6),FOUL,PHI,SKW,STBI,S
1TSAT1,TUBESW,INCIR,IOP1,PIST(15),SECHID,IBAF,ISEC,JBAF(16),JGAS,MD
2IAM,MPITCH,NEE,NEI,NETE(6),NETI(6),NRNE(6),NRNI(6),NORONS,WTST(15)
3,WST,PFILL
COMMON /QRC2/ ANT(100,15),STB2ES,VW(100)
COMMON /CONST/ AMWNC,CBI,CPB,PI,SG,IFIRST
DIMENSION R2(3),E2OK(3)
HE TON=0.
IF (HETCN.NE.1.) GO TO 10
M5=1
WRITE (6,310) M5
WRITE (6,320) IR,LJ
WRITE (6,330) OD,TID
WRITE (6,340) SHWINV,STSAT
WRITE (6,350) WST,WNC
C-----
HET 2
C-----
DATA INITIALIZATION:
BB = COOLANT FLOW IN TUBE LBM/HR-FT**2
DGFLM = CALCULATED TEMP DROP ACROSS FILM??
DLFLM = CALCULATED TEMP DROP ACROSS LIQUID FILM??
HEFF = NONCONDENSIBLE FILM HEAT TRANSFER COEF, BTU/HR-FT**2-F
UEST = ESTIMATED OVERALL HEAT TRANSFER COEF
VALUES FOR USE IN SUBROUTINE DSFVTV
E2OK = FORCE CONSTANT FOR NONCOND GAS
R2 = GAS COLLISION DIAMETER IN ANGSTROMS
ZZZ HET-2
C-----
10 IF (WNC.EQ.0.) DGFLM=0.
IF ((LJ.EQ.1).AND.(IR.EQ.1)) GO TO 20

```

CON24010
CON24020
CON24030
CON24040
CON24050
CON24060
CON24070
CON24080
CON24090
CON24100
CON24110
CON24120
CON24130
CON24140
CON24150
CON24160
CON24170
CON24180
CON24190
CON24200
CON24210
CON24220
CON24230
CON24240
CON24250
CON24260
CON24270
CON24280
CON24290
CON24300
CON24310
CON24320
CON24330
CON24340
CON24350
CON24360
CON24370
CON24380
CON24390
CON24400
CON24410
CON24420
CON24430
CON24440
CON24450
CON24460
CON24470
CON24480

```

IF (IR.EQ.1) GO TO 30
UE ST=UESTSV
HEFF=HEFFSV
DGFLM=DGFLMS
DLFLM=DLFLMS
TB2=TB2SV
XNRET=XNRES
GO TO 40
IF (IFIRST.EQ.0) GO TO 30
HEFF=2100.
DATA UE ST,DGFLM,DLFLM,XNRET/700.,0.05,2.0,100000./
DATA RZ1,E2OK/3.617,3.996,3.838,97.0,190.0,140.75/
TB2=STB2ES
IFIRST=0
GO TO 40
UE ST=UEST1
HEFF=HEFF1
DGFLM=DGFLM1
DLFLM=DLFLM1
TB2=TB21
XNRET=XNRE1
CONTINUE

FSAVE IS AN IMPUT ITEM WITH A VALUE BETWEEN 0 AND 1 RELATED TO TUBE
SPACING AND ORIENTATION.
FSAVE=C.5

BNF=ANTI(IR.LJ)
IF (BNF.LT.1.) BNF=1.
BB=WB/(PI*FID*TID/4.)
AI=PI*FID*ALST
AO=PI*GC*ALST
ENHI=1.
ENHF=1.
ENHO=1.
IF (NEI.EQ.0) GO TO 60
DO 50 I=1,NEI
ITEM1=NRN1(1)+NEI(1)-1
ITEM2=ITEM1+NEI(1).AND.(1.LE.ITEM2)) ENHI=ENI(1)
IF ((1.GE.ITEM1).AND.(1.LE.ITEM2)) GO TO 80
DO 70 I=1,NEE
ITEM1=NRNE(1)
ITEM2=ITEM1+NEI(1)-1
IF (1.LT.ITEM.OR.1.GT.ITEM2) GO TO 70
EHND=END(1)

```

20

30

40

CC

CC

CC

CC

CC

50

60

PSATFN ; SMUFN ; AMUFN ; HFGFN ;

```

C ZZZ HET-3
C-----
90 K=0
  WBO TH=HST+WNC
  RC=WNC/(WBO TH)
  TSAT=STSAT+459.69
  GMAX=(WBO TH)/AXO
  PSAT=PSATFN(TSAT)
  AMOLSS=WST/18.015
  AMOLSC=WNC/AMWNC
  AMOLT=AMOLSS+AMOLSC
  AMWAV=(WBO TH)/AMOLT
  RMWNC=SQRT(AMWNC)*AMOLSC/AMOLT
  RMWSC=4.24444*AMOLSS/AMOLT
  AVIS=(SMJFN(TSAT)*RMWSC+AMUFN(TSAT,JGAS)*RMWNC)/(RMWSC+RMWNC)
  HSTO=HFGFN(STSAT)
  STBAVE=(STBI+TB2)/2.0
  DLFLM=DLFLM
  DLGFLM=DGFLM
  STWO=STSAT-DELFLM-DLGFLM
  STFO=(STSAT+STWO)/2.0
  XNRE=OD*(WBO TH)/(AXO*3600.*AVIS)
  IF (HETCN.NE.1.) GO TO 100
  M5=3
  WRITE (6,310) M5
  WRITE (6,410) GMAX,PSAT
  WRITE (6,420) AMOLSS,AMOLSC,AMOLT
  WRITE (6,430) RMWNC,RMWSC
  WRITE (6,440) AVIS,HSTO,XNRE
  WRITE (6,450) STBAVE,STFO,STWO
  WRITE (6,460) DELFLM,DLGFLM
C-----
C$ HET 5
C COLBY J FACTOR CALCULATION AND BRANCH
C WNC1 = TOTAL WEIGHT OF NONCOND ENTERING CONDENSER
C IF NO NONCOND, THEN SKIP DIFFUSIVITY CALCULATION.
C ZZZ HET-5
C-----
100 CONTINUE
  COLBJ=EXP(0.53883-0.544*ALOG(XNRE))
  IF (HETCN.NE.1.) GO TO 110
  M5=5
  WRITE (6,310) M5
  WRITE (6,470) COLBY,WNC
  IF (WNC.EQ.0.) GO TO 120
110

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CON24570
CON24580
CON24590
CON25000
CON25010
CON25020
CON25030
CON25040
CON25050
CON25060
CON25070
CON25080
CON25090
CON25100
CON25110
CON25120
CON25130
CON25140
CON25150
CON25160
CON25170
CON25180
CON25190
CON25200
CON25210
CON25220
CON25230
CON25240
CON25250
CON25260
CON25270
CON25280
CON25290
CON25300
CON25310
CON25320
CON25330
CON25340
CON25350
CON25360
CON25370
CON25380
CON25390
CON25400
CON25410
CON25420
CON25430
CON25440

```



```

CJ=COLBJ*GMAX/(XNSCH**0.066667)
IF (HETCN.NE.1.) GO TO 120
M5=6
WRITE (6,310) M5
-----
C$ HET 7
CCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCCC
      BEGIN ITERATIVE CALCULATIONS FOR:
      HEAT TRANSFER COEF
      TEMP DROP ACROSS LIQUID FILM
      TEMP DROP ACROSS N/C FILM (IF ANY)

      THE PROGRAM CONTINUES TO RETURN HERE UNTIL ONE
      OR MORE OF THE FOLLOWING CONDITIONS ARE MET:
      1) CHANGE IN THE CALCULATED HEAT TRANSFER COEF IS
        LESS THAN OF THE PREVIOUS VALUE AND AT LEAST
        FOUR ITERATIONS HAVE BEEN MADE.
      2) CHANGE IN THE CALCULATED TEMP ACROSS THE LIQUID
        FILM IS LESS THAN .01 DEGREES AND THE CHANGE
        IN CALCULATED TEMP DIFF ACROSS THE GAS FILM
        IS LESS THEN .001 DEGREES.
      3) TEN ITERATIONS HAVE BEEN COMPLETED.

      AI = INTERNAL SURFACE AREA OF ONE TUBE FT**2
      AO = EXTERNAL SURFACE AREA OF ONE TUBE FT**2
      BB = COOLANT FLOW IN TUBE LBM/HR-FT**2
      BNUF = COOLANT VISCOSITY LBM/HR-FT
      CBI = TUBE FLOODING FACTOR
      ENHI = COOLANT CONCENTRATION ENHANCEMENT FACTOR
      ENHO = INTERNAL FILM COEF ENHANCEMENT FACTOR
      RIN = EXTERNAL FILM COEF ENHANCEMENT FACTOR
      TID = RESISTANCE TO HEAT TRANSFER DUE INNER FILM
      OD = TUBE ID FT
      SHBI = TUBE OD FT
      SHBI = SPECIFIC HEAT OF COOLANT BTU/LBM-F
      SHI = INTERNAL FILM HEAT TRANSFER COEF BTU/HR-FT**2-F
      SHMK = EXTERNAL FILM HEAT TRANSFER COEF BTU/HR-FT**2-F
      SKBQ = THERMAL CONDUCTIVITY OF THE COOLANT BTU-FT/HR-FT**2-F
      SKBQ = THERMAL CONDUCTIVITY OF OUTER LIQUID FILM
      STBAVE = AVE COOLANT TEMP. LIQUID FILM (SEE NOTE)
      STFQ = AVE TEMP OF OUTER LIQUID FILM (SEE NOTE)
      STSAT = AVE LOCAL SAT TEM
      TB2 = OUTLET COOLANT TEM (SEE NOTE ON TB2 IN HET-3)
      WB = COOLANT FLOW RATE PER TUBE LBM/HR
      XNREB = REYNOLDS NUMBER OF COOLANT
      XNPRB = PRANDTL NUMBER OF COOLANT

      NOTE: SHMK IS CALCULATED FIRST WITHOUT TAKING FLOODING
      INTO ACCOUNT. SEE NUSSELT EQU PG. 16.

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CON26410
CON26420
CON26430
CON26440
CON26450
CON26460
CON26470
CON26480
CON26490
CON26500
CON26510
CON26520
CON26530
CON26540
CON26550
CON26560
CON26570
CON26580
CON26590
CON26600
CON26610
CON26620
CON26630
CON26640
CON26650
CON26660
CON26670
CON26680
CON26690
CON26700
CON26710
CON26720
CON26730
CON26740
CON26750
CON26760
CON26770
CON26780
CON26790
CON26800
CON26810
CON26820
CON26830
CON26840
CON26850
CON26860
CON26870
CON26880

NOTE: STFO IS INITIALLY GUESSED BASED ON STWO WHICH
IS IN TURN BASED ON DLFLM AND DGFLM. DGFLM AND
DLFLM ARE INITIALIZED BY CATA STATEMENT UPON
ENTERING THIS SUBROUTINE. ALL FOUR OF
THESE VARIABLES ARE UPDATED BELOW.

ZZZ MET-7

120 TB2=STSAT-(STSAT-STBI)/EXP(UEST*AO/(WB*CPFN(CBI,STBAVE)))

STBAVE=(STBI+TB2)/2.
SKBO=SKBFN(O.,STFO)
SKB=SKBFN(CBI,STBAVE)
BMU=BMUFN(CBI,STBAVE)
SHBI=CPFN(CBI,STBAVE)
XNREB=TID*BB/BMU
XNPRB=SHBI*BMU/SKB

SHI=0.023*(XNREB)**0.8*XNPRB**0.33333*(SKB/TID)*ENHI
RIN=AO/(SHI*AI)
SHMK=0.725*(SKBO**3*ROEFN(O.O,STFO)**2*HFGFN(STFO)*416975040.0/(BM
UFN(O,STFO)*OD*DELFLM))**.25*ENHO

THIS IS THE PLACE TO ENTER CORRECTIONS TO THE EXTERNAL FILM COEFF. THE
FOLLOWING IS A CORRECTION ACCORDING TO FUJII, ET AL, TO ACCOUNT FOR
THE EFFECTS OF VAPOR SHEAR AT HIGH VAPOR REYNOLDS NUMBERS.

SHMK1=SHMK
ANUS=SHMK*OD/SKBQ
EMUL=BMUFN(O.,STSAT)
EMUS=SMUFN(TSA,T)*3600.
RHOL=ROEFN(O.,STSAT)
RHOS=1./VGFN(STSAT,PSAT)
VISRA=(EMUS/RHOS)/(EMUL/RHOL)
RETP=XNRE*VISRA
TERM=SGRT(RETP)/ANUS
IF (TERM.LT..278) GO TO 130
ANUSP=1.24*(ANUS**0.8)*(RETP**0.1)
GO TO 140
ANUSP=ANUS*0.70/0.725
SHMKP=ANUSP*SKBQ/OD
SHMK=SHMKP

IF (HETGN.NE.1.) GO TO 150
M5=7
WRITE (6,310) M5
WRITE (6,480) TB2,STBAVE

CON26890
CON26900
CON26910
CON26920
CON26930
CON26940
CON26950
CON26960
CON26970
CON26980
CON26990
CON27000
CON27010
CON27020
CON27030
CON27040
CON27050
CON27060
CON27070
CON27080
CON27090
CON27100
CON27110
CON27120
CON27130
CON27140
CON27150
CON27160
CON27170
CON27180
CON27190
CON27200
CON27210
CON27220
CON27230
CON27240
CON27250
CON27260
CON27270
CON27280
CON27290
CON27300
CON27310
CON27320
CON27330
CON27340
CON27350
CON27360

WRITE (6.490) SK80,SKB
WRITE (6.500) BMJ,SHBI
WRITE (6.510) XNREB,XNPRB
WRITE (6.520) SHI,RIN,SHMK

CC HET 9

TEST FOR TUBE FLOODING, MODIFY
SHMK AS NEEDED

THIS SECTION MODIFIES THE EXTERNAL HEAT TRANSFER
COEF GIVEN BY NUSSELT EQN. FOR TUBE FLOODING.

BNF = CALCULATED TUBE FLOODING FACTOR (SEE NOTE BELOW)
FDAVE = INPUT VALUE OF TUBE FLOODING FACTOR (SEE NOTE BELOW)
FDAVN & FDAVM ARE INTERMEDIATE VALUES USED LATER.
FDOUL = TUBE FOULING FACTOR INPUT BY USER
RFACF = SUM OF THERMAL RESISTANCES NEGLECTING GAS FILM
RIN = RESISTANCE TO HEAT X-FER DUE TO INTERNAL FILM
SHNF = EXTERIOR HEAT X-FER COEFF SHMK MODIFIED FOR RAIN
SHWINV = INVERSE OF WALL HEAT TRANSFER CCOEF

NOTE: ADD CALC FOR FDAVE CURRENTLY UNDEF

NOTE: CALC FOR FDAVM AND FDAVN SHOULD BE MOVED
ABOVE LINE 40.

ZZZ HET-9

150 CONTINUE

INUNDATION EFFECT MAY BE BYPASSED BY SETTING BNF = 1.

BNF = 1.
IF (FDAVE.LT.0. OR BNF.LT.2.) GO TO 160
FDAVN=0.6*FDAVE+(1.-0.5647*FDAVE)/BNF**20
FDAVM=0.6*FDAVE+(1.-0.5647*FDAVE)/(BNF-1.)**20
SHNF=SHMK*(BNF*FDAVN-(BNF-1.)*FDAVM)
GO TO 170
SHNF=0.95*(BNF**0.9-(BNF-1.1**0.9)*SHMK
RFACF=RIN+SHWINV+FOUL+1./SHNF
IF (HETCN.NE.1.) GO TO 180
M5=9

160
170

WRITE (6.310) M5
WRITE (6.330) FDAVN,FDAVM
WRITE (6.340) SHNF,RFACF

CC HET 10

CON27850
CON27860
CON27870
CON27880
CON27890
CON27900
CON27910
CON27920
CON27930
CON27940
CON27950
CON27960
CON27970
CON27980
CON27990
CON28000
CON28010
CON28020
CON28030
CON28040
CON28050
CON28060
CON28070
CON28080
CON28090
CON28100
CON28110
CON28120
CON28130
CON28140
CON28150
CON28160
CON28170
CON28180
CON28190
CON28200
CON28210
CON28220
CON28230
CON28240
CON28250
CON28260
CON28270
CON28280
CON28290
CON28300
CON28310
CON28320

CONTROL PASSES FROM THIS ROUTINE TO ONE OF TWO PLACES,
LINE 40 (HET-7) TO START A NEW ITERATION, OR TO
LINE 170 (HET-13) TO TERMINATE THIS HETTRN CALL
WHEN ONE OF THE FOLLOWING CRITERIA ARE MET:
1) 10 ITERATIONS COMPLETED WITHOUT CONDITION 2 BEING
MET.
2) CHANGE IN HEAT TRANSFER COEF. LT. 1 PERCENT
BETWEEN SUCCESSIVE ITERATIONS.

DELFM = SAVED VALUE OF DLFLM, USED ONLY FOR PRINT
DGFLM = TEMP DROP ACROSS GAS FILM, SET TO 0 HERE
DLFLM = TEMP DROP ACROSS LIQUID CONDENSATE FILM
K = COUNTER FOR NUMBER OF ITERATIONS
RFACT = SUM OF THERMAL RESISTANCES
ROUT = EXTERNAL FILM RESISTANCE. (SEE NOTE)
OD = TUBE OD
SHNF = EXTERNAL FILM HEAT X-FER COEF
SKBO = THERMAL CONDUCTIVITY OF EXTERNAL LIQUID FILM
STCO = TEMP AT SURFACE OF OUTER LIQUID FILM
STFO = AVE TEMP OF OUTER LIQUID FILM
STBAVE = AVE COOLANT TEMP
STSAT = STEAM SATURATION TEMP
STWD = TUBE OUTER WALL TEMP
UEST = VALUE OF UEST FROM LAST ITERATION
UESTS = SAVED VALUE OF UEST, USED ONLY FOR PRINT
UTEST = TUBE HEAT X-FER COEF.
XNU = NUSSELT NUMBER

NOTE: CONSIDER REQUIREMENT FOR MINIMUM OF
FOUR ITERATIONS PRIOR TO UPDATING UEST. COULD
BE AN ALLOWANCE FOR DELFLM TO CATCH UP IN
CONVERGENCE. IF SO, TEST DELFLM FOR ITS
OWN CONVERGENCE, ELIMINATE MIN OF 4 ITERATIONS.

NOTE: ROUT WILL BE REDEFINED AS 1/ROUT
IN HET-13 PRIOR TO EXIT FROM HETTRN

ZZZ HET-11

ROUT=1./SHNF
UTEST=1./RFACT
XNU=SHNF*OD/SKBO
IF (ABS(UEST-UTEST)/UTEST.LT..01) GO TO 290
DE STSV=UEST
UEST=UTEST
IF (K.GT.4) UEST=0.5*(UTEST+UESTSV)
STWD=STSAT-(STSAT-STBAVE)*UTEST/SHNF

AD-A138 568

MARINE STEAM CONDENSER DESIGN OPTIMIZATION(U) NAVAL
POSTGRADUATE SCHOOL MONTEREY CA T M BUCKINGHAM DEC 83

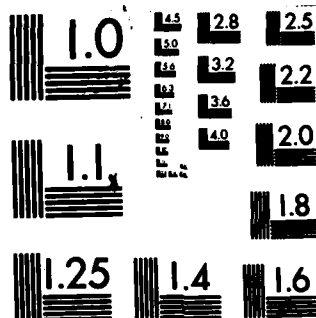
3/3

UNCLASSIFIED

F/G 13/1

NL

END
DATE
FILMED
5-8-84
DTIC




```

CON2 8810
CON2 8820
CON2 8830
CON2 8840
CON2 8850
CON2 8860
CON2 8880
CON2 8890
CON2 8900
CON2 8910
CON2 8920
CON2 8930
CON2 8940
CON2 8950
CON2 8960
CON2 8970
CON2 8980
CON2 8990
CON2 9000
CON2 9010
CON2 9020
CON2 9030
CON2 9040
CON2 9050
CON2 9060
CON2 9070
CON2 9080
CON2 9090
CON2 9100
CON2 9110
CON2 9120
CON2 9130
CON2 9140
CON2 9150
CON2 9160
CON2 9170
CON2 9180
CON2 9190
CON2 9200
CON2 9210
CON2 9220
CON2 9230
CON2 9240
CON2 9250
CON2 9260
CON2 9270
CON2 9280

RFACT = SUM CF THERMAL RESISTANCES NEGLECTING N/C GASSES
ROUT = EXTERNAL HEAT X-FER COEF
SHNF = THERMAL LIQUID FILM HEAT X-FER COEF
STBAVE = THERMAL CONDUCTIVITY OF OUTER LIQUID
STCO = THERMAL COOLANT TEMP
STFC = TEMP AT SURFACE OF OUTER LIQUID FILM
STSAT = TUBE SATURATION TEMP
STWO = TUBE OUTER WALL TEMP
T = AVG LIQUID FILM TEMP IN RANKIN
TDIF = TEMP DIFF BETWEEN SAT STM AND AVE COOLANT TEMP
TSAT = STM SAT TEMP IN RANKIN
UTEST = UTEST SV - VALUE OF UTEST AND UEST FROM PREVIOUS ITERATION
XNU = NUSSELT NUMBER

ZZZ HET-12
CONTINUE
M5=12
IF (HETCN.EQ.1) WRITE (6,310) M5
STCO=STSAT+STCO*459.69/2.0
T=TSAT+1./((6452.562+2.*837533.2/T)/T**2)*EXP(14.15012-(6452.562+83
17533.2/T)/T)
BONE=-1.*(CJ*HSTO/ALMTD+(PG8*UTDP/ALMTD+1.)/RFACT)
UTEST=CJ*HSTO/(ALMTD*RFACT)
UTEST=(-SORT(BONE**2-4.*CONE)-BONE)/2.
DENOM=1.-UTEST*RFACT
IF (DENOM.GT.1.E-7) GO TO 240
HEFF=1.25
GO TO 240
HEFF=UTEST/DENOM
CONTINUE
ROUT=(HEFF+SHNF)/(HEFF*SHNF)
TDIF=STSAT-STBAVE
IF (TDIF.GT.0) GO TO 260
IF (TDIF.EQ.0) WRITE (6,660) STSAT,STBAVE,LJ,IR
TDIF=-1.
CONTINUE
DEFLM=DELTAT/HEFF
STCO=STFC-DGFLM
STWO=STCO-DLFLM

```

CON29290
CON29300
CON29310
CON29320
CON29330
CON29340
CON29350
CON29360
CON29370
CON29380
CON29390
CON29400
CON29410
CON29420
CON29430
CON29440
CON29450
CON29460
CON29470
CON29480
CON29490
CON29500
CON29510
CON29520
CON29530
CON29540
CON29550
CON29560
CON29570
CON29580
CON29590
CON29600
CON29610
CON29620
CON29630
CON29640
CON29650
CON29660
CON29670
CON29680
CON29690
CON29700
CON29710
CON29720
CON29730
CON29740
CON29750
CON29760

```

STFO=(STCO+STNO)/2.
XNU=OD/(SKOD*ROUT)
IF (ABS(UTEST-UEST),LJ,001) GO TC 270
IF (HETCN.EQ.1.) WRITE (6,610) K
DE LFLM=DLFLM
DLGFLM=DGFLM
UEST=UEST
K=K+1
IF (K.GT.4) UEST=0.5*(UTEST+UESTSV)
IF (K.LT.10) GO TO 120
IF (HETCN.EQ.1.) WRITE (6,640) UESTSV,UTEST
GO TO 290
IF (ABS(DLFLM-DLFLM),LJ,.01) GO TO 280
IF (HETCN.EQ.1.) WRITE (6,620) K
DE LFLM=DLFLM
DLGFLM=DGFLM
K=K+1
IF (K.LT.10) GO TO 120
WRITE (6,650) DLFLM,LJ,IR
IF (ABS(DLGFLM-DGFLM),LJ,.001) GO TO 290
K=K+1
IF (K.LT.20) GO TO 120
WRITE (6,630) DLGFLM,UEST,UTEST,LJ,IR
-----
HET 13
FINAL CALCULATIONS: EXIT HETTRN
HEFF = SEE XHEFF
TB2 = TUBE OUTLET TEMP
VNF = OVERAL HEAT X-FER COEF
VPSMH = OUTLET COOLANT TEMP
XHEFF = NUC GAS FILM HEAT X-FER COEF
NOTE: HERE VALUES OF HEFF, UEST, AND TB2 ARE PASSED
OUT OF HETTRN AND SAVED, BUT NOT RE-USED
TO START NEXT ITERATION. SEE NOTES IN
HET-2 AND HET-3.
-----
ZZZ HET-13
M5=13
WRITE (6,310) M5
VNF=UTEST
ROUT=1./ROUT
IF (IR.GT.1) GO TO 300
UEST=UEST

```


CON3 1210
CON3 1220
CON3 1230
CON3 1240
CON3 1250
CON3 1260
CON3 1270
CON3 1280
CON3 1290
CON3 1300
CON3 1310
CON3 1320
CON3 1330
CON3 1340
CON3 1350
CON3 1360
CON3 1370
CON3 1380
CON3 1390
CON3 1400
CON3 1410
CON3 1420
CON3 1430
CON3 1440
CON3 1450
CON3 1460
CON3 1470
CON3 1480
CON3 1490
CON3 1500
CON3 1510
CON3 1520
CON3 1530
CON3 1540
CON3 1550
CON3 1560
CON3 1570
CON3 1580
CON3 1590
CON3 1600
CON3 1610
CON3 1620
CON3 1630
CON3 1640
CON3 1650
CON3 1660
CON3 1670
CON3 1680

TB2=TB2C
AOC=PI*ALST*S00
AB=AO
WB=WB
FD AVE=0.5
SDI=SDI
SDI=SDI
AT=PI*ALST*SDI
SHMINV=SHMINC
ENHO=ENHOC
ENHF=ENHFC
STDIR=STBI*459.69
PTLIN=PSATFNTSIBIR
SHTBIC=0.0
SHTB2C=0.0
SUMQC=0.0
MTSTC=0.0
IRONC=0.0
WSOUT=0.0
SBRATC=0.0
TBDRYC=0.0
AMLSCC=WNCC/AMWNC
AXOC=SDC*HNOC*ALST*(SDDMIN-1.0)
SVGEXT=VGFNTSATEX*PMXEXT
SVNCEX=10.729*TSATEX/(AMWNC*(PMXEXT))
AMLT=AMLSEX+AMLSCC
SVMXEX=1.0/(AMLSEX/(AMLT*SVNCEX))
VELC(1)=(WSEXT+WNCC)*SVMXEX/(AXOC*3600.0)
VL CMAX=VELC(1)
G2=288.0*SG*SVMXEX
IF (VELC(1)-VELEX) 10,10.20
A2 DAL=VELC(1)/VELEX
DELPCT=((1.0-A2DAL)*VELEX**2)/G2
GO TO 50
A2 DAL=VELEX/VELC(1)
IF (A2DAL-0.715)*40.40.30
DELPCT=((0.73*(1.0-A2DAL)*VELC(1)**2)/G2
GO TO 50
DELPCT=((0.4*(1.25-A2DAL)*VELC(1)**2)/G2
PHIXC(1)=PMXEXT-DELPCT
PSATC(1)=PHIXC(1)*AMLSEX/(AMLSEX+AMLSCC)
RECALCULATE THE AREA RATIO (THE RATIO OF TUBE X-SECTIONAL
AREA TO TUBE SHEET AREA) TO INCLUDE THE COOLER

CON3 1690
CON3 1700
CON3 1710
CON3 1720
CON3 1730
CON3 1740
CON3 1750
CON3 1760
CON3 1770
CON3 1780
CON3 1790
CON3 1800
CON3 1810
CON3 1820
CON3 1830
CON3 1840
CON3 1850
CON3 1860
CON3 1870
CON3 1880
CON3 1890
CON3 1900
CON3 1910
CON3 1920
CON3 1930
CON3 1940
CON3 1950
CON3 1960
CON3 1970
CON3 1980
CON3 1990
CON3 2000
CON3 2010
CON3 2020
CON3 2030
CON3 2040
CON3 2050
CON3 2060
CON3 2070
CON3 2080
CON3 2090
CON3 2100
CON3 2110
CON3 2120
CON3 2130
CON3 2140
CON3 2150
CON3 2160

```

C      SECFLG=FLOAT(I,SEC)
      TSAREA=PI*(RNDRAD**2)*SECFLG*SECWID/360.
      AHOLE3=AAATD*TSAREA
      AHOLE5=AHOLE3*(PI*SDDO**2)*TNOC/4.
      TSAREA=TSAREA+HTCLR*HNOC*SDDC*SDDC
      ARATIO=AHOLE5/TSAREA

C      CALCULATE THE COOLER VOLUME
      VOLC=HTCLR*SDDC*SDDC*HNOC*ALST

C      CHECK TO SEE IF INITIAL PRESSURE LOSSES DROP THE PRESSURE
C      BELOW PTLIM
      IF (PSATC(1).GT.PTLIM) GO TO 80
      SUMOC=0.
      NRWSP4=1+VNOC*1
      CONSLA=PTLIM/LOAT(NRWSP4)
      CONSLB=PHXEXT/LOAT(NRWSP4)
      CUMDPC(1)=PHIX1-PHXEXT
      PSATC(1)=PTLIM
      PHIXC(1)=PHXEXT
      QOAC(1)=0.
      DELPC=PHXEXT
      UNOC(1)=700.
      WSC(1)=WSEXIT
      WCNDC(1)=0.

C      DO 60 M=2,NRWSP4
      WSC(M)=WSEXIT
      WCNDC(M)=0.
      PHIXC(M)=PHIXC(M-1)-CONSLB
      PSATC(M)=PSATC(M-1)-CONSLA
      CUMDPC(M)=PHIX1-PHIXC(M)
      CONTINUE

C      DO 70 M=2,IWNOC
      UNOC(M)=700.
      QOAC(M)=0.
      ALMTDC(M)=0.
      CONTINUE
      SHWBC=SHWBC+WB*TNOC
      SHTBIC=WB*TNOC*STBI
      SHTRC=1.
      EXIT
      RETURN
C

```

```

80      PAL=PSATC(I)
      TAL=TSATFN(PAL)
      STSATC(I)=TAL-459.69
      WSC(I)=WSEXIT
      CHECK TO SEE IF INLET STEAM TO COOLER IS 0
      IF (WSC(I).GT.1.) GO TO 90
      ENTER DUMMY VALUES IN COOLER VARIABLES
      CREATE NEGATIVE FLOW PARAMETER FOR USE IN COMPUTING EXITFRC
      TDRYC=TNOG
      SBRATC=WCNOAV
      SBFLOC=SBRATC+TDRYC
      WSC(I)=1.
      IROWC=3
      WG=VGFN(TAL,PMIXC(I))
      AMLSSC=WSC(I)/18.015
      VNC=10.729+TAL/(AMWNC*PMIXC(I))
      VMIX=1.0/((AMLSSC/(VG*(AMLSSC+AMLSSC)))+(AMLSSC+AMLSSC/
      (VNC)))
      VELC(I)=(WSC(I)+WNC)/VMIX/(AXOC*3600.0)
      NFC=(VNC+1.)/2.0
      ANFC=NFC
      IDT=0
      IRC=0
      IBT=0
      DO 450 IK=1,IVNOC
      I=IK
      LJ=7
      ROW BY ROW CALCULATION A LA HETTRN
      STSAT=STSATC(I)
      ANF=ANFC
      WS=WSC(I)
      WNC=WNC
      AXO=AXOC
      IR=I
      DATA HEFF,UEST,DGFLM,DLFLM/2100.,700.,0.05,2.0/
      DATA R2,E2OK/ 3.617,3.996,3.838,97.0,109.0,140.75/
      DATA R2/3.617,3.996,3.838/
      K=0
      RC=WNC/(WS+WNC)
CON3 2170
CON3 2180
CON3 2190
CON3 2200
CON3 2210
CON3 2220
CON3 2230
CON3 2240
CON3 2250
CON3 2260
CON3 2270
CON3 2280
CON3 2290
CON3 2300
CON3 2310
CON3 2320
CON3 2330
CON3 2340
CON3 2350
CON3 2360
CON3 2370
CON3 2380
CON3 2390
CON3 2400
CON3 2410
CON3 2420
CON3 2430
CON3 2440
CON3 2450
CON3 2460
CON3 2470
CON3 2480
CON3 2490
CON3 2500
CON3 2510
CON3 2520
CON3 2530
CON3 2540
CON3 2550
CON3 2560
CON3 2570
CON3 2580
CON3 2590
CON3 2600
CON3 2610
CON3 2620
CON3 2630
CON3 2640

```

```

TSAT=TSAT+459.69
GHAX=(WS+WNCI)/AXO
PSAT=PSATFN(TSAT)
AMOLSS=WS/18.015
AMOLSC=HNC/AMWNC
AMOLI=AMOLSS+AMOLSC
AMWAV=(WS+WNCI)/AMOLI
RMWNC=SQRT((AMWNCI)*AMOLSC/AMOLI)
RMWSC=4.24444*AMOLSS/AMOLI
AVIS=(SHUFN(TSAT))
HSTO=HFGFN(TSAT)
BB=WB/(PI*SDI*SDI/4)
STBAVE=(STBI+TB2)/2.0
DELFM=DLFLM
DLGFLM=DGFLM
STMO=TSAT-DELFM-DLGFLM
STFO=(STSAT+STMO)/2.0
XNRE=SDO*(WS+WNCI)/(AXO*3600.*AVIS)
IF (XNRE.GE.100.) GO TO 100
CONTINUE
COLB=EXP(0.53883-0.544*ALOG(XNRE))
IF (WNCI.EQ.0.) GO TO 110
PATM=PSAT/14.7
PG8=PSAT*(AMOLSC/AMOLSS)
TSATK=TSAT/1.8
CALL DFSVTY (TSATK,PATM,18.015,AMWNC,2.655,R2(JGAS),363.,E2OK(JGAS)
1),0.0,0.0G,DG)
C***
C 0.256 CONVERTS CM2/S TO FT2/HR AND 3600. CONVERTS VISCOSITY TO
C LB/F-HR FROM LB-F-S. 0.258 * 3600. = 928.8
C***
XNSCH=(AVIS*TSAT*10.73/((PSAT+PGB)*AMWAV*DG)) * 928.8
CJ=COLB*GHAX/(XNSCH*0.666667)
TB2=TSAT-(TSAT-TBI)/EXP(UEST*AD/(WB*CPFN(CBI,STBAVE)))
STBAVE=(STBI+TB2)/2.
SKBO=SKBFN(O.,STFO)
SKB=SKBFN(CBI,STBAVE)
BMU=BMUFN(CBI,STBAVE)
SHBI=CPFN(CBI,STBAVE)
XNREB=SDI*BB/BMU
XNPRB=SHBI*BMU/SKB
SHI=0.023*(XNREB)*0.8*XNPRB**0.33333*(SKB/SDI)*ENHI
RIN=AO/(SHI*AI)
BNF=ANF
IF (ANF.LE.1.0) BNF=1.0
IF (ANF.GT.1.0) BNF=ANF
SHMK=0.725*(SKBO**3*ROEFN(0.0,STFO)**2*HFGFN(STFO)*41.6975040.0/(BM
1UFN(0.,STFO)*SDO*DELFM))**0.25*ENHO
C

```

C THIS IS THE PLACE TO ENTER CORRECTIONS TO EXTERNAL FILM COEFFICIENT
C FOLLOWING IS A CORRECTION ACCORDING TO FUJII, ET. AL, TO ACCOUNT FOR
C EFFECTS OF VAPOR SHEAR AT HIGH VAPOR REYNOLDS NUMBERS

SHMK1=SHMK*SDO/SKBO
ANUS=SHMK*SDO/STSA1
EMUL=BMUFN(0,STSA1)*3600.
RHOL=RCFEN(0,STSA1)
RHOL=1./VGFN(1,STSA1,PSAT)
VISRA1=(EMUL/RHOL)/(EMUL/RHOL)
RETP=XNRE*VISRA1

IF (RETP.LT.0.) RETP=0.
IF (RETP.LT.0.) GO TO 120

TERM=SGRT(RETP1/ANUS
IF (TERM.LT.278) GO TO 130
ANUSP=1.24*(ANUS**0.8)*(RETP**0.1)
GO TO 140

ANUSP=ANUS*0.70/0.725
SHMKP=ANUSP*SKBC/SDO
SHMK=SHMKP

IF HO > 40,000

IF (SHMK.GT.40000.) GO TO 49
IF (SHMK.LT.40000.-AND.DELFLM.GT..0001) GO TO 49

49 CONTINUE

INUNDATION EFFECT MAY BE BYPASSED BY SETTING BNF = 1.

BNF = 1.
IF (FDAVE.LT.0.-OR.BNF.LT.2.) GO TO 150
FDAVN=0.6*FDAVE+(1.-0.5647*FDAVE)/BNF**20
FDAVM=0.6*FDAVE+(1.-0.5647*FDAVE)/(BNF-1)**20
SHNF=SHMK*(BNF*FDAVN-(BNF-1.)*FDAVM)
GO TO 160
SHNF=0.95*(BNF**0.9-(BNF-1.))**0.9)*SHMK

RFAC=RJN+SHWINV*FOUL+1./SHNF

COMPUTE LOG MEAN DELTA TEMP., ALMTD

CUN33130
CUN33140
CUN33150
CUN33160
CUN33170
CUN33180
CUN33190
CUN33200
CUN33210
CUN33220
CUN33230
CUN33240
CUN33250
CUN33260
CUN33270
CUN33280
CUN33290
CUN33300
CUN33310
CUN33320
CUN33330
CUN33340
CUN33350
CUN33360
CUN33370
CUN33380
CUN33390
CUN33400
CUN33410
CUN33420
CUN33430
CUN33440
CUN33450
CUN33460
CUN33470
CUN33480
CUN33490
CUN33500
CUN33510
CUN33520
CUN33530
CUN33540
CUN33550
CUN33560
CUN33570
CUN33580
CUN33590
CUN33600

```

C*****
HOMCI=STSAT-STBI
HIMCO=STSAT-TB2
C
IF (HIMCO.LT.1.E-15) WRITE (6,530) HOMCI,HIMCU,LJ,IR
IF (HIMCO.LT.1.E-15) HIMCO=1.E-15
C
RODT=HOMCI/HIMCO
C
IF INLET/OUTLET DELTA T RATIO IS NEAR 1.0, ALMTD = ARITH AVE
IF (RODT.GT.1.1) GO TO 170
ALMTD=0.5*(HOMCI+HIMCO)
C
IF (JRC.EQ.0) WRITE (6,540) STSAT,STBI,TB2,LJ,IR
JRC=1
GO TO 180
170
ALMTD=(HOMCI-HIMCO)/ALGG(RODT)
CONTINUE
IF (HOMCI.NE.0.) GO TO 190
RODT=1./SHNF
UTEST=1./RFACT
XNU=SHNF*SDD/SKBD
IF (ABS(UEST-UTEST)/UTEST.LT..001) GO TC 260
UEST=UTEST
IF (K.GT.4) UEST=0.5*(UTEST+UESTSV)
STWO=STSAT-(STSAT-STBAVEI)*UTEST/SHNF
STCO=STSAT
STFO=(STCO+STWO)/2.
DGLFM=0
DLFLM=STCO-STWO
DELFLM=DLFLM
K=K+1
IF (K.LT.20) GO TO 110
WRITE (6,510) UESTSV,UTEST
GO TO 280
CONTINUE
STCO=STSAT-DLGLFM
T=TSAT+STCO*55.69/2.0
DTDP=1./((6452.562+2.*837533.2/T)/T**2)*EXP(14.15012-(6452.562+83
17533.2/T)/T))
BONE=-1.*(CJ*HSTO/ALMTD+(PG8*DTDP/ALMTD+1.)/RFACT)
CONE=CJ*HSTO/(ALMTD*RFACT)
TTERM1=BONE**2
TTERM2=4.*CONE
TTERM=TTERM2/TTERM1
IF (TTERM.LT.0.999999) GO TO 200
UTEST=-BONE/2.
GO TO 220
190

```

```

200 IF ((4.*CONE).GT.(BONE**2)) UTEST=0.
210 IF ((4.*CONE).GT.(BONE**2)) GO TO 210
220 UTEST=1.-SORT((BONE**2-4.*CONE)-BONE)/2.
230 DENOM=1.
240 CONTINUE
250 IF (DENOM.GT.1.E-7) GO TO 230
HEFF=1.0E8
GO TO 240
HEFF=UTEST/DENOM
CONTINUE
ROUT=(HEFF+SHNF)/(HEFF*SHNF)
260 IF (STSAT-STBAVE
270 IF (TDIF.GT.0) GO TO 250
280 IF (IBT.EQ.0) WRITE (6,530) STSAT,STBAVE,LJ,IR
IBT=1
290 IF (IBT=1
300 CONTINUE
310 IF (LTAU=TDIF*UTEST
320 DGLFM=DELTAU/HEFF
330 DGLFM=DELTAU/SHNF
340 STCO=STCO-DGLFM
350 STFO=(STCO+STWO)/2.
360 XNU=SDO/(SKBO*ROUT)
370 IF (ABS(UTEST-UEST)/UTEST.LT..001) GO TO 260
380 DGLFM=DGLFM
390 DGLFM=DGLFM
400 UEST=UTEST
410 K=K+1
420 IF (K.GT.4) UEST=0.5*(UTEST+UESTSV)
430 IF (K.LT.20) GO TO 110
440 WRITE (6,510) UESTSV,UTEST
450 GO TO 280
460 IF (ABS(DELFLM-DGLFM).LT..01) GO TO 270
470 DGLFM=DGLFM
480 K=K+1
490 IF (K.LT.20) GO TO 110
500 IF (K.LT.320) DELFLM,LJ,IR
510 IF (ABS(DLGLFM-DGLFM).LT..001) GO TO 280
520 DGLFM=DGLFM
530 K=K+1
540 IF (K.LT.20) GO TO 110
550 WRITE (6,500) DLGLFM,UEST,UTEST,LJ,IR
560 VNF=UTEST
570 VPSH=TB2
580 XHEFF=HEFF

```

```

CON3 4090
CON3 4100
CON3 4110
CON3 4120
CON3 4130
CON3 4140
CON3 4150
CON3 4160
CON3 4170
CON3 4180
CON3 4190
CON3 4200
CON3 4210
CON3 4220
CON3 4230
CON3 4240
CON3 4250
CON3 4260
CON3 4270
CON3 4280
CON3 4290
CON3 4300
CON3 4310
CON3 4320
CON3 4330
CON3 4340
CON3 4350
CON3 4360
CON3 4370
CON3 4380
CON3 4390
CON3 4400
CON3 4410
CON3 4420
CON3 4430
CON3 4440
CON3 4450
CON3 4460
CON3 4470
CON3 4480
CON3 4490
CON3 4500
CON3 4510
CON3 4520
CON3 4530
CON3 4540
CON3 4550
CON3 4560

```

CON34570
CON34580
CON34590
CON34600
CON34610
CON34620
CON34630
CON34640
CON34650
CON34660
CON34670
CON34680
CON34690
CON34700
CON34710
CON34720
CON34730
CON34740
CON34750
CON34760
CON34770
CON34780
CON34790
CON34800
CON34810
CON34820
CON34830
CON34840
CON34850
CON34860
CON34870
CON34880
CON34890
CON34900
CON34910
CON34920
CON34930
CON34940
CON34950
CON34960
CON34970
CON34980
CON34990
CON35000
CON35010
CON35020
CON35030
CON35040

```

ROUT=1./ROUT
UNC(I)=VNF
ALMTDC(I)=ALMTD
SHIC(I)=SHI
SHNFC(I)=SHNF
RCC(I)=RC
ROUTC(I)=ROUT
VNREC(I)=XNRE
VPSHC(I)=VPSHH
HEFFC(I)=SHEFF

C COMPLETION OF TUBE H/T CALCULATION
C
HFG=HFGFN(STSATC(I))
MCNDC(I)=UNC(I)*AD*HNOC*ALMTDC(I)/HSTD
CALL PRSDRP (AL,VHIX,WSC(I),WNCC,AXOC,SDO,VPSHC(I),DELTPC,ENHF)
JY=0
WSC(I+1)=WSC(I)-MCNDC(I)
GFLWC(I)=WSC(I)+WNCC(I)/AXOC
CHECK FOR NEGATIVE STEAM FLOW
IF (WSC(I+1)-1) 300,300,360
IF PREVIOUS COND. RATE PREDICTS STEAM FLOW WILL GO NEG AFTER THE
NEXT ROW, SET CONDENSATE EQUAL TO STEAM FLOW.
MCNDC(I)=WSC(I)
IF STEAM FLOW HAS ALREADY GONE NEGATIVE THEN AVOID CALCULATING
TEST VARIABLE
IF (IROWC.GT.0) GO TO 310
CREATE A TEST VARIABLE INDICATING POINT IN COOLER WHERE STEAM
BAD AND A NEGATIVE FLOW RATE FOR USE IN CALCULATING EXITFRC
WTSTC=(WSC(I+1)-1.)/(WSC(I)-WSC(I+1)+1.)
WTSTC=WTSTC-FLOAT(IVNOC-I)
IROWC=1
NRDRY=IVNOC-I
TBDRYC=INOC*(FLOAT(NRDRY)/FLOAT(IVNOC))
TBDRYC=TBDRYC-WTSTC*HNOC
SBRATC=WCNDC(I)/HNOC
SBRFLOC=SBRATC+TBDRYC

```

C C

290

C C C

300

C C C C

C C C C

C

C


```

310 STSATC(I+1)=STFC
C TSATMN=STSATC(I+1)+459.69
C PHIN=PSATFN(TSATMN)
C ENTER DUMMY VALUE FOR NEXT ROW MSC
C MSC(I+1)=1.
C QGC=(WSC(I)*CPSFN(TAL)/18.015+WNCC*CPAFN(TAL,JGAS)/AMWNC)*(TAL-TSA
1TMN)
C QTC=QGC+HCNDC(I)*HFG
320 IF (STSATC(I)-TB2) 320,320,330
330 TB2=STSATC(I)-0.1
C CONTINUE
C IF (STSATC(I+1).GT.STBI) GO TO 340
C ALMTDC(I)=ALMTDC(I-1)
C GO TO 350
340 CONTINUE
C ALMTDC(I)=(STSATC(I+1)-STBI)-(STSATC(I)-TB2))/ALOG((STSATC(I+1))-S
1TB1)/(STSATC(I)-TB2))
C CONTINUE
350 CONTINUE
C UNCL(I)=QTC/(AD*HNOC*ALMTDC(I))
C AMLSSC=WSC(I+1)/18.015
C PHIXC(I+1)=PHIXC(I)-DELTPC
C PHIXC(I+1)=PHIXC(I)-DELTPC
C PSATC(I+1)=(PHIXC(I+1)*AMLSSC)/(AMLSSC+AMLSCC)
C TSATC(I)=TSATMN
C GO TO 440
C AMLSSC=WSC(I+1)/18.015
C PHIXC(I+1)=PHIXC(I)-DELTPC
360 PSATC(I+1)=(PHIXC(I+1)*AMLSSC)/(AMLSSC+AMLSCC)
C CHECK TO SEE IF STEAM CORRECTIONS FOR DRY TUBES OKOVE PSATC TOO LO
C IF ((ROWC-GT.0).AND.(PSATC(I+1).LE.PTILM)) WRITE (6,560) 1
C PSATC(I+1)=PSATC(I)
C CHECK FOR PRESSURE DROPPING BELOW PTILM
C IF (PSATC(I+1).GT.PTILM) GO TO 390
C CALCULATE PARAMETERS FOR CURRENT ROW
C PSATC(I)=PTILM
C CUMDPC(I)=PHIXC(I)
C SUMQC=SUMQC+UNC(I)*AD*ALMTDC(I)*HNOC
C QDAC(I)=UNC(I)*ALMTDC(I)

```

```

C
SMNBC=SMWBO+WB*HNOC
SMTBI C=SMTBI C+WB*HNOC*STBI
SMTBI C=SMTBI C+WB*HNOC*STBI
NRWSP4=IYNOC+1
RTG=ELQAT(NRWSP4-1)
NRWSP3=1+1
CONST=PHIXC(1)/RTG
CONST2=PI*Y/R TG
C
C
CALCULATE PARAMETERS FOR THE REMAINING ROWS
DO 370 M=NRWSP5,NRWSP4
GO AC(M)=0
WSC(M)=WSC(M-1)
MCNOC(M)=0
ST SATC(M)=ST SATC(M-1)
PSATC(M)=PSATC(M-1)-CONST2
PHIXC(M)=PHIXC(M-1)-CONST
VELC(M)=VELC(M-1)
CONTINUE
370
C
DO 380 IFX=NRWSP5, IYNOC
UNC(1,IFX)=UNC(1,IFX-1)
CUMNOC(1,IFX)=CUMNOC(1,IFX-1)+PHIXC(1,IFX-1)
SMTBI C=SMTBI C+WB*HNOC*STBI
SMTBI C=SMTBI C+WB*HNOC*STBI
GO AC(1,IFX)=0
SMNBC=SMNBC+WB*HNOC
ALHTDC(1,IFX)=0
380
C
DE LPC=PHIXC(1)-PHIXC(NRWSP4)
GO TO 460
C
390
PAL=PSATC(1+1)
IF (PAL.GT.0.) GO TO 400
WRITE (4,530) PHIXC(1),1
COMTE NUE
ISATC=1+STFNM(PAL)
ST SATC(1+1)=TSATC-PAL) .LT.0.001) ISATC=IAL-0.001
IF (AB$ (UNC(1)+1)=TSATC-PAL) .LT.0.001) ISATC=IAL-0.001
MCNOC(1)=UNC(1)+1+TSATC-PAL) .LT.0.001) ISATC=IAL-0.001
1PAFNI(TSATC,JGA SI/AMWNC)+TSATC-IAL-1SATC(1)/HFG
IF (AB$ (MCNOC(1)-1.01)-.005) 430,410,410
MCNOC(1)=MCNOC
JV=JV+1
IF (JY-50) 290,290,420
C
410

```



```

C
500  RETURN
510  FORMAT (1H0.36H NO CONVERGENCE IN FILM TEMPERATURES, 8H DLVFLM=, E12.5/10H SECTOR =, E12.5H ROW=, I5)
520  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
530  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
540  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
550  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
560  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
570  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
580  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
590  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
600  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
610  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
620  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
630  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
640  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
650  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
660  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
670  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
680  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
690  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
700  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
710  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
720  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
730  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
740  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
750  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
760  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
770  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
780  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
790  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
800  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
810  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
820  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
830  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
840  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
850  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
860  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
870  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
880  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
890  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
900  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
910  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
920  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
930  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
940  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
950  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
960  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
970  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
980  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
990  1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)
1000 1.5TH UEST =, E12.5H SECTOR =, E12.5H ROW=, I5)

```

```

2VP SHHC(100),HEFFC(100),UNC(100),WCNDC(100),GFLOWC(100),QOAC(100),C CON3 6970
3UMDPC(100) CON3 6980
COMMON /COOL/ IYNOC,HNOG,INOC,TSATEX,PMXEXT,AMLSEX,WSEXIT,VEEXT,T CON3 6990
1B2C,ENHIC,ENHOC,ENHFC,SHWINC,WBC CON3 7000
COMMON /OUT2/ R CORR,RSPP,PHPCON,VOLIC CON3 7010
DIMENSION ANTS(15) CON3 7020
DELPVE=0. CON3 7030
ADT=0. CON3 7040
VEL3=0. CON3 7050
CAHT=0. CON3 7060
UBARW=0. CON3 7070
VBARW=0. CON3 7080
SECFLG=FLOAT(1 SEC) CON3 7090
DO 10 I=1,NOROWS CON3 7100
OO=OOO I-DELOC*FLOAT(1-1) CON3 7110
CAHT=CAHT+(CO*OO/144.-SID(I))*TBNPR(I) CON3 7120
AD=3.141594OO*ALST*TBNPR(I)/12. CON3 7130
VBARW=VBARW+VW(I) CON3 7140
ADT=AOT+AO CON3 7150
BUNHT=PI*CAHT*ALST*TUBESW*SECFLG/4. CON3 7160
ADT=AOT+SECFLG CON3 7170
DO 30 J=1,1 SEC CON3 7180
DO 20 I=1,NOROWS CON3 7190
UBARW=UBARW+UN(I,J)*TBNPR(I) CON3 7200
VEL3=VEL3+VEL(NOROWS,J) CON3 7210
DELPVE=DELPVE+DELP(J) CON3 7220
CONTINUE CON3 7230
UBARW=UBARW/TNO CON3 7240
VBARW=VBARW/FLQAT(NOROWS) CON3 7250
VEL3=VEL3/SECFLG CON3 7260
DELPVE=DELPVE/SECFLG CON3 7270
ADTCND=SUMQ/(UBARW*AOT) CON3 7280
STSATX=TSATEX-459.69 CON3 7290
TDROP1=STSAT(1,1)-STSATX CON3 7300
RSPI=RSPP*12. CON3 7310
BNDIAM=BNDRAD*2. CON3 7320
BL=ALST/2. CON3 7330
VOID1=RAIDINS*2. CON3 7340
AVTB2=SHTB1/SHWB CON3 7350
HDLOSS=DELP*144./62.366 CON3 7360
CON3 7370
CON3 7380
CON3 7390
CON3 7400
CON3 7410
CON3 7420
CON3 7430
CON3 7440

```

THERE IS THE POSSIBILITY THAT THE AVERAGE INLET COOLANT TEMP
 (AVTB1) EQUALS THE AVERAGE OUTLET COOLANT TEMP (AVTB2). WHEN
 THE CONDENSER IS CONFIGURED SUCH THAT NO HEAT IS REMOVED FROM
 THE STEAM

CON38890
CON38900
CON38910
CON38920
CON38930
CON38940
CON38950
CON38960
CON38970
CON38980
CON38990
CON39000
CON39010
CON39020
CON39030
CON39040
CON39050
CON39060
CON39070
CON39080
CON39090
CON39100
CON39110
CON39120
CON39130
CON39140
CON39150
CON39160
CON39170
CON39180
CON39190
CON39200
CON39210
CON39220
CON39230
CON39240
CON39250
CON39260
CON39270
CON39280
CON39290
CON39300
CON39310
CON39320
CON39330
CON39340
CON39350
CON39360

```

VHBARC=VHBAR
IF (AVTBIC.EQ.AVTB2C) DTCOL2=0
IF (AVTBIC.EQ.AVTB2C) UPCCOL=UBARWC
IF (AVTBIC.EQ.AVTB2C) GO TO 20

DTCOL2=(AVTB2C-AVTB1C)/ALOG((STSATX-AVTB1C)/(STSATX-AVTB2C))
UPCCOL=SUMQC/(AOTC*DTCOL2)

VALUES FOR OVERALL OUTPUT
AOTOT=AOTC+AOT
TNOT=INC+TNOC
UBAROA=(UBARWC*TNOC+UBARWC*TNOC)/TNOC
ADTOA=(SUMQC+SUMQ)/UBAROA
DELPOA=PHIX1-PHIXC(IVNOG+1)
TORPOA=STSAT1-STSATC(IVNOG+1)
SUMQOA=SUMQC+SUMQ
HTQA=BUNWT+COOLWT
AVTB1A=(AVTB1*TNOC+AVTB1C*TNOC)/TNOC
AVTB2A=(AVTB2*TNOC+AVTB2C*TNOC)/TNOC
SMWBOA=SMWBC+SMWB
HOLSDA=DELWP*144./62.366
DTOA=(AVTB2A-AVTB1A)/ALOG((STSAT1-AVTB1A)/(STSAT1-AVTB2A))
UPQA=SUMQOA/(AOTOT*DTOA)
WRITE (6,60)
WRITE (6,50)
WRITE (6,60)
WRITE (6,70)
WRITE (6,110)
WRITE (6,100)
IF (EXITFC.LT.-900.) WRITE (6,100)
IF (EXITFC.LT.-900.) GO TO 30
WRITE (6,80) EXITFC
IF (WTSTC.LT.0) WRITE (6,90) WTSTC
WRITE (6,120)
WRITE (6,130)
WRITE (6,140)
WRITE (6,150)
WRITE (6,160)
WRITE (6,170)
WRITE (6,180)
WRITE (6,190)
WRITE (6,210)
WRITE (6,220)

```

C

C

C

C

20

C

C

C

30

C

[illegible]

```

20  C10=0.1685/TKOE**1.2063+0.5328/TKOE**0.1579
    RTSM=(1./AM1+1./AM2)*0.5
    B=(10.7-2.46*RTSM)*1.E-4
    DG=B*TK**1.5*RTSM/PATH/R12**2/CID
    IF (V1.EQ.0.0) GO TO 40
    CONTINUE
    DGG=0.0043*TK**1.5*RTSM/PATH/(V1**0.333+V2**0.333)**2
    GO TO 40
30  CONTINUE
40  WRITE(6,50)
    RETURN
50  FORMAT (103H0 ** NEITHER FORCE CONSTANTS NOR MOLECULAR VOLUMES EX
    LIST AS ARGUMENTS. CALCULATIONS CANNOT PROCEED. **)
    END
C
C *****
C FUNCTION XTR (X,Y,N,T,SM,XIN,YN,M)
C *****
C FUNCTION XTR ASSUMES A LOG-LOG MODEL, IE LOG Y = A + B1 * LOG
C AND PERFORMS A LINEAR LEAST SQUARE REGRESSION ON THE
C TRANSFORMED POINTS, ALL POINTS ARE USED FOR EACH REGRESSION
C EXCEPT FOR THE FIRST, WHICH IS NOT USED AT ALL
C *****
DI MENSICN XIN(11),YN(11)
IF (Y.EQ.0.) Y=0.0001
IF (N.EQ.0.) GO TO 30
X1N(N)=ALOG(X)
YN(N)=ALOG(Y)
IF (N.LT.2) GO TO 40
SX1N=0.0
SYN=0.0
IF (M.LT.N-3) M=N-3
DO 10 I=M,N
    SX1N=SX1N+XIN(I)
    SYN=SYN+YN(I)
CONTINUE
X1BAR=SX1N/(N-M+1)
YBAR=SYN/(N-M+1)
SX1Y=0.0
DO 20 I=M,N
    SX12=SX12+(XIN(I)-X1BAR)*(YN(I)-YBAR)
    SX1Y=SX1Y+(XIN(I)-X1BAR)*YBAR
CONTINUE
B1=SX1Y/SX12
A=YBAR-B1*X1BAR
TN=ALOG(T)

```

CON41290
 CON41300
 CON41310
 CON41320
 CON41330
 CON41340
 CON41350
 CON41360
 CON41370
 CON41380
 CON41390
 CON41400
 CON41410
 CON41420
 CON41430
 CON41440
 CON41450
 CON41460
 CON41470
 CON41480
 CON41490
 CON41500
 CON41510
 CON41520
 CON41530
 CON41540
 CON41550
 CON41560
 CON41570
 CON41580
 CON41590
 CON41600
 CON41610
 CON41620
 CON41630
 CON41640
 CON41650
 CON41660
 CON41670
 CON41680
 CON41690
 CON41700
 CON41710
 CON41720
 CON41730
 CON41740
 CON41750
 CON41760

```

30 XTR=EXP((TN-A)/B1)
40 GO TO 50
C *****
C XTR=X*(1.+(Y-T)*5.*SW)
C *****
C CHANGE OF VARIABLE IS LIMITED TO 10 PERCENT
C *****
50 IF (ABS(XTR-X)/X-LT.0.1) GO TO 60
C XTR=X*(1.+0.1*ABS(Y-T)/(Y-T)*SW)
60 RETURN
C END
C
C FUNCTION AMUFN (T,JGAS)
C IMIX=0
C GO TO (30,20,10), JGAS
10 IMIX=1
20 CONTINUE
C INERT GAS IS CO2
C ** VISCOSITY FOR CARBON DIOXIDE LB/FT-SEC
C GAS2=1.0E-5*(-0.046+(2.282E-3+(-6.131E-7+9.699E-11*T)*T)*T)
C AMUFN=GAS2
C IF (IMIX.EQ.0) RETURN
30 CONTINUE
C INERT GAS IS AIR
C GAS1=1.0E-5*(0.1490+(0.238E-2)*T-(-.7209E-6)*T**2+(-.1184E-9)*T**3)
C AMUFN=GAS1
C IF (IMIX.EQ.0) RETURN
C INERT GAS IS MIXTURE OF AIR & CO2
C GAS3=(GAS1+GAS2)/2.0
C AMUFN=GAS3
C RETURN
C END
C
C FUNCTION BMUFN (C,T)
C VISCOSITY OF SALINE SOLUTION. RANGE OF DATA WAS 0 - 24 PERCENT
C CONCENTRATION AND 40 - 210 DEGREES FARENHEIT.
C R=T+.55.69
C BMUFN=DEXP(-0.11591155D+2*C+0.12602329D-1*C*R+0.38637378D+4*C/R+0.
14606532D-2*R+0.47595941D+4/R-0.1059252566D+2)
C RETURN
C END
C
C FUNCTION CPAFN (T,JGAS)
C IMIX=0
C GO TO (30,20,10), JGAS

```

CON41770
 CON41780
 CON41790
 CON41800
 CON41810
 CON41820
 CON41830
 CON41840
 CON41850
 CON41860
 CON41870
 CON41880
 CON41890
 CON41900
 CON41910
 CON41920
 CON41930
 CON41940
 CON41950
 CON41960
 CON41970
 CON41980
 CON41990
 CON42000
 CON42010
 CON42020
 CON42030
 CON42040
 CON42050
 CON42060
 CON42070
 CON42080
 CON42090
 CON42100
 CON42110
 CON42120
 CON42130
 CON42140
 CON42150
 CON42160
 CON42170
 CON42180
 CON42190
 CON42200
 CON42210
 CON42220
 CON42230
 CON42240

```

10      IMIX=1
20      CONTINUE
C** INERT GAS CAPACITY FOR MW = 40.1      BTU/LB-MOL - DEG R
      GAS2=0.209*40.1
      CP AFN=GAS2
      IF (IMIX.EQ.0) RETURN
30      CONTINUE
C** INERT GAS IS AIR
      CP AFN=1.7139-0.9884E-3*T+0.1393E-5*T**2-0.3367E-9*T**3
C AIR
      GAS1=7.139-0.9884E-3*T+0.1393E-5*T**2-0.3367E-9*T**3
      CP AFN=GAS1
      IF (IMIX.EQ.0) RETURN
C INERT GAS IS MIXTURE OF AIR & CO2
      GAS3=(GAS1+GAS2)/2.0
      CP AFN=GAS3
      RETURN
      END
C
      FUNCTION CPSFN (C,T)
      IF (C-0.005) 20,20,30
      IF (C-0.005) 20,20,30
      EQUATION SPECIFIC HEAT FOR PURE WATER
      GO TO 40
      EQUATION SPECIFIC HEAT FOR BRINE
      CP = 96946859+(2*(10.00010404965)*T)-(.91199294*(C1)+(2*(.000648296
      1591*(C#1)+(1.535779*(C#2)))+(2*(.0076721465)*(C#2)*T)+16.7981008
      2*(C#3)))+(2*(.012610354)*(C#3)*T)
      CPSFN=CP
      RETURN
      END
C
      FUNCTION CPSFN (T)
C** CPSFN CALCULATES THE HEAT CAP OF STEAM IN BTU/LB-MOL-R GIVEN T IN
      DEG R. EQUATIONS FROM H. NORITAKE, BASED ON TABULATED VALUES IN
      NASA TR-R-132
C** CPSFN=(7.838-(.2531E-3-(.2892E-6-(.7693E-10*T)*T)*T)
      RETURN
      END
C
      FUNCTION HFGFN (T)
      HFGFN=1093.88-0.5703*T+.00012819*T**2-.0000008824*T**3
      RETURN
      END

```

```

CON42250
CON42260
CON42270
CON42280
CON42290
CON42300
CON42310
CON42320
CON42330
CON42340
CON42350
CON42360
CON42370
CON42380
CON42390
CON42400
CON42410
CON42420
CON42430
CON42440
CON42450
CON42460
CON42470
CON42480
CON42490
CON42500
CON42510
CON42520
CON42530
CON42540
CON42550
CON42560
CON42570
CON42580
CON42590
CON42600
CON42610
CON42620
CON42630
CON42640
CON42650
CON42660
CON42670
CON42680
CON42690
CON42700
CON42710
CON42720

```



```

C
C
CCC
C
C
END
SUBROUTINE PRSDRP (TSAT,VMIX,WS,MNC,AXC,SDO,SF,DELPTP,ENHF)
PRSDRP REBUILT ON 9-16-69 TO USE EQUATION FOR SF
SG=32.174
GSTAR=(WS+MNC1/(AXD*3600.))
ANRE=(SCD*GSTAR)/SMUFN(TSAT)
SF=(10.102+52.2/ANRE)*ENHF
DELPTP=SF*GSTAR**2*VMIX/(72.0*SG)
RETURN
END
C
FUNCTION PSATFN (T)
PSATFN=2.718**((14.150119-(6452.5621/T))-(837533.21/T**2))
RETURN
END
C
C
C
FUNCTION ROEFN (C,T)
DENSITY OF SALINE SOLUTION. RANGE OF DATA WAS 0 - 26 PERCENT
CONCENTRATION AND 40 - 300 DEGREES FARENHEIT
ROEFN=0.62707172E2+0.49364088E2*C-(0.43955304E-2+0.32554667E-1*C+
10.46076921E-4-0.63240299E-4*C1)*T
RETURN
END
C
C
C
FUNCTION SKBFN (C,T)
THERMAL CONDUCTIVITY OF SALINE SOLUTION. RANGE OF DATA
0 - 24 PERCENT CONCENTRATION AND 40 - 300 DEGREES FARENHEIT
SKBFN=(-301.57913+.697989E-3*T-.012506E-5*T**2-.2072E-10*T**3)*(-.16
187109+C+1.)
RETURN
END
C
C
C
FUNCTION SMUFN (T)
SMUFN=1.0E-5*(0.122+(1.001E-3)*T+(2.892E-7)*T**2-(7.693E-11)*T**3)
RETURN
END
C
C
FUNCTION TSATFN (P)
AA=(ALOG(P))-14.150119)

```

CON42730
CON42740
CON42750
CON42760
CON42770
CON42780
CON42790
CON42800
CON42810
CON42820
CON42830
CON42840
CON42850
CON42860
CON42870
CON42880
CON42890
CON42900
CON42910
CON42920
CON42930
CON42940
CON42950
CON42960
CON42970
CON42980
CON42990
CON43000
CON43010
CON43020
CON43030
CON43040
CON43050
CON43060
CON43070
CON43080
CON43090
CON43100
CON43110
CON43120
CON43130
CON43140
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CON43200

CON43210
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CON43370
CON43380
CON43390
CON43400
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CON43460
CON43470
CON43480
CON43490
CON43500
CON43510
CON43520
CON43530
CON43540

```

DET=6452.5621*2-(4.0*AA*837533.21)
IF (DET) 10,20,20
WRITE (6,60)
CALL EXIT
X=(-6452.5621+SQRT(DET))/(2.0*AA)
Y=(-6452.5621-SQRT(DET))/(2.0*AA)
IF (X-V) 30,40,40
TSATFN=Y
GO TO 50
TSATFN=X
CONTINUE
RETURN
FORMAT (1H1,37H SUBROUTINE TSATFN FINDS COMPLEX ROOTS)
END

FUNCTION VGFN (T,P)
X=ALOG(T/P)
VGFN=EXP((.103758E-2*X-.0177861)*X+1.10267)*X-.72240)
RETURN
END

SUBROUTINE SWITCH (A,N)
DIMENSION A(N)
NN=N/2
K=N+1
DO 10 I=1,NN
T=A(I)
A(I)=A(K-I)
A(K-I)=T
CONTINUE
RETURN
END

```

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5